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REQUIREMENTS FOR EXPLOSION-PROOF ELECTRICAL EQUIPMENT IN AIR FORCE HANGARS

Lester A. Eggleston, et al

Southwest Research Institute

Prepared for:

Air Force Weapons Laboratory

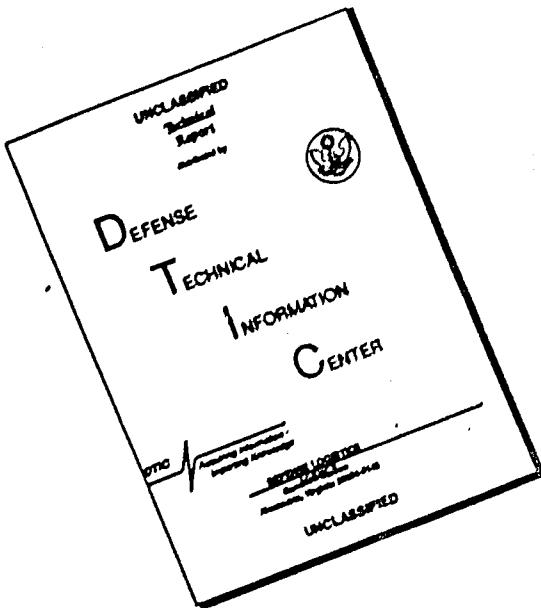
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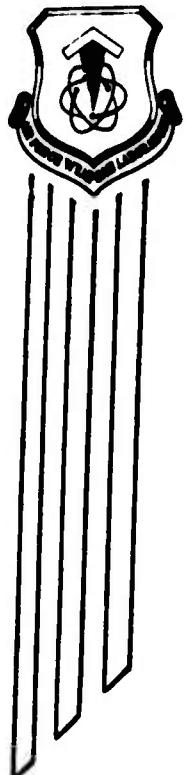
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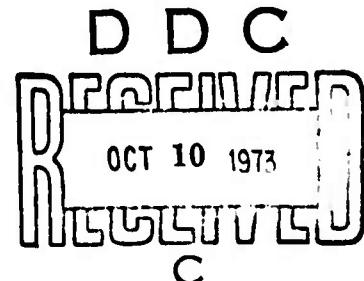
Lester A. Eggleston

Michael D. Pish

Southwest Research Institute
San Antonio, Texas

TECHNICAL REPORT NO. AFWL-TR-72-135

August 1973



AIR FORCE WEAPONS LABORATORY
Air Force Systems Command
Kirtland Air Force Base
New Mexico

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Lester A. Eggleston
Michael D. Pish
Southwest Research Institute
San Antonio, Texas

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FOREWORD

This report was prepared by the Southwest Research Institute, San Antonio, Texas, under Contract F29601-71-C-0116. The research was performed under Program Element 63723F, Project 683M, Task 2.

Inclusive dates of research were June 1971 through July 1972. The report was submitted 15 June 1973 by the Air Force Weapons Laboratory Project Officer, Mr. Frederick H. Peterson (DEZ).

This technical report has been reviewed and is approved.



FREDERICK H. PETERSON
Project Officer



OREN G. STROM
Lt Colonel, USAF
Chief, Aerospace Facilities Branch



WILLIAM B. LIDDICOET
Colonel, USAF
Chief, Civil Engineering Research
Division

ABSTRACT

(Distribution Limitation Statement A)

The objective of this research effort was to determine if current requirements for explosion-proof equipment in USAF hangars are more stringent than necessary, and thereby result in unnecessary expense in meeting such requirements. Experiments and tests conducted, both in actual USAF hangars and in the laboratory, indicated that the vapor explosibility hazard from leaks and fuel spills is lower than generally believed. The results of this study indicate that hazardous zone definitions in existing codes could be relaxed without compromising safety. Vertical profile measurements of fuel spills and fuel leak vapors showed that under normal conditions of ventilation, the atmosphere in the 2-in. level was usually well below the lower explosive limit (LEL). Even with the extreme condition of volatile fuel spills in quiescent, confined spaces, the LEL level did not rise above 7 inches. It was concluded, therefore, that all portions of hangar spaces more than 12 in. above the floor could be considered as nonhazardous with respect to vapors from aircraft fuel spills and leaks relating to explosion-proof equipment requirements. In view of this, it further concluded that the 18-inch upper boundary in existing National Electric Code (NEC) and the Occupational Safety and Health Act (OSHA) requirements are more than adequate to ensure safety.

CONTENTS

<u>Section</u>		<u>Page</u>
I	INTRODUCTION	1
II	DISCUSSION OF THE PROBLEM	2
III	TEST PROGRAM INSTRUMENTATION	6
	Instrument Package Design	6
	Calibration	8
	Sampling Considerations	11
IV	TEST FACILITIES	12
	Simulated Hangar Space	12
	Selected USAF Hangars	12
V	TEST PROGRAM CHRONOLOGY AND TABULATED RESULTS	18
	Phase 1	18
	Phase 2	18
	Phase 3	18
	All-Phase Work	21
	Phase 4	21
	Data Reduction	21
VI	ANALYSIS OF RESULTS AND CONCLUSIONS	26
	Discussion of the Test Results	26
	Conclusions	28
	Recommended Revised Text for Par 7-10, AFM 88-15	29
APPENDIXES		
	I. Excerpts from AFM 88-15 and National Electrical Code	30
	II. Sampling Configurations	35
	III. Plots of the Test Information	44
	IV. Tables of Test Results	74

CONTENTS (cont'd)

<u>Section</u>	<u>Page</u>
REFERENCES	114
DISTRIBUTION	115

ILLUSTRATIONS

<u>Figure</u>		<u>Page</u>
1	Comparison of Hazardous Area Definitions by Article 513 of National Electrical Code and AFM 88-15	4
2	Instrument Package System Diagram	7
3	Photograph of Instrument Package	9
4	Lower Explosive Limits for Fuels and Various Saturated Hydrocarbons	10
5	Floor Plan--Simulated Hangar Space	13
6	Interior View of Simulated Hangar Space	14
7	View of Hangar 5, at Randolph Air Force Base, During Test 26	15
8	View of Randolph Air Force Base Spill Test 27	16
9	View of Hangar 4337, at Bergstrom Air Force Base, During Test 28	17
10	Vertical Profiles of Vapor Concentration, Tests 34-37	23
11	Calculated Diffusion of Benzene into Air	26

TABLES

<u>Table</u>		<u>Page</u>
1	Maximum Vapor Concentrations in a 200-Sq-Ft Closed Room, Quiescent Conditions, Sampling in a Single Plane	19
2	Maximum Vapor Concentrations in a 200-Sq-Ft Closed Room, Quiescent Conditions, Sampling in Three Vertical Planes	20
3	Vertical Profiles of Maximum Vapor Concentrations in Sealed Room	22
4	Maximum Vapor Concentrations in Selected Typical USAF Hangars	24

ABBREVIATIONS

AC	alternating current
ASTM	American Society for Testing Materials
atm	atmosphere(s)
avgas	aviation gasoline
Div	Division
LEL	lower explosive limit
l/min	liters per minute
MSA	Mine Safety Appliances
NA	nonapplicable
NEC	National Electrical Code
NFPA	National Fire Protection Association
O.D.	outside diameter
Ref(s)	reference(s)
R.H.	relative humidity
sec	second
UDMH	unsymmetrical dimethyl hydrazine
UEL	upper explosive limit
V	volt
Vol%	percent by volume

SECTION I

INTRODUCTION

Many informed persons have been concerned about existing codes pertaining to the explosivity of aircraft fuel vapors in aircraft hangars and resultant requirements for explosion-proof electrical equipment. No data were available with which engineering judgments could be made of criteria now in force. Accordingly, the Civil Engineering Division of the Air Force Weapons Laboratory was directed early in 1971 to carry out an appropriate investigation of the basic problem. On 16 June 1971, the Air Force Weapons Laboratory negotiated a contract with the Southwest Research Institute to accomplish the required research. The Statement of Work for this specifically required the contractor to prepare and submit recommended revisions of AFM 88-15, if such were deemed necessary.

The decided approach to the problem consisted of both laboratory and field tests. Initially, spill and leakage tests would be conducted on a small scale in a simulated hangar environment. These would provide information on the effects of varying fuels, exposed surface areas, temperature, humidity, barometric pressure, and various typical building design features (such as pressurizing to block vapor flow). Laboratory work was carried out in three phases. In Phase 1, sampling was carried out in a single geometric plane for points 18 inches apart between the vapor source and the wall of the room. Vertical increments were taken at points 4 inches to 16 inches above the floor. In Phase 2, sampling was carried out at the center of the room and at points 2 feet from the walls of each corner at heights of 2, 12, 18, and 48 inches. In addition, three points were monitored at the 96-inch ceiling level. Phase 3 studied vertical profiles of vapor concentration at 2-inch intervals up to 24 inches and at 1/2-inch intervals up to 12 inches. Field work was carried out in USAF hangars at Kelly AFB, Randolph AFB, and Bergstrom AFB. The objective of this work was to secure maximum parking and maximum maintenance occupancy for worst-case conditions with fully fueled aircraft and extended closed door operations. A large-scale JP-4 spill test also was included. Sampling was generally at 2 inches above the floor.

To secure quantitative information on actual vapor concentrations arising from flammable liquid spills or leaks under various conditions, a total of 32 tests was carried out under simulated hangar conditions, together with five tests in operating USAF hangars. A total of 124,122 data points was recorded during 591 hours and 10 minutes of testing. The instrumentation consisted of a Beckman Model 400 Total Hydrocarbon Analyzer and a Honeywell 24-Point Recorder which controlled a bank of three-way solenoid valves in a continually purged and synchronized sampling system. The instrumentation was regularly calibrated against a standard methane-air mixture which had been analyzed using a Perkin-Elmer Gas Chromatograph. Based on data compiled by the US Bureau of Mines, the average lower explosive limit (LEL) of JP-4 and 115/145 avgas was taken at 1.25 percent by volume (12,500 ppm). This figure was then used in calculating the fuel vapor equivalent of the methane-air standard calibration gas.

SECTION II

DISCUSSION OF THE PROBLEM

An unwritten principle of industrial safety states that if a hazard is known to exist, adequate measures must be taken to avoid loss of life or property because of it. Sound economic practice requires that any protective measures taken must be suited both to the severity of the exposure and to the likelihood of adverse consequences. Whenever data on severity and probability are not available, it is not unusual to assume the worst situation and devise countermeasures accordingly.

This practice can be justified only on the grounds that any and all expenditures for safety are worthwhile - a premise which is difficult to defend. Frequently, the costs of protection can far exceed the benefits to be realized, and unless safety requirements are based on sound information, the expense may quickly reach the point of diminishing returns on the investments involved and defeat its own purpose. Appreciable savings can be realized when the costs of the safety measures provided are equated against the hazard probabilities.

The use, handling, and storage of flammable liquids involves an unavoidable hazard potential. Hangars used for parking and maintenance of partially or fully fueled aircraft can regularly contain areas where concentrations of fuel vapors could conceivably build up to the lower explosive limit (LEL). Some aircraft fuel systems have no allowance for thermal expansion. A fueled aircraft moved into a warm hangar will drip fuel at the tank outlets. In such areas, any source of ignition might produce serious consequences. One obvious protective measure is to minimize the ignition probability by using explosion-proof electrical fixtures in zones where vapor concentrations could present a hazard. These are specified in both the National Fire Protection Association (NFPA) Standards for civil aircraft which include the National Electrical Code (NEC) and AFM 88-15 for military hangars. The question thus arises as to which standard is most appropriate. If one is just adequate, the other would appear to be either deficient or excessive, depending on which is used as the reference. For both, the fuel volatilities involved are essentially the same.

The NFPA began formulating its aviation standards about 1950 when piston aircraft dominated the scene and gasoline was the principal fuel used. Efforts to ascertain the basis used by the NFPA committee in defining the limits of the hazardous areas have been unsuccessful. As far as could be determined, however, no quantitative data on hangar conditions were then available. Harvey Hansberry (Ref. 1), current Vice Chairman of the Aviation Committee, states that he is unaware of any published hangar work. Three reports (Refs. 2, 3, 4) were found which dealt with the vapor envelope at tank vents during outdoor refueling. But since refueling in hangars is presently prohibited by NFPA Standard No. 407, they were inapplicable except for general information. It can only be assumed that the standards represent subjective judgements on the part of those involved.

High-volatility fuels (gasoline, JP-4, and Jet B) are still in sufficient use to warrant the application of appropriate standards. With low-volatility fuels (Jet A, JP-5, and JP-8), the hazard would be almost nonexistent.

Piston engines require a tailored gasoline fuel, while turbine engine fuel requirements are much less critical. JP-4 and Jet B are kerosene-gasoline blends, while Jet A, JP-5, and JP-8 are straight kerosenes. Since the problem is to determine what constitutes an appropriate standard in terms of the more hazardous fuels, the standard should be based on objective judgements resulting from quantitative measurements.

Both aviation gasoline (avgas) and military turbine fuel (JP-4) have flash points below 0°F. By definition, this is the lowest temperature at which, under controlled conditions, the vapor layer over the fuel reaches the LEL. The flash point is commonly determined by the closed cup method - ASTM D-56. Since normal hangar ambient conditions are invariably well above 0°F, it can be assumed safely that at the immediate liquid surface of any fuel spill or leak and at some finite distance above it, an explosive concentration can exist. Whether or not this would constitute a hazard depends upon many interrelated variables such as

- (1) the partial pressure of the volatile fuel components;
- (2) the volume and surface area of the exposed fuel;

- (3) air currents in the vicinity of the spill which may dilute the released fuel vapor; and
- (4) the time required for cleanup of spills or effective dissipation of volatile fractions.

From an engineering standpoint, any fuel spill involves a diffusion/evaporation process, and, if all the factors were known, equations could conceivably be written to characterize the phenomena. In actual practice, spills are not predictable in size and nature. Temperatures, irregular surface areas, rates of fuel release, and ventilation conditions vary so widely that about the only practical approach to hazard assessment is measurement of vapor concentrations in some worst-case situations.

All of the fuel vapors involved with the fuels mentioned are essentially butane-pentane-hexane mixtures that are several times heavier than air. It would be normal to expect the highest concentrations of flammable gases to build up at floor level or below it, with gradually decreasing concentrations at higher levels as the fuel vapors diffuse upwards or are diluted by air currents. This philosophy is the basis of the several electrical standards in use today which set various distances above the floor as zones in which explosion-proof equipment is mandatory. Such standards can be evaluated only from data on the horizontal and vertical distributions of fuel vapor and the concentrations reached at various times as the fuel evaporates and as vapors are dissipated by convection and diffusion.

There are a number of possible sources of fuel vapors in hangars. These are evaporation from the exposed surfaces of containers, accidentally spilled fuels, inadvertent losses during maintenance operations, leaks dripping onto the floor, and the displacement of vapors from aircraft tanks during thermal expansion or refueling. Once generated, the vapors could move by gravity flow or wind pressure differentials anywhere within the area of concern. Therefore, the overall protective scheme should be based on actually measured concentrations of vapors under representative conditions and should consider the costs of providing adequate protection against adverse situations. By simulation of drips and spills in a small-scale facility under controlled conditions and tests in actual operating hangars, it should be possible to secure useful data on the magnitude of the hazard exposure.

Protection may take a number of forms, and all may supplement each other. In aircraft hangars, an obvious approach is to establish operating practices which minimize the release of vapors. NFPA Standard No. 407 on aircraft fueling, which requires this to be done out-of-doors, is a step in this direction. This eliminates large-scale indoor vapor venting. The cited references 2, 3, and 4 deal with vapor venting.

The requirements of the two codes of interest are shown for an assumed hangar situation in Figure 1. Article 500 of the NEC, which governs hazardous areas in general, classifies them in three ways:

- Class I - flammable vapors in sufficient quantities to produce an explosive mixture
- Class II - combustible dusts
- Class III - easily ignitable fibers.

It should be noted that while the mere presence of flammable vapors could categorize aircraft hangars as Class I, the vapors must be produced in sufficient quantities to present a appreciable hazard. That is, the degree of exposure factor must be represented. If the hazard is continuous, intermittent, or periodic under normal operating conditions, it is described as Class I, Division 1. On the other hand, if the flammables are normally confined and the presence of vapors is the exception rather than the rule, the area is described as Class I, Division 2, and the electrical requirements are less rigorous.

When explosion-proof equipment is necessary, it must be suited to the specific vapors (or dusts) with respect to the maximum explosion pressures the fixture must be able to withstand and the allowable clearances which control flame stopping effectiveness. This requires a further classification by vapor properties as may be seen from reference to Table 500-2(c) of the NEC, included as Appendix 1 on page 32. Almost all flammable liquids, including petroleum fuels, fall into Class I, Group D (Div. 1 or 2). A few compounds used in aerospace work, especially UDMH, are in Class I, Group C. The presence of Group C liquids in hangars, however, is unlikely, and spills of such liquids in hangars are even less likely.

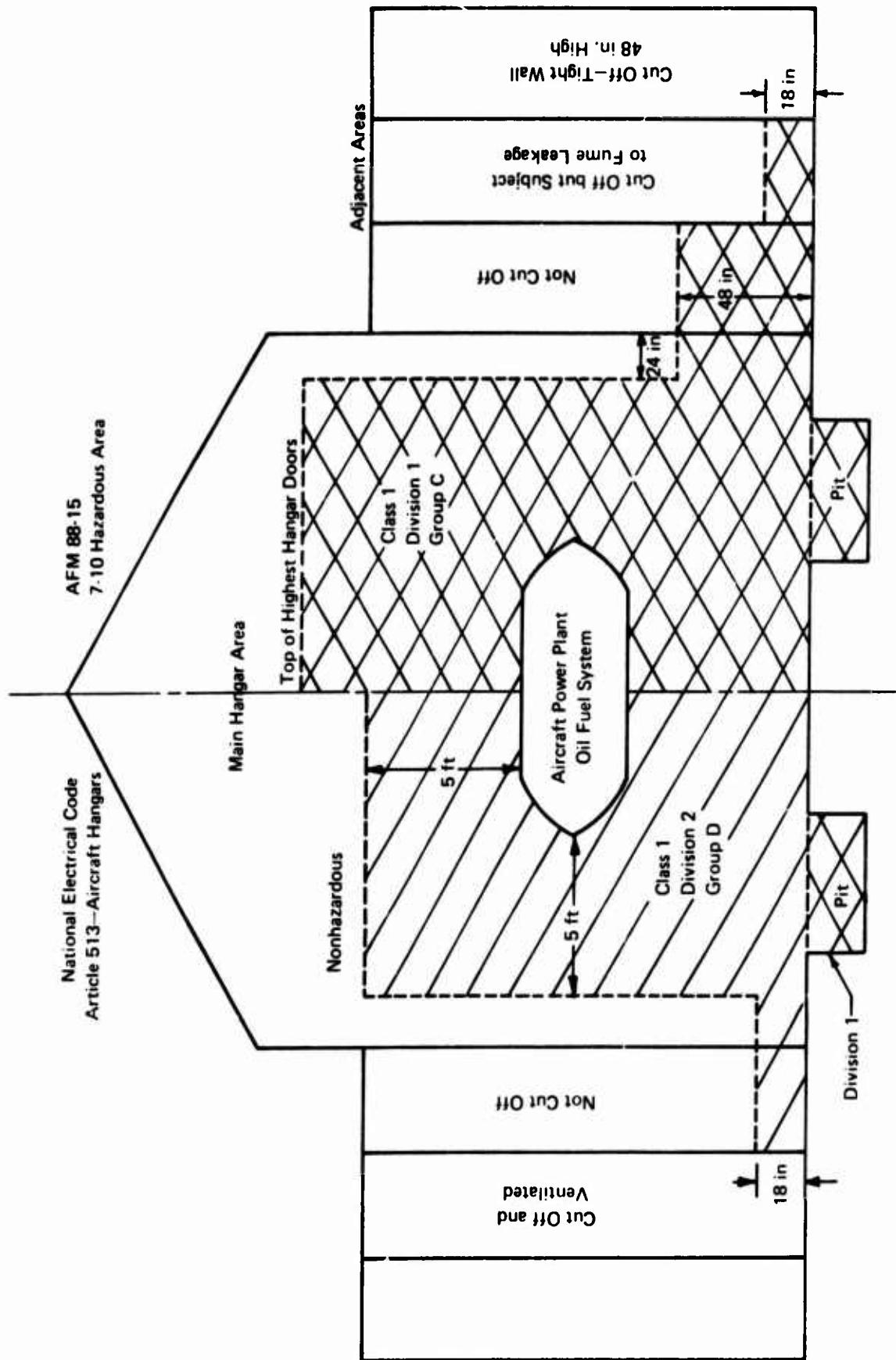


FIGURE 1. COMPARISON OF HAZARDOUS AREA DEFINITIONS BY ARTICLE 513
OF NATIONAL ELECTRICAL CODE AND AFM 88-15

It is very important that any heat-generating equipment selected for use in a hangar not produce a surface temperature high enough to cause auto-ignition of the particular fuel vapor under consideration. The revised National Electric Code states:

- (a) Approval for Class and Properties. Equipment shall be approved not only for the class of location but also for the explosion properties of the specific gas, vapor, or dust that will be present. In addition, equipment shall not have exposed any surface that operates at a temperature in excess of the ignition temperature of the specific gas vapor or dust.

The characteristics of various atmospheric mixtures of hazardous gases, vapors, and dusts depend on the specific hazardous material involved.

- (b) Marking. Approved equipment shall be marked to show the Class, Group and operating temperature, or temperature range, based on operation in a 40°C ambient for which it is approved.

The temperature range, if provided, shall be indicated in identification numbers, as shown in Table 500-2(b).

Identification numbers marked on equipment nameplates shall be in accordance with Table 500-2(b).

Exception: Equipment of the nonheat-producing type, such as junction boxes, conduit and fittings, are not required to have a marked operating temperature.

For purposes of testing and approval, various atmospheric mixtures (not oxygen enriched) have been grouped on the basis of their hazardous characteristics, and facilities have been made available for testing and approval of equipment for use in the atmospheric groups listed in Table 500-2(c). Since there is no consistent relationship between explosion properties and ignition temperature, the two must be regarded as independent requirements.*

There are appreciable cost differences between the various Group and Division ratings, and between explosion-proof and nonexplosion-proof equipment.

Explosion-proof equipment is more expensive than nonexplosive-proof equipment. For any particular installation wherein operations are well established (in this case, aircraft hangars), it is logical to gather quantitative data on the actual hazard exposure under the most adverse exposure conditions, allow a reasonable margin for any unknowns, and then determine the adequacy of existing safety measures. Accordingly, this research program was designed to provide firm data which could be used by USAF engineers to evaluate the requirements for explosion-proof electrical outlets in USAF aircraft hangars. Pertinent portions of Air Force Manual (AFM) 88-15 and the National Electric Code (NEC) are presented in Appendix I for convenient reference.

*1971-72 Revised National Electric Code, paragraphs 500-2(a) and (b).

SECTION III

TEST PROGRAM INSTRUMENTATION

1. INSTRUMENT PACKAGE DESIGN

The magnitude of any flammable vapor hazard can be exposed as a percentage of the LEL. If it is below the LEL, the mixture cannot be ignited. A mixture above the LEL must be considered dangerous. Even if the mixture is above the upper explosive limit (UEL), it may become diluted enough to fall within the explosive range.

There are two basic techniques for measuring vapor concentrations. One uses catalytic oxidation of the sample gas by a hot platinum filament to unbalance an electrical bridge circuit and produce a direct readout calibrated in percent of LEL. A portable instrument is available with a hand operated sample pump for quick checking of areas for hazardous gases. Multi-point devices of this design are available with built-in sampling pumps for permanent installation. If desired, special explosion-proof diffusion heads can make the measurement directly at the immediate sampling point. Without special calibration, the latter instruments cannot measure concentrations above the LEL. Common ranges available are 0 to 10 percent and 0 to 100 percent of LEL. Thus, these oxidation type devices were considered to have too limited a range for this program (except for checking purposes) since the range to be investigated was on the order of 0 to 200,000 ppm.

The most versatile instrument for measuring hydrocarbon vapor concentrations is the hydrogen flame ionization meter. This instrument has been available for many years, and its accuracy and stability are well established. Since it was recognized that the vapor concentrations in the test program could vary from extremely low values to well above the LEL and since quantitative results were needed, the ionization type meter was selected.

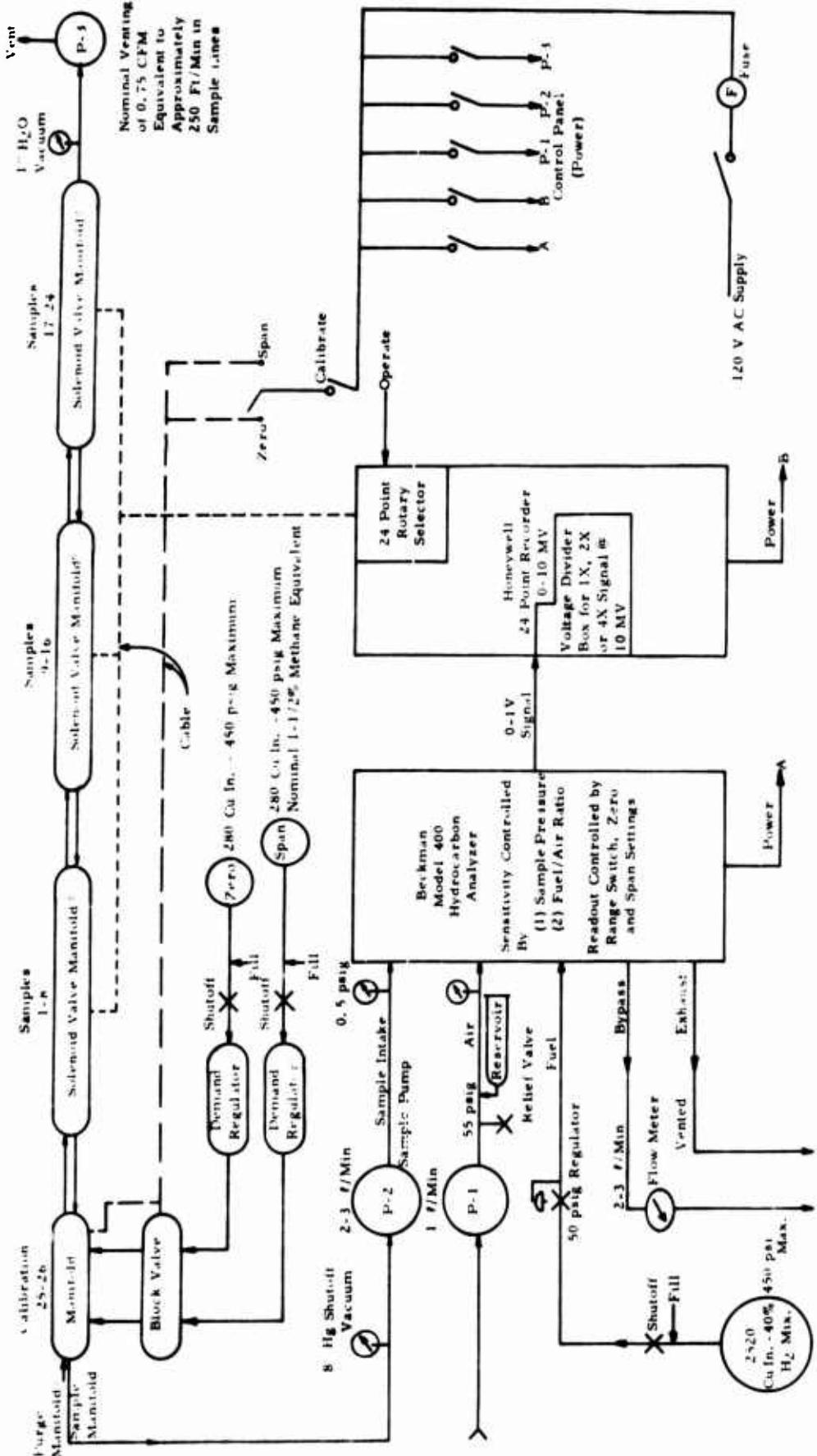
The instrument used had a stated useful range from 1 ppm full-scale to 100,000 ppm full-scale (based upon methane). These values were indicative but not limiting. The lowest range used during the program was 0 to 10 ppm of fuel vapor. The highest was 0 to 20,000 ppm of fuel vapor. Calibration to higher ranges would have been possible, but this was not necessary.

The original plan was to use two instruments. One was to be used to monitor ten fixed points, while the other was to monitor a scanner probe moving horizontally and vertically across selected planes in the simulated hangar space. This, however, would have greatly complicated data reduction and would have been poorly suited to the required full-scale hangar tests. After further study, it was decided to use a single instrument to monitor twenty-four fixed points placed in accordance with the needs of the experiment.

A 24-point Honeywell recording thermometer also was made available to the program. This was modified by the manufacturer to:

- (1) isolate the 24-point thermocouple selector switch from the measuring circuit and convert it to a 120-VAC rotary selector switch to control the sampling solenoids;
- (2) change the chart drive gear trains to print 12 points/in., regardless of time. This prevented overprinting of closely grouped data points;
- (3) provide readily changeable drive motors to enable sampling speeds between 5 and 30 sec/point as desired; and
- (4) calibrate the measuring circuits for 0 to 10 mV DC. To print out the signals from the fuel vapor measurements at each sample point.

An operational schematic of the instrument package is shown as Figure 2. The rotary switch on the Honeywell drive motor controls a bank of twenty-four 3-way solenoid valves. Normally each sample line (about 50 to 100 ft of 1/4-in. O.D. polyethylene tubing) was connected to a purge manifold, which exhausted a total of about 21 l/min from the system, keeping a continually fresh sample at the manifold. As each sample solenoid was activated in turn, the stream was switched to the sample manifold. The sample pump sent 2 to 3 l/min to a Beckman Model 400 Total Hydrocarbon Analyzer where it indicated the vapor content. The signal was then fed to the 24-point recorder through a small voltage divider box which enabled any reading to be multiplied by 2 or 4 for convenience in readout. At the conclusion of the sample period, the recorder printed an identified data point.



Three-way valves. Sample line normally connected to purge manifold (P-3) then to purging solenoid transfer stream to sample manifold (P-2).

FIGURE 2. INSTRUMENT PACKAGE SYSTEM DIAGRAM

The instruments, pumps, and sampling system were assembled into a standard 6-ft rack cabinet. The lower portion contained nine pressure tanks rated at 500 psig which could contain enough of the 40-percent hydrogen/60-percent nitrogen fuel gas mix for the Beckman Analyzer to support operation for over a week. It also contained a switch selectable tank of calibration gas and a tank of nitrogen for a zero gas. The instrument package is illustrated in Figure 3.

It was constructed for complete portability and ready movement to any selected test site. Allowing time for warmup of the instrument and running sample lines, a test could be started approximately 4 hr after arrival at the point of intended use.

2. CALIBRATION

Calibration of any instrument, such as the Beckman Model 400 Analyzer to read total volume of a mixture of hydrocarbon vapors, requires the determination of a typical analysis so that a reference gas can be prepared. Since the desired end product of the study was related to the LEL of aviation fuel vapors, advantage was taken of Zabetakis' (Ref. 5) work in this area. He points out that there is some disagreement on the flammability limit of fuel blends, but suggests these values:

<u>Fuel</u>	<u>LEL (Vol %)</u>
Avgas 100/130	1.3
Avgas 115/145	1.2
Jet Fuel JP-4	1.3

The LEL of a fuel vapor blend is related to the LEL of its various components, and the same reference cites these figures:

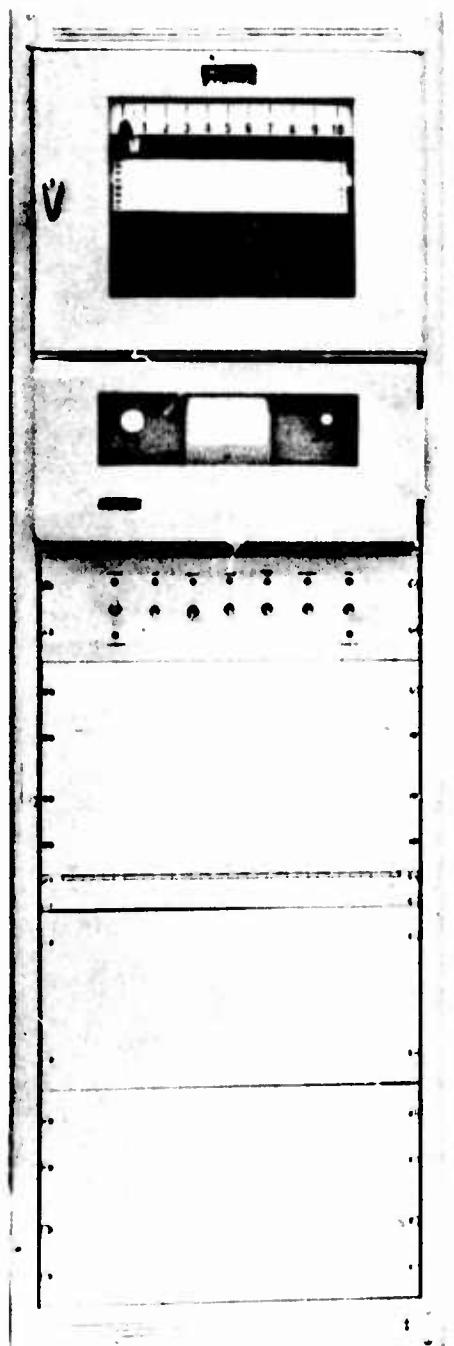
<u>Compound</u>	<u>LEL (Vol %)</u>
Methane	5.0
Ethane	3.0
Propane	2.1
Butane	1.8
Pentane	1.4
Hexane	1.2
Heptane	1.05
Octane	0.95

Cross plotting vapor LEL's with the number of carbon atoms involved (as shown in Figure 4), it may be seen that a typical aviation fuel spill would have an averaged LEL of approximately 1.5 percent, corresponding to a pentane/hexane mix with a median of 5.75 carbon atoms per molecule. The vapor would also contain relatively small amounts of butane and heavy ends. Some slight differences could be expected between the heavy ends from avgas and those from JP-4 by reason of the higher final boiling point of JP-4.

For the same volume percentage, an aviation fuel vapor would read 5.75 times higher on the analyzer than methane vapor. This fact was used in preparing the calibration gas. Methane was selected as the basic component gas since it would remain in the vapor state when stored and mixed at high pressures.

The calibration sample was prepared by charging 1-1/2 atm of methane to an evacuated pressure cylinder which was then pressurized by adding 100 atm of compressed air. This was equilibrated for 4 days with a steam coil and water coil on opposite sides of the cylinder to set up convection mixing currents. The contents were then analyzed on a Perkin-Elmer Gas Chromatograph against a reference sample prepared by injecting 10 ml of pure methane into a 1000-ml flask. Three runs on each gas, with run-to-run errors under 5 percent, showed the calibration gas contained 1.34 percent of methane.

In use, the gas was equivalent to 1.34 percent/5.75 percent or 0.233 percent of typical fuel vapor. As may be seen from Figure 2, a calibration gas cylinder was readily available at the input manifold. Before, during, and after each run, the instrument was set either to 10,000-ppm full-scale (2330 ppm) in calibration, or 20,000-ppm full-scale (1165 ppm) as required by the experiment.



Front

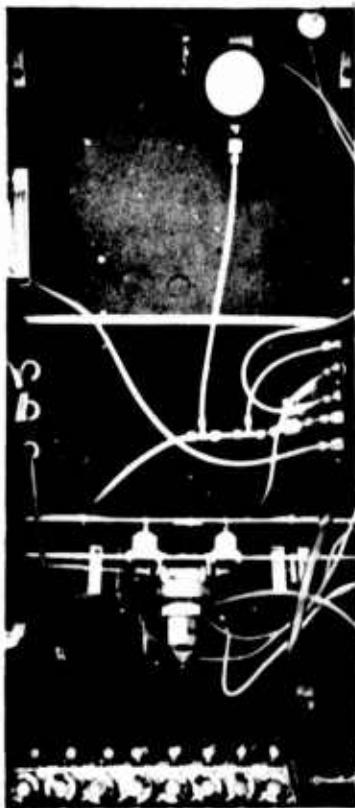
Recorder and
Sample Point
Selector

Analyzer
Section

Pump Deck

Manifold
Assembly

Fuel and
Calibration
Gas Storage



Back



FIGURE 3. PHOTOGRAPH OF INSTRUMENT PACKAGE

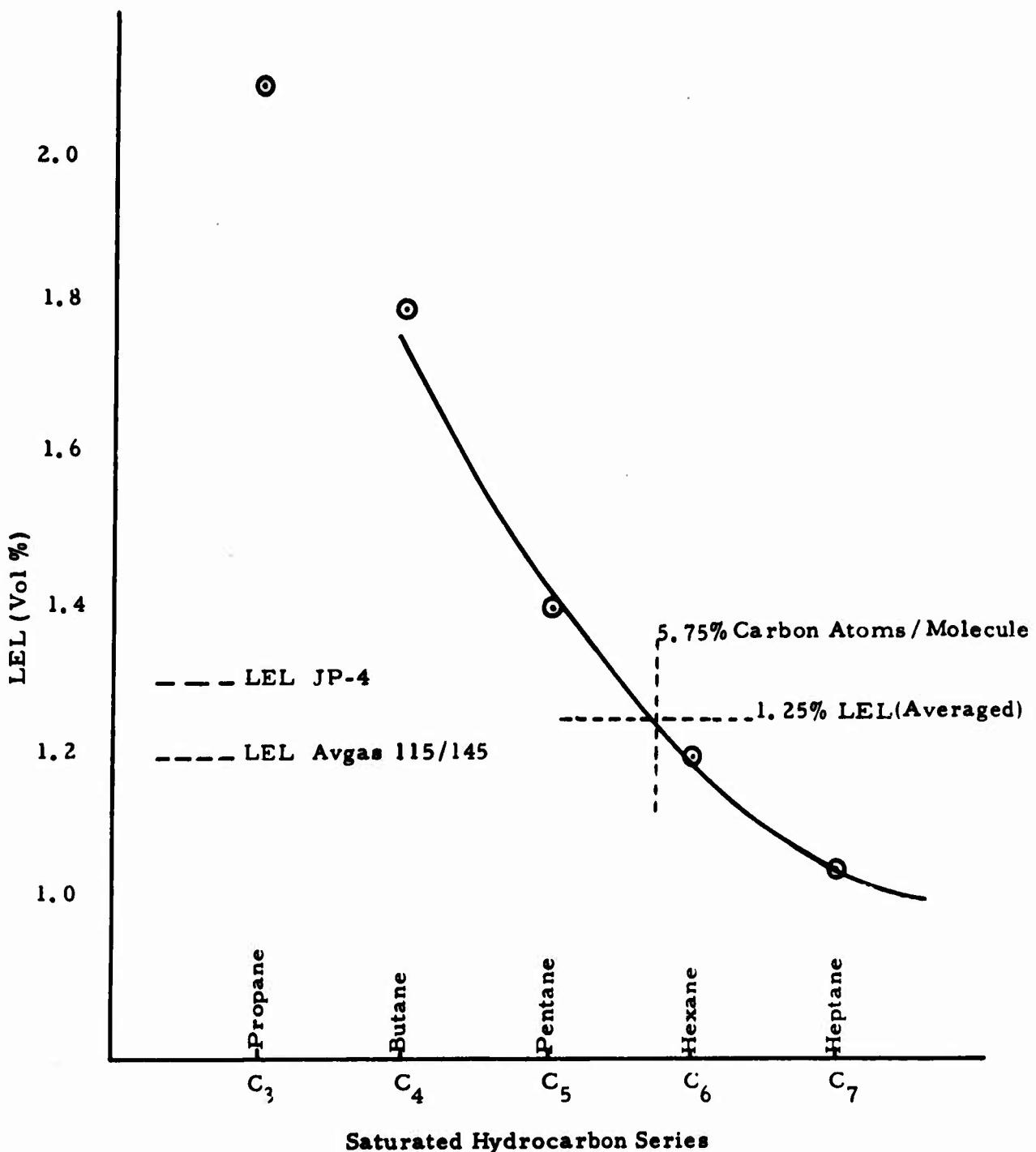


FIGURE 4. LOWER EXPLOSIVE LIMITS FOR FUELS AND VARIOUS SATURATED HYDROCARBONS

3. SAMPLING CONSIDERATIONS

For acceptable results, the sampling process must not affect the conditions being observed. The sample must be promptly analyzed, and, in a multipoint system, proper separations must be maintained. These criteria received continual attention during the program.

At no times were significant volumes being used for analysis. The sample and purge pumps continually removed approximately 1 cfm, and this was less than the air leakage in-and-out expectable in the 1600-cu ft enclosure involved. The samples were drawn parallel to the floor to avoid any effects on the vapor layer. No approach velocity could be noted above or below the sample point, and, even in the same plane, it was difficult to detect with a hot wire anemometer. Nevertheless, in the final vertical profile series when sampling at 1/2-in. intervals above the floor, a special stack was constructed to insure horizontal low-velocity laminar sampling.

The purge pump maintained a fresh sample at the manifold at all times. Calculations indicated that the typical lags between sample entry and arrival at the manifold were between 10 and 25 seconds.

For adequate separation between samples, the volume of the sample system must be minimized, and the flow must be made high enough to completely flush out the preceding sample before a new measurement is made. The initial shakedown runs showed obvious sample overlap when running at 5 sec/point. A speed of 7.5 sec/point was marginal if appreciable changes in vapor concentration occurred. Most of the work was carried out at 10 or 15 sec/point, except for the long duration runs in USAF hangars where 30 sec/point was deemed adequate. In addition, each sampling plan was based on graduated cycling from areas of high-vapor concentration to areas of low-vapor concentration and back again, avoiding abrupt changes in vapor values.

Sampling was under continual study during the program. During the latter phases, the instrument package was modified to reduce the original sample manifold volume from 9 cu in. to 1.5 cu in. and to meter the sample flow rate. With these improvements, an instrument response time of 5 sec/point was anticipated. The sample system performed as expected, but the recorder bridge balance circuit could not respond fast enough to make the 5-sec cycle feasible without further modifications. Excellent response was secured at 10 sec/point.

SECTION IV

TEST FACILITIES

The program required extensive testing in a simulated hangar space, a term which was not defined in the Statement of Work but was left to the interpretation of the contractor. It also specified field tests in USAF hangars selected as suitable to the purpose.

1. SIMULATED HANGAR SPACE

An aircraft hangar is essentially little more than a sizeable building designed for the storage and maintenance of aircraft. Large end doors are provided to permit passage in and out. Hangars are reasonably draft free, and, in temperate or cold climates, heaters are installed for working comfort. Aircraft shelters and nose docks meet this general description, also.

For the purposes of these tests, it was felt that as long as a semiquiescent environment could be secured, size (within reason) was not especially important. An unused concrete structure with a buildup joist roof was available which would supply a 14 X 14-ft working space and an adjoining 10 X 10-ft instrument room. This was rehabilitated for the purpose, and a floor plan is shown in Figure 5. An inside view of the experimental space is shown in Figure 6.

In order to investigate the effect of drafts coming from under a hangar door, a 4-in. plenum space was constructed across the inside east wall. This extended to within 2 in. of the floor and connected to two 18-in., low-capacity, tangential blowers set into the wall. Only one was used in testing. The second was utilized to expedite ventilation between tests. Typical velocities produced during tests are indicated in Figure II-1 of Appendix II.

A 4-in. low-power, shaded-pole fan was placed in one corner to produce floor drafts from ventilation inside the building. The velocities are noted in Figure II-3 of Appendix II.

For the first part of tests all sample lines were supported on ringstands. A plastic-covered, wire-grid system was then installed for mounting the polyethylene sample lines and securing better spatial distribution. Diagrams of the sample locations (Figs. II-1 through II-9) are included in Appendix II. Portable electric unit heaters were used prior to all runs at high-ambient temperatures to achieve the desired conditions.

2. SELECTED USAF HANGARS

A survey of the San Antonio area showed numerous hangars which could be made available to the program. The requirement essentially was for one or more large hangars which, on occasion, were filled with fueled aircraft and where vapor concentration measurements could be made over a 2- or 3-day period under closed door conditions. Three hangars were considered at Kelly AFB, four at Randolph AFB, and three at Bergstrom AFB. The final choices were Hangar 935 at Kelly AFB (Texas Air National Guard, F-100's); Hangar 5 at Randolph AFB (Air Training Command, T-38's); and Hangar 4337 at Bergstrom AFB (Tactical Air Command, RF-4's). The respective commands afforded excellent cooperation in making these hangars available and in aiding project personnel in setting up the instrument package. Randolph AFB officials were especially helpful in authorizing the desired large-scale spill test at the conclusion of the monitoring runs. Sketches showing sample points of the hangars and their aircraft occupancy are included in Appendix II. Figure 7 is a photograph of the aircraft in Hangar 5 at Randolph AFB during Test 26. The aircraft shown represented maximum hangar parking occupancy. The tests at Kelly AFB and Bergstrom AFB were conducted with maximum maintenance occupancy. The spill test at Randolph AFB is illustrated in Figure 8, while the Bergstrom tests are shown in Figure 9. The number and positions of aircraft in occupancy are shown as Figures II-6, II-7, and II-9 of Appendix II.

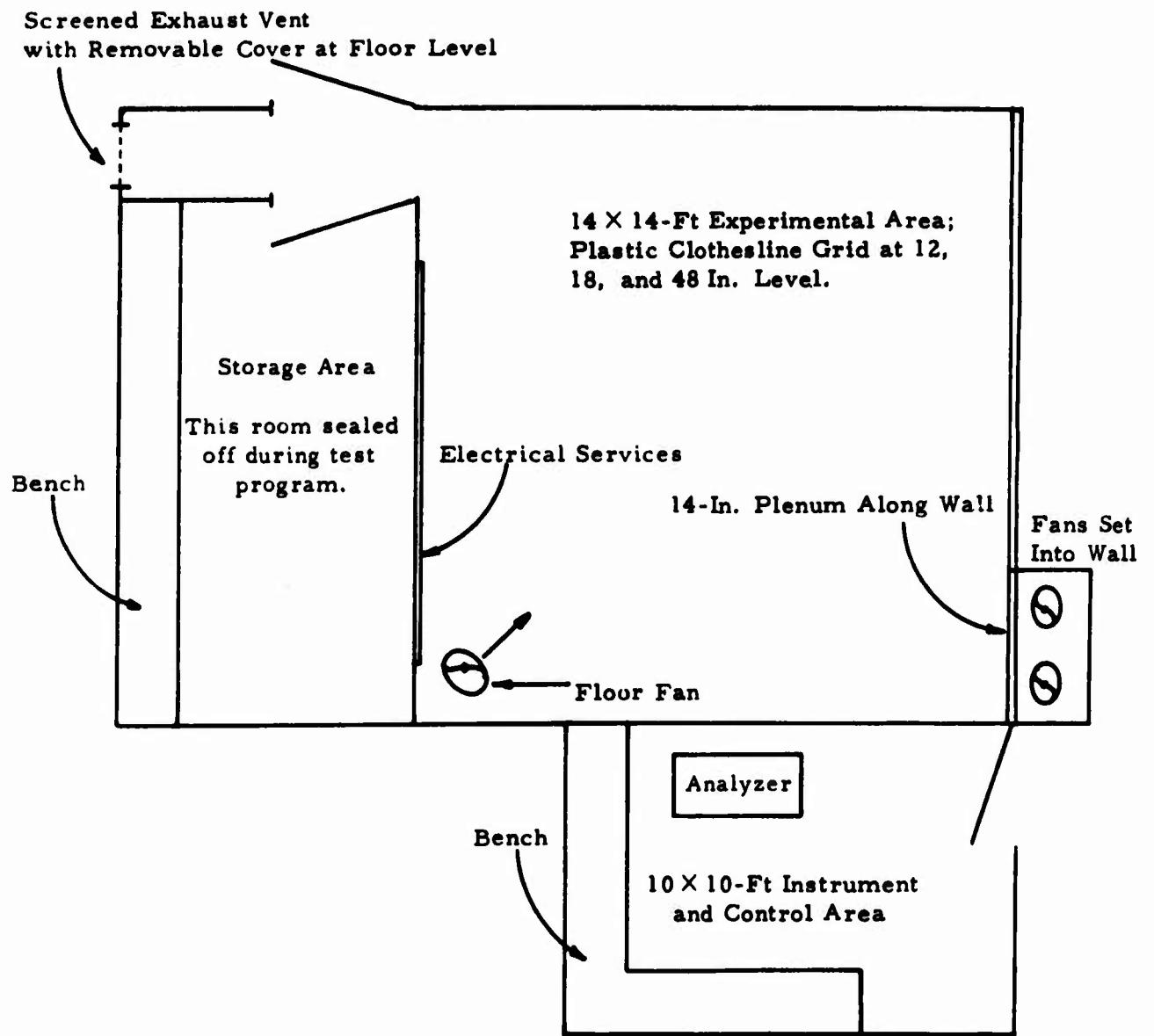


FIGURE 5. FLOOR PLAN—SIMULATED HANGAR SPACE

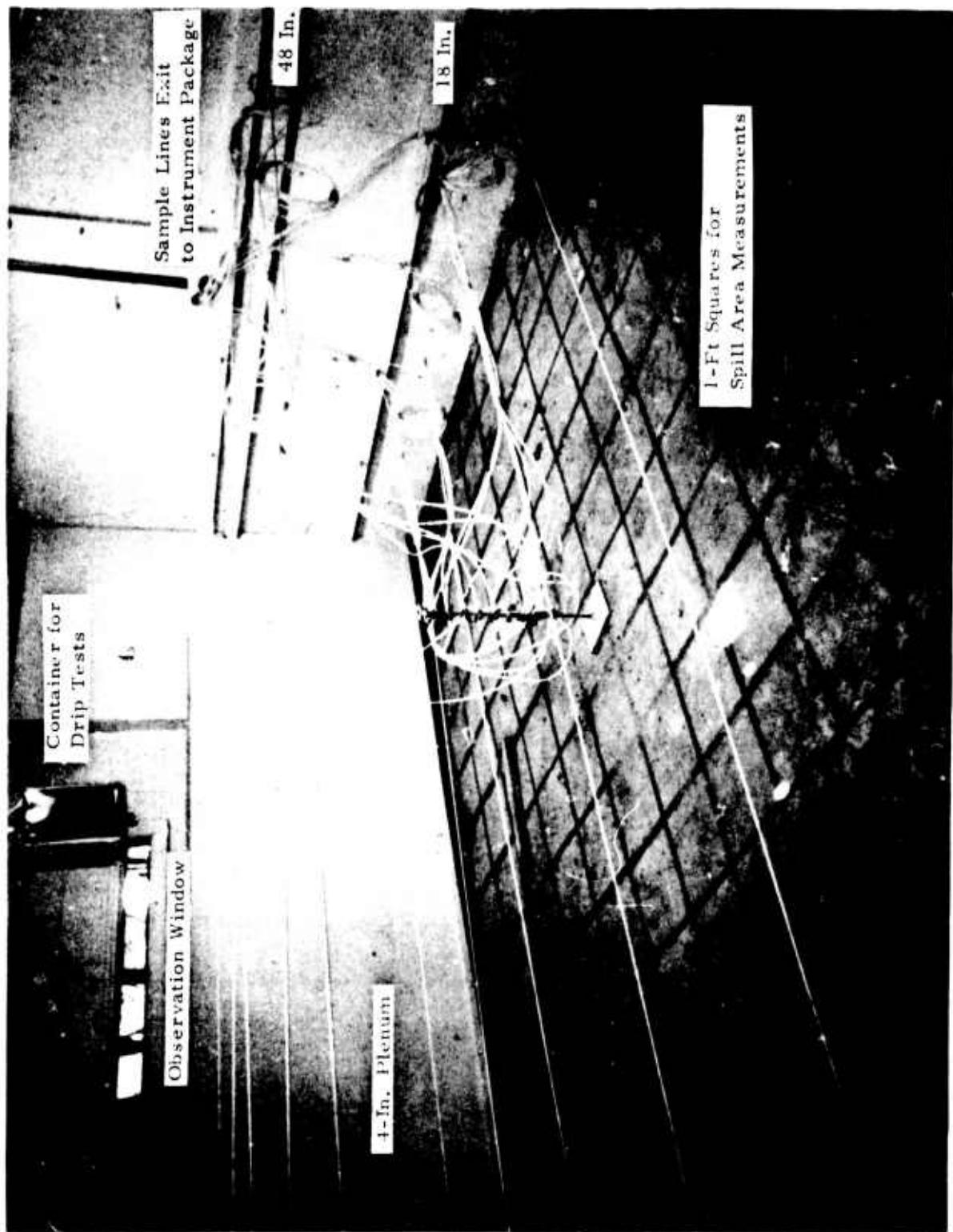


FIGURE 6. INTERIOR VIEW OF SIMULATED HANGAR SPACE

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FIGURE 7. VIEW OF HANGAR 5, AT RANDOLPH AIR FORCE BASE, DURING TEST 26



FIGURE 8. VIEW OF HANGAR 5, RANDOLPH AIR FORCE BASE SPILL TEST 27

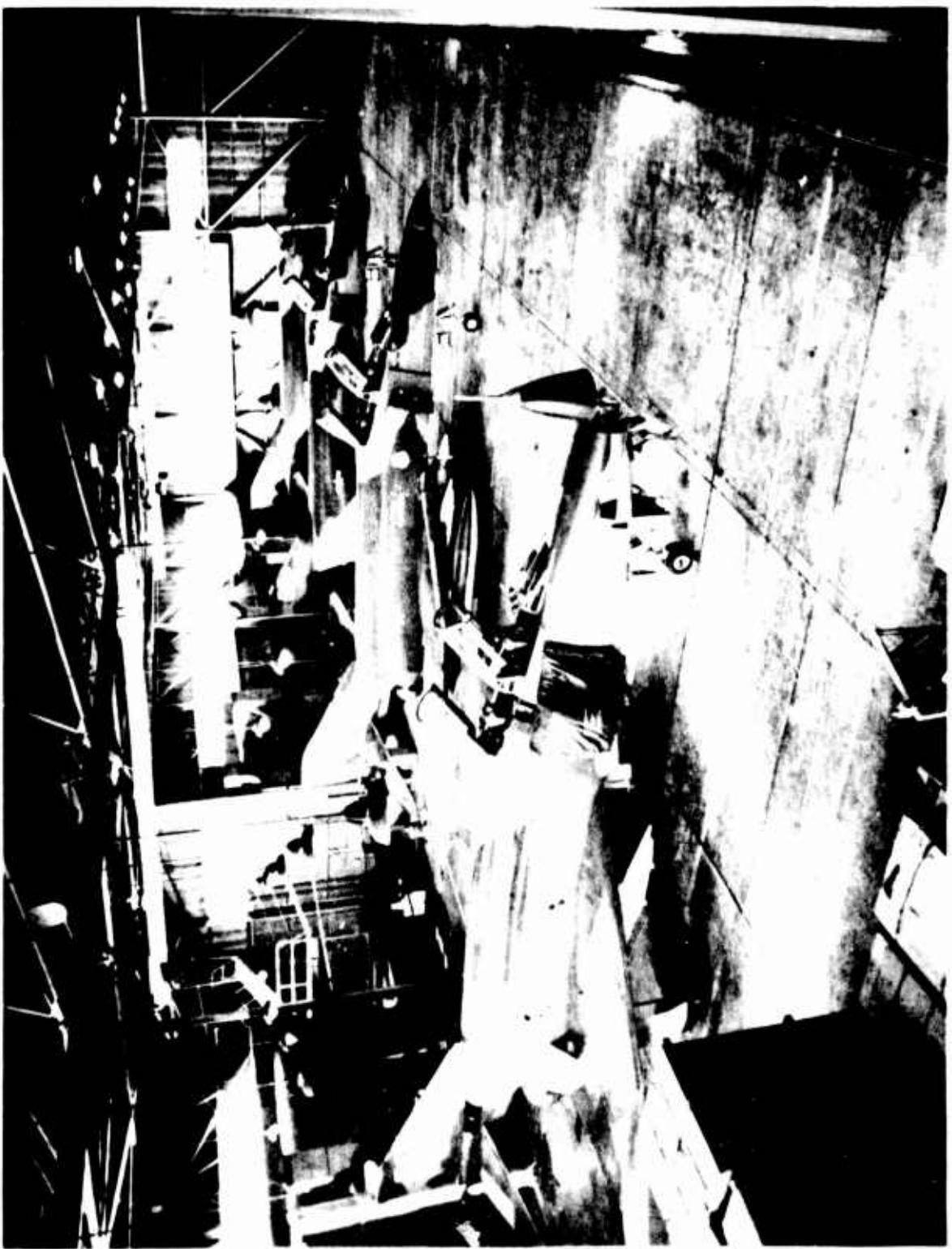


FIGURE 9. VIEW OF HANGAR 4337, AT BERGSTROM AIR FORCE BASE, DURING U.S.I. 28

SECTION V

TEST PROGRAM CHRONOLOGY AND TABULATED RESULTS

In the absence of any known information on the subject, the experimental approach was almost completely empirical. The test facility attempted to simulate actual conditions in actual buildings so as to determine what could be expected in USAF hangars under spill or leakage conditions. As the data from each run were collected, they were used to plan succeeding tests until the character of the vapor distribution pattern began to make itself evident and the relative importance of the variables could be discerned. This resulted in three separate but interrelated phases for the simulated hangars plus a fourth phase of field testing in actual hangars at USAF bases.

1. PHASE 1

Tests 1 through 5 were exploratory in nature, investigating the way in which vapor from an open pan would spread along a single vertical plane at 4 to 16 in. above the floor, starting above the pan in the center and extending toward the wall. It also measured the effect of dumping fuel on the floor and introducing floor drafts. The sampling plan appears in Appendix II as Figure II-1. The results are summarized in Table 1.

The Phase 1 data did not support previously held theories on vapor distribution and on the magnitude of the explosibility hazard. Accordingly, the recorded values were not considered acceptable until they had been checked and confirmed by an MSA Model 2A Explosibility Meter. Even though the facility provided an essentially draft-free, quiescent environment and no obvious air movements could be detected, it was concluded that some air currents did, in fact, exist which could dilute the vapor concentrations at the immediate liquid surface or divert rich mixtures away from the sample points.

2. PHASE 2

In the light of the Phase 1 results, the logical step was to increase the spatial coverage of the sampling and investigate vapor concentrations at significant levels between floor and ceiling. A support grid of plastic-coated wire simplified location of sample points at 2, 12, 18, and 48 in. above the floor and at the 96-in. ceiling level. Five locations were checked at each level. These were 2 ft from the walls at each corner, corresponding to the hazard area definition used in AFM 88-15, and in the center of the room.

Phase 2 work included a total of twenty-two tests with an ambient temperature range of 50°F to 98°F. Relative humidity was also recorded, but it was quickly apparent that humidity did not affect the results. Phase 2 results are summarized in Table 2.

While the Phase 2 work was in progress, it was learned (Ref. 6) that Eastman Kodak had been conducting a comparable program on various solvents, both in the laboratory and in a 20 X 40 X 15-ft plastic-covered, field facility. This work confirmed the importance of convection mixing currents in producing low vapor concentrations and the inapplicability of diffusion law theories. Accordingly, even though the quiescent air conditions in the facility appeared representative of typical installation, special efforts, including the use of smoke bombs to indicate air leakage, were made to secure a tight vapor seal. Test 19 and succeeding runs were made with the better sealed facility. These were essentially a repetition of Tests 10 through 14 and 17 to check the effect of possible air cross-currents and improve the validity of the earlier data. As may be seen by comparing the data of Table 2, higher maximum values were usually observed close to the floor in the sealed chamber, indicating that vapor leakage in an unsealed building can be appreciable. There were no significant differences at higher levels.

After consultation with the Project Monitor, the accumulated data were made available to Eastman Kodak for analysis and a conference arranged to compare the two programs. It was found (Ref. 7) that although the experimental approaches differed appreciably, the results were generally in good agreement. The Eastman Kodak work has not been completed, and no decision has yet been reached on publication.

3. PHASE 3

As the investigation proceeded, it became increasingly apparent that vertical profile information on vapor concentrations would be needed. While maximum values exceeding the LEL were occasionally noted at the 2-in. level, values were never

TABLE 1. MAXIMUM VAPOR CONCENTRATIONS IN A 200-SQ-FT CLOSED ROOM,
QUIESCENT CONDITIONS, SAMPLING IN A SINGLE PLANE

(LEL = 1.5 min ppm)

Test Parameters	Test Number				
	1	2	3	4a*	4b*
Fuel Vapor Source	avgas pan	JP-4 pan	avgas pan	avgas spill	avgas spill with exhaust
Wetted Area (sq ft)	6	6	5	35	35
Total Area (%)	3	3	2.5	17.5	17.5
Temperature (°F)	71	73	62	62	63
Vapor Concentration (ppm) at:					
16 In. Above Floor	1400	1100	730	3950	920
12 In. Above Floor	1600	1250	715	4100	950
8 In. Above Floor	1800	1240	665	4850	950
4 In. Above Floor	3350	2300	1000+	9750	900
Time to Reach Maximum (min)	24	72	114	24	n/a

*Tests 4a and 4b continue Test 3. Pan was dumped on floor. After peak concentration had been reached, air inlet fan was started.

**TABLE 2. MAXIMUM VAPOR CONCENTRATIONS IN 200-SQ-FT CLOSED ROOM,
QUIESCENT CONDITIONS, SAMPLING IN THREE VERTICAL PLANES**

Test Parameters	Test Number									
	0	7	8	9	10	11	12	13	14	
Fuel	avgas	JP-4	avgas	JP-4	JP-4	avgas	avgas	avgas	JP-4	
Vapor Source	pan	pan	2-gal drip	2-gal drip	4-gal drip	4-gal drip	4-gal spill	4-gal spill	4-gal spill	
Wetted Area (sq ft)	5	5	10	10	30	30	98	96	98	
Total Area (%)	25	25	5	5	15	15	49	48	48	
Temperature (°F)	60	75	72	54	71	79	52	98	95	
Vapor Concentration (ppm) at:										
46 In. Above Floor	520	455	2,700	850	800	1,100	2,500		2,700	
48 In. Above Floor	840	620	2,800	1,050	950	1,450	3,300	7,300	2,900	
16 In. Above Floor	790	665	3,450	1,050	1,050	1,850	5,200	9,200	3,200	
12 In. Above Floor	920	750	3,700	1,000	1,050	1,900	7,000	10,000	4,400	
2 In. Above Floor	10,000+	2,050	10,000+	3,700	5,100	9,450	20,000+	19,800	20,000+	
Time to Reach Maximum (min)	10	4	34	282	60	258	3	3	4	
Test Parameters	Test Number									
	15	16	17	18	19*	20*	21*	22*	30*	
Fuel	avgas	avgas	JP-4	JP-4	JP-4	JP-4	JP-4	JP-4	JP-4	
Vapor Source	4-gal spill	10-gal spill	4-gal spill	10-gal spill	4-gal spill					
Wetted Area (sq ft)	98	156	98	176	98	98	98	98	98	
Total Area (%)	49	73	49	88	49	49	49	49	48	
Temperature (°F)	52	60	50	64	67	67	61	77	82	
Vapor Concentration (ppm) at:										
46 In. Above Floor	2,400	1,700	1,600	1,800	2,900	1,600	4,400	1,500	1,750	
48 In. Above Floor	2,600	1,600	1,500	2,800	2,700	1,200	4,300	1,000	1,900	
16 In. Above Floor	3,600	1,800	1,800	2,300	6,700	5,800	7,400	2,500	5,650	
12 In. Above Floor	4,600	3,500	1,550	3,900	10,100	7,800	10,200	4,300	8,700	
2 In. Above Floor	20,000+	20,000+	10,200	20,000+	20,000+	20,000+	20,000+	20,000+	20,000+	
Time to Reach Maximum (min)	6	7	11	7	3	7	7	7	3	
Test Parameters	Test Number									
	30**	31*	31**	32*	32**	33*	33**			
Fuel	avgas	JP-4	JP-4	avgas	avgas	JP-4	JP-4			
Vapor Source	floor fan	4-gal spill	floor fan	4-gal drip	floor fan	4-gal drip	floor fan			
Wetted Area (sq ft)	96	96	94	38	25	35	25			
Total Area (%)	48	48	47	18	12.5	17.5	12.5			
Temperature (°F)	82	89	89	90	90	85	85			
Vapor Concentration (ppm) at:										
46 In. Above Floor	1,250	275	125	3,500	585	2,000	1,700			
48 In. Above Floor	1,900	350	350	5,900	640	3,300	2,300			
16 In. Above Floor	1,900	450	450	7,600	675	4,300	3,075			
12 In. Above Floor	1,900	550	475	8,850	695	5,400	3,050			
2 In. Above Floor	2,250	10,150	2,750	20,000+	930	20,000+	13,000			
Time to Reach Maximum (min)	---	33	---	55	---	68	---			

*Extra care taken in sealing room.

**Small fan on floor in corner aimed at center to simulate floor drafts.

Note: Values shown as 10,000+ and 20,000+ were slightly over range of instrument but did not warrant a change in scale.

Values are short time maximums. Duration may be obtained from data plots or tables in Appendixes III and IV.

See configurations II-2 and II-3 for sampling details.

observed at the next level, 12 in. above the floor, nor at the 18-in. level used in NEC Par. 513, nor at the 48-in. level used in AFM 88-15 to define the hazard zone. Tests 23 and 29 measured the vertical profiles for JP-4 and avgas spills at 2-in. intervals up to 24 in. above the floor in a sealed environment. As may be seen from the data of Table 3, the LEL could exist at 4 and 6 in. above the floor. Additionally, Tests 34 through 37 were run to examine the profile in more detail, sampling at 1/2-in. increments. Since the lowest points were close enough to the liquid surface of the spill so that surface conditions could be affected by sampling, extra care was taken through the use of a laminar flow, low-velocity sampling deck. The results of the Phase 3 tests are plotted in Figure 10 which shows that even when plotting short time maximums in a nontypical sealed environment, the actual hazard zone for the most volatile fuel was less than 8 in. above the floor.

4. ALL-PHASE WORK

Repeated checks were made of the effects of movements at floor level. It had been noted in Phase 1 that if project personnel entered the test chamber and walked across the room, the vapor concentration temporarily dropped at the 4-in. level. Tests 4b and 5 documented the air movement effect when a draft was simulated under the hangar door. The cross floor velocity was approximately 75 ft/minute. Air movement was again investigated during Tests 30 through 33, when a 4-in. flow fan was operated for a short time during the test. The location of the fan and air velocities are shown in Figure II-3 of Appendix II. In every case, any disturbance of the air at floor level immediately reduced the vapor concentration until the movement was stopped, at which time it gradually returned to near its previous equilibrium value.

5. PHASE 4

The required field tests in USAF hangars were planned on the basis of information from Phases 1, 2, and 3. Since the observed vapor concentrations had been so low in the small sealed test facility, it appeared that meaningful results in large open area hangars could be secured only in worst-case situations such as with tightly closed doors, maximum fueled aircraft occupancy, and conditions when fuel leaks or drips could occur.

Hangar doors are normally open during operations. A survey was taken, however, which revealed weekend periods for some hangars at Kelly AFB, Randolph AFB, and Bergstrom AFB during which "worst-case" tests could be run. The aircraft involved were the F-100, T-38, and RF-4. With the complete cooperation of all three Air Force Commands, weekend monitoring tests were set up at the three bases. These were designated as Tests 24 through 28. The sampling plans are shown in Figures II-6, II-7, and II-9 of Appendix II, while the results are listed as Table 4.

The large-scale spill test, which was to be run if a suitable facility could be obtained, was carried out as Test 27 at Randolph AFB, after conclusion of the monitoring tests. Hangar 5 was cleared of aircraft, and the doors were closed. The floor area, including two adjacent shops, was covered with sample lines as shown in Figure II-8 of Appendix II. The floor drains were sealed. With the Base Fire Department standing by to observe and monitor, a drum of JP-4 fuel was dumped on the floor. The test ran approximately 2-1/2 hr, after which the doors were opened and the floor washed down. The data for this test appear in Appendix IV as Table IV-27. Fire Department checks with a MSA Model 2A Explosibility Meter showed values at or above the LEL only at the immediate liquid level in a single low spot of the floor at the drain.

6. DATA REDUCTION

A total of 124,122 data points were recorded during this study covering some 600 hr of test operation. The tabulated data for each run are included as Appendix IV. To visualize better the physical relationships, the runs in the test facility have been plotted against time for various heights above the floor and are included as Appendix III. From these curves, it may be seen that the maximum vapor concentration values are of relatively short duration. Except close to the floor, the vapor explosibility hazard is essentially nonexistent.

No effects could be noted that related to barometric pressure or humidity. Theoretically, pressure or humidity would be relevant only if diffusion theory had been shown to be controlling, which was not the case.

In the same manner, the hazard differences between avgas and JP-4 fuels for spill conditions with limited amounts were not significant, nor was the temperature. Avgas and JP-4 are both essentially high-volatility fuels as far as flash point is concerned. Their volatile fractions are almost the same. The primary difference between these fuels is the amount per gallon of each fuel that will readily evaporate in a given length of time. Differences in ambient temperature vary the thermal driving force which is measured from the below-zero ($^{\circ}$ F) flash point. At elevated temperatures, the volatile fractions of both fuels

TABLE 3. VERTICAL PROFILES OF MAXIMUM VAPOR CONCENTRATIONS IN SEALED ROOM

Test No.	Fuel	Type	Area (sq ft)	Area (%)	Temp (°F)	Height Above Floor (in.)	23		29		34		35		36		37	
							JP-4	4-gal spill	avgas*	4-gal spill	avgas	4-gal spill	JP-4	avgas	4-gal spill	JP-4	avgas	4-gal drip
			9.4	-	-	24	1200	1300	-	-	-	-	-	-	-	-	-	-
			4.7	-	-	22	1300	1500	-	-	-	-	-	-	-	-	-	-
			6.2	-	-	20	1700	2900	-	-	-	-	-	-	-	-	-	-
			1.8	-	-	18	1700	3300	-	-	-	-	-	-	-	-	-	-
			1.6	-	-	16	1300	3900	-	-	-	-	-	-	-	-	-	-
			1.4	-	-	14	1600	4700	-	-	-	-	-	-	-	-	-	-
			1.2	-	-	12	1500	5200	-	-	-	-	-	-	-	-	-	-
			9.5	-	-	11.5	-	-	8100	8600	4300	5900	4400	5800	7400	7400	7400	7400
			9.0	-	-	11.0	-	-	8300	9000	4400	5900	5400	6200	7600	7600	7600	7600
			8.5	-	-	10.5	-	-	7100	8900	5900	6300	6300	6400	7800	7800	7800	7800
			8.0	-	-	10.0	1900	-	10000	10000	6200	6200	6700	6400	8100	8100	8100	8100
			7.5	-	-	9.5	-	-	9800	10800	10800	10600	7300	7100	6700	6700	6700	6700
			7.0	-	-	7.0	-	-	11600	11600	11600	11600	7600	7400	7400	7400	7400	7400
			6.5	-	-	6.5	-	-	11700	11700	11700	11700	7900	7900	9000	9000	9000	9000
			6.0	-	-	6.0	-	-	12400	12400	12400	12400	8200	8100	9300	9300	9300	9300
			5.5	-	-	5.5	-	-	12700	12700	12700	12700	8500	8600	8800	8800	8800	8800
			5.0	-	-	5.0	-	-	13400	13400	13400	13400	8800	8900	9800	9800	9800	9800
			4.5	-	-	4.5	-	-	14100	14100	14100	14100	10100	10100	10600	10600	10600	10600
			4.0	-	-	4.0	-	-	14900	14900	14900	14900	10900	10900	11200	11200	11200	11200
			3.5	-	-	3.5	-	-	14900	-	-	-	11100	11100	11300	11300	11300	11300
			3.0	-	-	3.0	-	-	15900	-	-	-	10500	10500	11600	11600	11600	11600
			2.5	-	-	2.5	-	-	16000	16000	16000	16000	10600	10600	12100	12100	12100	12100
			2.0	-	-	2.0	-	-	16600	-	-	-	11900	11900	12300	12300	12300	12300
			1.5	-	-	1.5	-	-	16700	-	-	-	11000	11000	12600	12600	12600	12600
			1.0	-	-	1.0	-	-	18400	-	-	-	12200	12200	13800	13800	13800	13800
			0.5	-	-	0.5	-	-	-	-	-	-	-	-	-	-	-	-

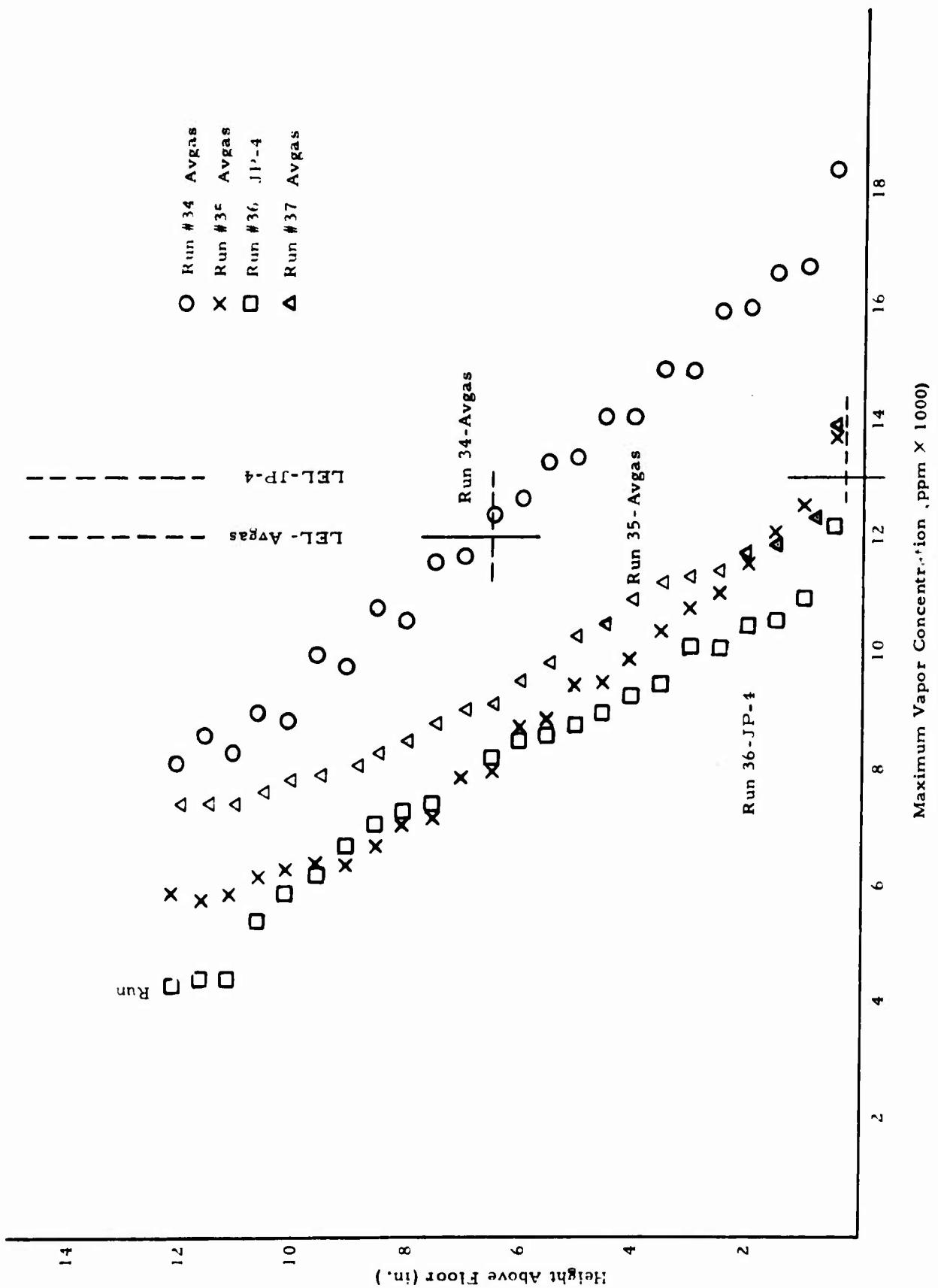


FIGURE 10. VERTICAL PROFILES OF VAPOR CONCENTRATION, TESTS 34-37

TABLE 4. MAXIMUM VAPOR CONCENTRATIONS IN SELECTED TYPICAL USAF HANGARS

	(I.E. 1:500 ppm)					
Test No.	24	25	26	27	28	
Fuel	JP-4	JP-4	JP-4	JP-4	JP-4	JP-4
Type	monitor	monitor	monitor	55-gal spill	monitor	
Location	Kelly AFB	Kelly AFB	Randolph AFB	Randolph AFB	Bergstrom AFB	
Aircraft	F-100	F-100	T-38	None	RF-4	
Temperature (°F)	65	65	65	57	46-66	
Vapor Concentration (ppm) at:						
18 In. Above Floor	NA	NA	NA	1175	NA	
10 In. Above Floor	NA	NA	NA	1755	NA	
2 In. Above Floor	40	26	24	2660*	1000+**	
Length of Run	45 hr 30 min	118 hr 30 min	63 hr 18 min	3 hr 48 min	61 hr 36 min	

*Maximum value in two adjoining rooms, door closed, was 340 ppm at 35 min.

**Maximum value was recorded 6 in. from 2 X 4 ft X 3-in. pan catching dripping JP-4 from wing tank fuel expansion. Typical maximums in other areas were 50 ppm or less.

would evaporate more rapidly and be dissipated sooner. That is, the vapor concentrations reached would be strongly affected by temperature differences within the room. The temperature differences also act as the driving forces for the diluting convection currents within the room.

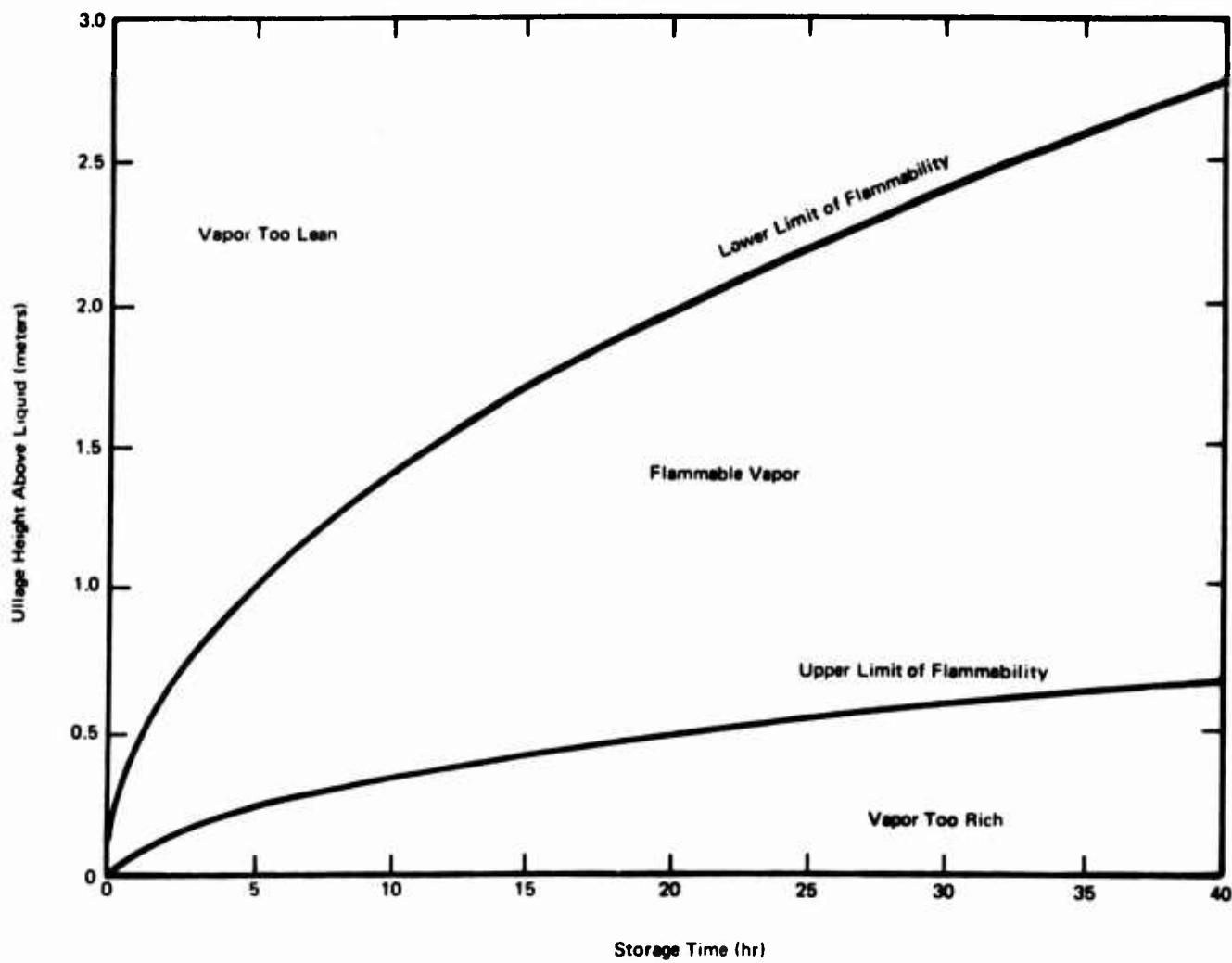
SECTION VI

ANALYSIS OF RESULTS AND CONCLUSIONS

I. DISCUSSION OF THE TEST RESULTS

At the outset of the program, it was expected that spills and leaks in aircraft hangars would follow a general pattern predictable from classical diffusion theory. If this were true, then for any given time after a spill, it would be possible to calculate the accumulated vapor build-up from the floor, up to any level.

An example of such a theoretical calculation for benzene is shown as Figure 11 (Ref 8). Zabetakis (Ref 5) gives 1.3 percent and 7.9 percent, respectively, for the LEL and UEL values of this material. These are about the same as for aviation fuel vapors so that the chart for such spills would be comparable.



Source: Ref 8.

FIGURE 11. CALCULATED DIFFUSION OF BENZENE INTO AIR

These calculations assumed an unlimited supply of the pure compound, an isothermal environment, and only molecular diffusion forces to accomplish the liquid-vapor-air mixing process. Such assumptions are completely unrealistic for the spill of some definite quantity of an aviation fuel, consisting of a blended hydrocarbon mixture in a building where floor-to-wall-to

ceiling temperature differences set up small but appreciable convection currents. Also, it has been believed that after any spill, the rapid flashoff of volatiles would create a rich vapor which would drift or be moved by convection currents, essentially undiluted, toward potential ignition points. Obviously, such a condition could be hazardous and would justify establishment of appropriate safety standards.

None of the experimental work conducted in this program supported this rich cloud concept. They did show that under extreme spill conditions in a small confined area, the vapor concentration could gradually build up and approach the LEL in a layer as high as 7 in. above the floor. The general vertical profile of maximum observed values, irrespective of time reached, is illustrated in Figure 10. It was also noticed that for any spill in a quiescent environment where the fuel collected in small pools on a rough concrete floor, a value near the LEL at the 1/2-in. level could continue for several hours. In the laboratory facility, maximum values slightly over 20,000 ppm were recorded at the 2-in. level on numerous occasions, but these could not be produced at will. Low-velocity convection currents produced by floor-wall-ceiling temperature differences appeared to be the controlling factor. Any disturbance causing air movement, regardless of how produced, caused dissipation of rich vapors and lowering of concentrations. As previously pointed out, the effect was noticeable whenever project personnel entered the chamber causing some air movement during a run. This was documented several times.

The concentrations observed in the confined test facility do not necessarily apply to typical USAF hangars with their large open areas where both convection currents and cross ventilation from external wind pressures can quickly sweep away and dilute fuel vapors to safe levels.

In Test 27, the open floor fuel spill at Randolph AFB, none of the readings at the 2-in. level exceeded 2660 ppm (21% of LEL), even at the edges of the spill. Scanning with an MSA Explosimeter showed readings above the LEL only at the immediate fuel surface in a low spot on the floor. The rich vapor layer, if any existed, could not be found as high as 1/2 in. off the floor. Under such conditions, it would not be logical to expect vapor travel along the floor into the adjacent hangar offices and shops, where none was detected.

A comparable effect was noted during Test 28 at Bergstrom AFB, when the area beside a 2 X 4-ft pan receiving JP-4 from a dripping RF-4 fuel tank never exceeded 1000 ppm (8% of LEL) at the 2-in. level.

The mass of data gathered in this study indicate that the overall mechanism is one in which the generation of vapor is evaporation-rate limited. That is, it is controlled by the ambient temperature and the vapor pressures of the volatile compounds in the fuels spilled.

The vapor concentrations in the spill area are determined by an equilibrium between the quantity of vapor evolved and the rapidity with which it is swept away and diluted by air currents. Classical diffusion theory, as such, does not apply under these conditions. Comparable results were obtained by Eastman Kodak in the previously cited work (Ref 7).

The data also indicate that most environmental factors have relatively little effect upon the results. Ambient temperature, barometric pressure, and relative humidity were found to be irrelevant. The differences between avgas and JP-4 were not appreciable. Both are high-volatility fuels and act in much the same manner. With any straight kerosene low-volatility fuel (such as JP-5, JP-8, or Jet A), the estimated hazard zone would appear to be well under the 2-in. level. A high degree of confinement and a volatile fuel can raise the hazard zone up to approximately 6 to 7 in. above the floor. Under such conditions, there is little or no justification for some protective techniques such as vapor seal barriers or pressurizing areas to prevent inward vapor flow.

Any device to produce positive air movement at floor level will immediately reduce the vapor concentration at the floor to a low level. This was demonstrated in Test 4B and again in Tests 30 through 33. For any confined area subject to spills, the use of an exhaust fan taking suction at floor level would be a logical and effective safety measure.

The objective of this research effort was to determine the extent of hazardous concentrations of explosive vapors in aircraft hangars in order to define areas which require explosion-proof electrical wiring and equipment. From the values shown in Figure 10 for a confined area, which is in itself an extreme situation, it can be seen that the nonhazardous area for hangars could be established as beginning at 12 inches above the floor and still retain an adequate margin of safety. This conclusion is supported by the results of actual tests in USAF hangars.

In the absence of measuring equipment, a strong smell of fuel vapors tends to alert personnel to the possible existence of an explosion hazard. It was noted again and again that such smells could exist at concentrations as low as 50 ppm—far below the LEL. The light petroleum vapors which constitute the hazard are odorless. The residual sulfur components which can be detected by the nose are no index as to the vapor concentration and can lead to highly erroneous conclusions as to the degree of hazard.

2. CONCLUSIONS

Presented in order, the following conclusions have been reached during the progress of the study:

- (1) Any spill or leak of a flammable liquid in a hangar can represent a fire hazard consistent with the amount released. The overall vapor explosibility hazard is low, of relatively short duration, and confined to a space only a few inches above the floor.
- (2) Even with the use of the most volatile fuels and spills covering up to 38 percent of the floor area, the expected vapor concentration was below the LEL at the 12-in. level. Thus, ordinary sized spills or leaks, representing up to 25 percent or more of the floor area, do not represent a serious vapor explosibility hazard. Ordinary washdown procedures not only reduce the fuel present but supply vapor mixing and dilution as well.
- (3) There appears to be little practical difference between avgas and JP-4 in their vapor hazard aspects except that avgas has a higher volatile content. Avgas can be expected to vaporize more rapidly and reach a somewhat higher short period peak vapor concentration within the 12-in. distance.
- (4) Fuel evaporation rate is temperature dependent. As the ambient temperature is increased, vapor is released more rapidly, and the available volatiles are dissipated in less time. There appears to be no significant effect on vapor concentrations within normal hangar temperature ranges. Humidity and barometric pressure are insignificant factors in the evaporation process.
- (5) Since normal convection currents in hangars already serve to dilute and dissipate vapors (keeping them below the LEL at working levels), the effect of hangar door cracks and openings is not significant, except to further improve ventilation and decrease vapor concentrations.
- (6) No penetration of vapors through closed doors or wall openings into adjoining areas was observed during the spill test at Randolph AFB. There was an intervening 3-in. sill between the spaces, and blocking of the high concentrations expectable along the floor could have been due either to this low barrier or to dissipation of the vapor by convection currents before it reached the wall.
- (7) Inasmuch as no penetration of vapors into adjacent unpressurized areas could be observed, there is no justification for pressurizing to block vapor flow.
- (8) Experiments investigated the action of a floor level fan and showed it to be extremely effective in lowering vapor concentrations. This is a mixing and dissipating action and does not require the vapor to be exhausted from the building.
- (9) Reviewing the provisions of Paragraphs 7 through 10 Hazardous Areas, of AFM 28-15 in the light of the test program and the preceding conclusions, it appears that a redefinition of the hazards is warranted.

3. RECOMMENDED REVISED TEXT FOR PAR 7-10, AFM 88-15

The following is recommended as a revision of AFM 88-15:

7-10. Hazardous Areas:

a. *Requirements.* Unless otherwise authorized, wiring materials and equipment within hazardous areas shall conform to the requirements for the particular hazard involved as specified in the National Electrical Code.

b. *Hangars and Docks:*

(1) All spaces below grade shall be considered to be Class 1, Division 1, Group D of hazardous locations.

(a) The entire area of the hangar, including any adjacent and communicating areas not suitably cut off, shall be considered to be Class 1, Division 2, Group D hazardous locations up to a level 12 in. above the floor.

(b) Where docks and hangars are used for fuel system and fuel cell repairs, the above criteria are applicable provided that any other special treatment requirements are also met.

(c) Wiring and equipment in nonhazardous areas shall meet the requirements of the National Electrical Code.

(d) Adjacent areas cut off at floor level by a barrier not less than 3-ft high are considered nonhazardous unless the usage of the area is hazardous.

c. *POL Areas.* All spaces below grade shall be considered Class 1, Division 1, Group D hazardous areas. The following spaces shall be considered Class 1, Division 2, Group D hazardous areas:

(1) Above grade pump, valve rooms, or similar areas.

(2) Locations within 20 ft of tank vents.

(3) Locations within tank dikes.

(4) Within 50 ft of tank loading or unloading outlets.

d. *General.* Any spaces above ground normally considered to be Class 1 Division 2 may be specified to fall within Division 1 if evidence exists that vapor concentrations exceeding the LEL regularly exist at least 2 inches above grade in the vicinity of electrical equipment.

APPENDIX I

EXCERPTS FROM AFM 88-15 AND NATIONAL ELECTRICAL CODE

Excerpts from AFM 88-15, 3 March 1970

7-10. Hazardous Areas:

a. *Requirements.* Unless otherwise authorized, wiring materials and equipment within hazardous areas shall conform to the requirements for the particular hazard involved as specified in the National Electrical Code.

b. *Hangars and Docks:*

(1) The following spaces are considered to be class 1, division 1, group C of hazardous locations:

(a) The main hangar or dock area inclosed by the building walls, exclusive of adjoining rooms, and extending from the floor to the top of highest hangar door, except for the space within 2 feet of the wall above a 4-foot level. (Special situations wherein encroachment may be acceptable due to particular aircraft size or configuration will be referred to AFOCE-KC.)

(b) The space below a 4 foot level from the floor in adjacent areas not cut off from the main area by doors or walls.

(c) The space below an 18 inch level from the floor in adjacent areas cut off from the main area by doors or walls subject to fume leakage.

(2) Adjacent areas cut off from the main area by a minimum 4 foot elevation or by walls not subject to fume leakage are considered nonhazardous unless the usage of the specific area itself is hazardous.

(3) All fixed electrical equipment and wiring should be located outside the hazardous space, wherever possible. If, in special cases, it is necessary to encroach into the hazardous space for installation of nonexplosion proof equipment, such equipment will be confined to the space 5 feet or more above the upper surface, or 5 feet or more horizontally out from the edges of the wings, fuselage, or any part of the aircraft which normally contains fuel tanks or vents for the largest aircraft that can be accommodated in the facility.

(4) Where docks and hangars are used for fuel system and fuel cell repair the above criteria are applicable, provided other special treatment requirements (vapor detection, fuel disposal, and approved exhaust air movements) are also met.

(5) Except as specifically stated above, all remaining electrical wiring and equipment shall meet requirements of the National Electrical Code.

c. *POL Areas.* Electrical equipment will be explosion proof as approved for class 1, group C, division 1, locations when installed under the following conditions.

(1) In below-grade housing or pits.

(2) In above-grade pump rooms, valve rooms, and similar areas.

(3) Within 20 feet of vents for underground tanks.

(4) Within dikes of above-ground tanks.

(5) Within 50 feet of tank loading or unloading outlets.

d. When required for industrial areas, explosion-proof lighting fixtures will be of incandescent type. Fluorescent type is not permitted in these areas.

Excerpts from National Electrical Code

NATIONAL ELECTRICAL CODE

ARTICLE 500 — HAZARDOUS LOCATIONS

500-1. Scope. The provisions of Articles 500 through 503 apply to locations in which the authority having jurisdiction judges the apparatus and wiring to be subject to the conditions indicated by the following classifications. It is intended that each room, section or area (including motor and generator rooms, and rooms for the enclosure of control equipment) shall be considered individually in determining its classification. Except as modified in Articles 500 through 503, all other applicable rules contained in this Code shall apply to electrical apparatus and wiring installed in hazardous locations. For definitions of "approved" and "explosion-proof" as used in these Articles, refer to Article 100. "dust-ignition-proof" is defined in Section 502-1.

Equipment and associated wiring approved as intrinsically safe may be installed in any hazardous location for which it is approved, and the provisions of Articles 500 through 517 need not apply to such installation. Intrinsically safe equipment and wiring are incapable of releasing sufficient electrical energy under normal or abnormal conditions to cause ignition of a specific hazardous atmospheric mixture. Abnormal conditions will include accidental damage to any part of the equipment or wiring, insulation or other failure of electrical components, application of overvoltage, adjustment and maintenance operations, and other similar conditions.

For further information see NFPA No. 493-1969 Standard for Intrinsically Safe Process Control Equipment for use in Class I Hazardous Locations.

Through the exercise of ingenuity in the layout of electrical installations for hazardous locations, it is frequently possible to locate much of the equipment in less hazardous or in nonhazardous areas and thus to reduce the amount of special equipment required. In some cases, hazards may be reduced or hazardous areas limited or eliminated by adequate positive-pressure ventilation from a source of clean air in conjunction with effective safeguards against ventilation failure. For further information see NFPA No. 496-1967 Standard for Purged Enclosures for Electrical Equipment in Hazardous Locations. It is recommended also that the authority having jurisdiction be familiar with such recorded industrial experience as well as with

Table 500-2(b). Identification Numbers

<u>Degrees C</u>	<u>Degrees F</u>	<u>Identification Number</u>
450	842	T1
300	572	T2
280	536	T2A
260	500	T2B
230	446	T2C
215	419	T2D
200	392	T3
180	356	T3A
165	329	T3B
160	320	T3C
135	275	T4
120	248	T4A
100	212	T5
85	185	T6

Excerpts from National Electrical Code (Cont'd)

ARTICLE 500—HAZARDOUS LOCATIONS

70-289

Table 500-2(c). Chemicals by Groups

Group A Atmospheres	Group D Atmospheres
Chemical	Chemical
acetylene	acetone
Group B Atmospheres	acrylonitrile
butadiene ¹	ammonia ¹
ethylene oxide ²	benzene
hydrogen	butane
manufactured gases containing more than 30% hydrogen (by volume)	1-butanol (butyl alcohol)
propylene oxide ²	2-butanol (secondary butyl alcohol)
Group C Atmospheres	n-butyl acetate
acetaldehyde	isobutyl acetate
cyclopropane	ethane
diethyl ether	ethanol (ethyl alcohol)
ethylene	ethyl acetate
isoprene	ethylene dichloride
unsymmetrical dimethyl hydrazine (UDMH 1, 1-dimethyl hydrazine)	gasoline
	heptanes
	hexanes
	methane (natural gas)
	methanol (methyl alcohol)
	3-methyl-1-butanol (isoamyl alcohol)
	methyl ethyl ketone
	methyl isobutyl ketone
	2-methyl-1-propanol (isobutyl alcohol)
	2-methyl-2-propanol (tertiary butyl alcohol)
	petroleum naphtha ¹
	octanes
	pentanes
	1-pentanol (amyl alcohol)
	propane
	1-propanol (propyl alcohol)
	2-propanol (isopropyl alcohol)
	propylene
	styrene
	toluene
	vinyl acetate
	vinyl chloride
	xylenes

¹ Group D equipment may be used for this atmosphere if such equipment is isolated in accordance with Section 501-5(a) by sealing all conduit ½-inch size or larger.

² Group C equipment may be used for this atmosphere if such equipment is isolated in accordance with Section 501-5(a) by sealing all conduit ½-inch size or larger.

³ For Classification of areas involving ammonia atmosphere refer to ANSI B9.1 Safety Code for Mechanical Refrigeration-1971 and ANSI K61.1 Storage and Handling of Anhydrous Ammonia-1971.

⁴ A saturated hydrocarbon mixture boiling in the range 20–135°C (68–275°F). Also known by the synonyms benzine, ligroin, petroleum ether or naptha.

Excerpts from National Electrical Code (Cont'd)

500-4. Class I Locations. Class I locations are those in which flammable gases or vapors are or may be present in the air in quantities sufficient to produce explosive or ignitable mixtures. Class I locations shall include the following:

(a) **Class I, Division 1.** Locations (1) in which hazardous concentrations of flammable gases or vapors exist continuously, intermittently, or periodically under normal operating conditions, (2) in which hazardous concentrations of such gases or vapors may exist frequently because of repair or maintenance operations or because of leakage, or (3) in which breakdown or faulty operation of equipment or processes which might release hazardous concentrations of flammable gases or vapors, might also cause simultaneous failure of electrical equipment.

This classification usually includes locations where volatile flammable liquids or liquefied flammable gases are transferred from one container to another; interiors of spray booths and areas in the vicinity of spraying and painting operations where volatile flammable solvents are used; locations containing open tanks or vats of volatile flammable liquids; drying rooms or compartments for the evaporation of flammable solvents; locations containing fat and oil extraction apparatus using volatile flammable solvents; portions of cleaning and dyeing plants where hazardous liquids are used; gas generator rooms and other portions of gas manufacturing plants where flammable gas may escape; inadequately ventilated pump rooms for flammable gas or for volatile flammable liquids; the interiors of refrigerators and freezers in which volatile, flammable materials are stored in open, lightly stoppered, or easily ruptured containers, and all other locations where hazardous concentrations of flammable vapors or gases are likely to occur in the course of normal operations.

(b) **Class I, Division 2.** Locations (1) in which volatile flammable liquids or flammable gases are handled, processed or used, but in which the hazardous liquids, vapors or gases will normally be confined within closed containers or closed systems from which they can escape only in case of accidental rupture or breakdown of such containers or systems, or in case of abnormal operation of equipment, (2) in which hazardous concentrations of gases or vapors are normally prevented by positive mechanical ventilation, but which might become hazardous through failure or abnormal operation of the ventilating equipment, or (3) which are adjacent to Class I, Division 1 locations, and to which hazardous concentrations of gases or vapors might occasionally be communicated unless such communication is prevented by adequate positive-pressure ventilation from a source of clean air, and effective safeguards against ventilation failure are provided.

This classification usually includes locations where volatile flammable liquids or flammable gases or vapors are used, but which, in the judgment of the authority having jurisdiction, would become hazardous only in case of an accident or of some unusual operating condition. The quantity of hazardous material that might escape in case of accident, the adequacy of ventilating equipment, the total area involved, and the record of the industry or business with respect to explosions or fires are all factors that should receive consideration in determining the classification and extent of each hazardous area.

Piping without valves, checks, meters and similar devices would not ordinarily be deemed to introduce a hazardous condition even though used for hazardous liquids or gases. Locations used for the storage of hazardous liquids or of liquefied or compressed gases in sealed containers would not normally be considered hazardous unless subject to other hazardous conditions also.

Electrical conduits and their associated enclosures separated from process fluids by a single seal or barrier shall be classed as Division 2 locations if the outside of conduit and enclosures is a nonhazardous area.

Excerpts from National Electrical Code (Cont'd)

ARTICLE 513 — AIRCRAFT HANGARS

513-1. Definition. This occupancy shall include locations used for storage or servicing of aircraft in which gasoline, jet fuels, or other volatile flammable liquids, or flammable gases, are used, but shall not include such locations when used exclusively for aircraft which have never contained such liquids or gases, or which have been drained and properly purged.

513-2. Hazardous Areas. Classification under Article 500.

(a) Any pit or depression below the level of the hangar floor shall be considered to be a Class I, Division 1 location which shall extend up to said floor level.

(b) The entire area of the hangar including any adjacent and communicating areas not suitably cut off from the hangar shall be considered to be a Class I, Division 2 location up to a level 18 inches above the floor.

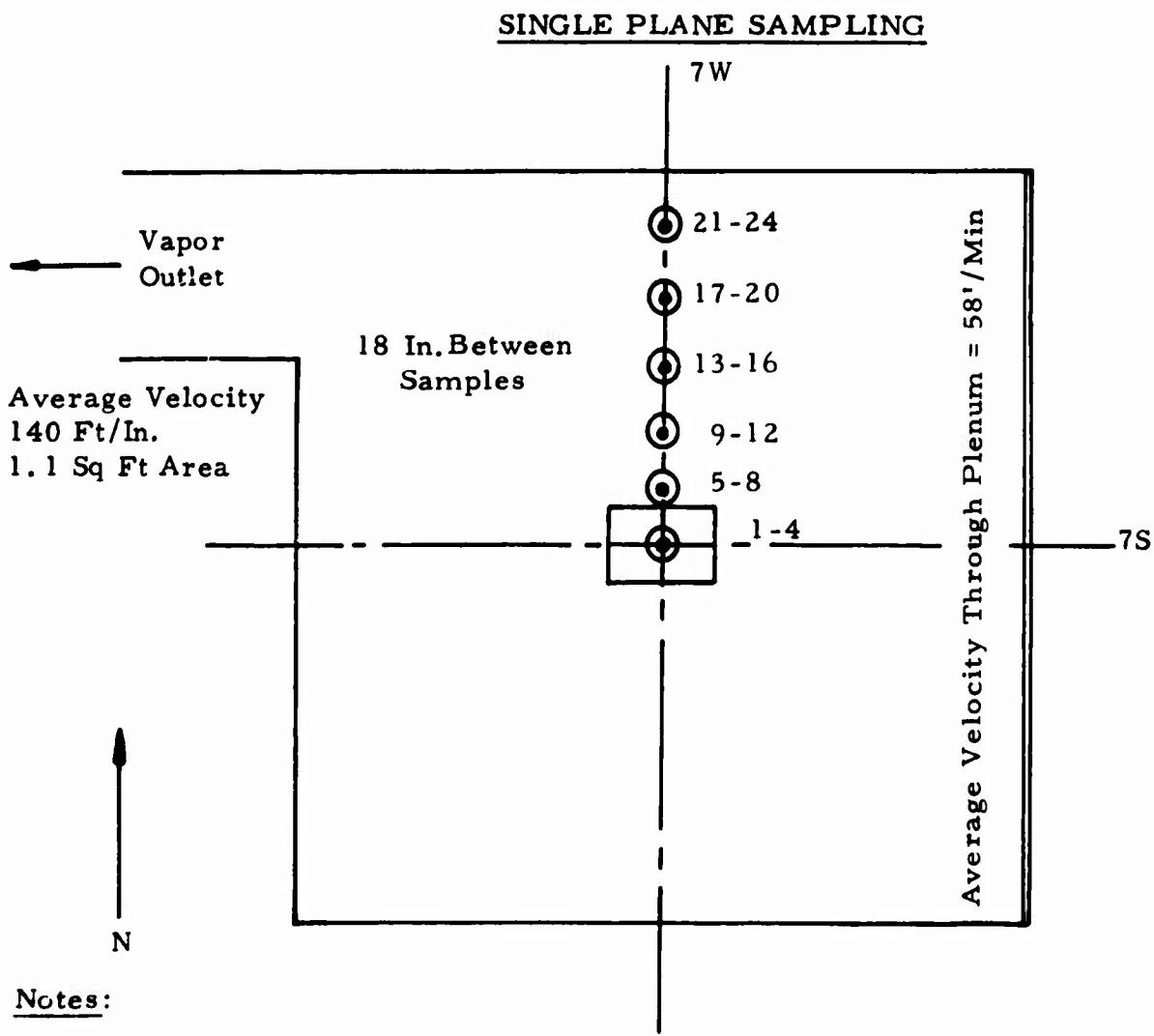
(c) The area within 5 feet horizontally from aircraft power plants, aircraft fuel tanks or aircraft structures containing fuel shall be considered to be a Class I, Division 2 hazardous location which shall extend upward from the floor to a level 5 feet above the upper surface of wings and of engine enclosures.

(d) Adjacent areas in which hazardous vapors are not likely to be released such as stock rooms, electrical control rooms, and other similar locations, should not be classed as hazardous when adequately ventilated and when effectively cut off from the hangar itself by walls or partitions.

513-3. Wiring and Equipment in Hazardous Areas. All fixed and portable wiring and equipment which is or may be installed or operated within any of the hazardous locations defined in Section 513-2 shall conform to applicable provisions of Article 501. All wiring installed in or under the hangar floor shall conform to the requirements for Class I, Division 1. When such wiring is located in vaults, pits, or ducts, adequate drainage shall be provided, and the wiring shall not be placed within the same compartment with any other service except piped compressed air.

Attachment plugs and receptacles in hazardous locations shall be explosion-proof or shall be so designed that they cannot be energized while the connections are being made or broken.

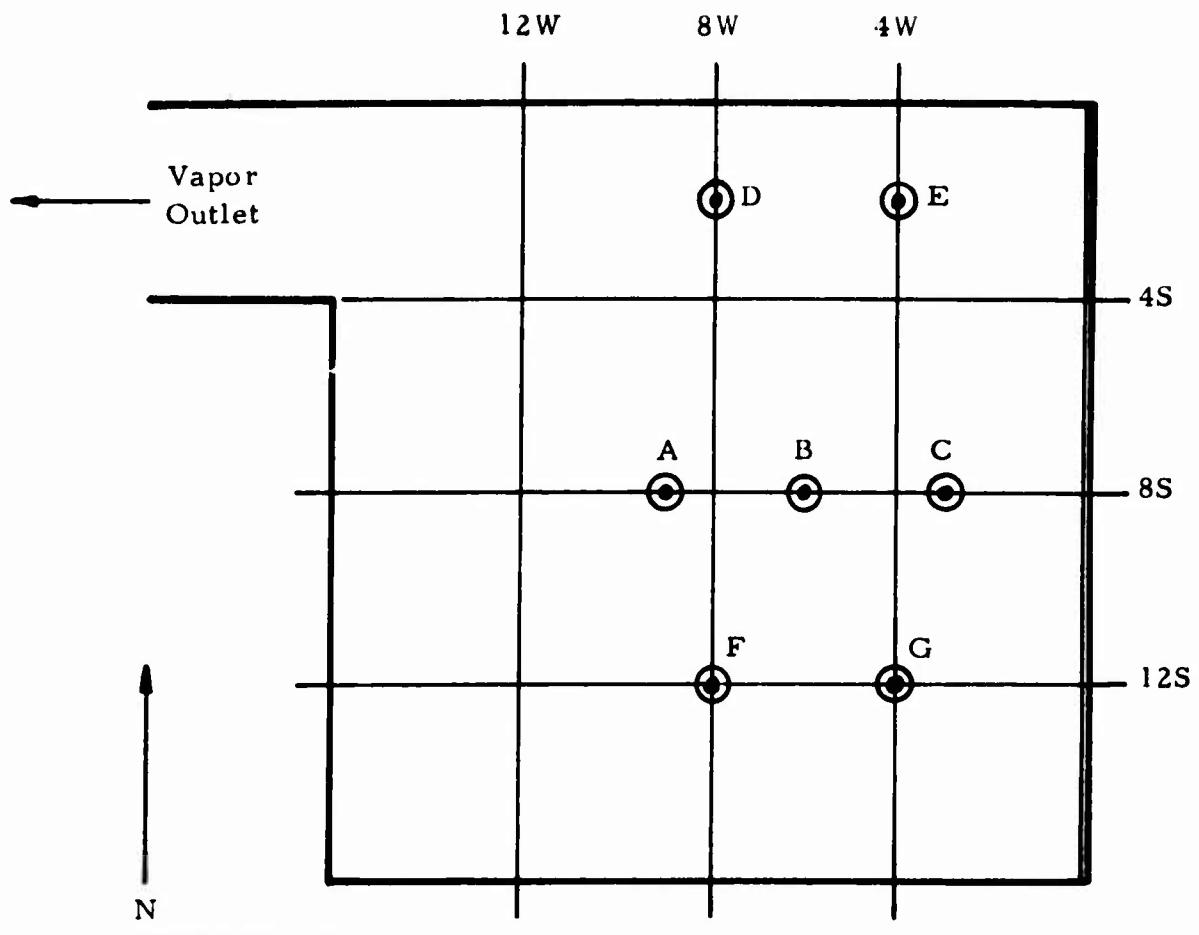
APPENDIX II
SAMPLING CONFIGURATIONS



Notes:

1. Sample points numbered upward from the floor 4, 8, 12, 16 in. levels.
2. For Test No. 4A, pan was upended to direct contents toward east wall.
3. For Test No. 4B, blowers were turned on. Average velocities shown refer only to this test.

FIGURE II-1. SAMPLE CONFIGURATION
NO. 1 FOR TESTS 1 THROUGH 5



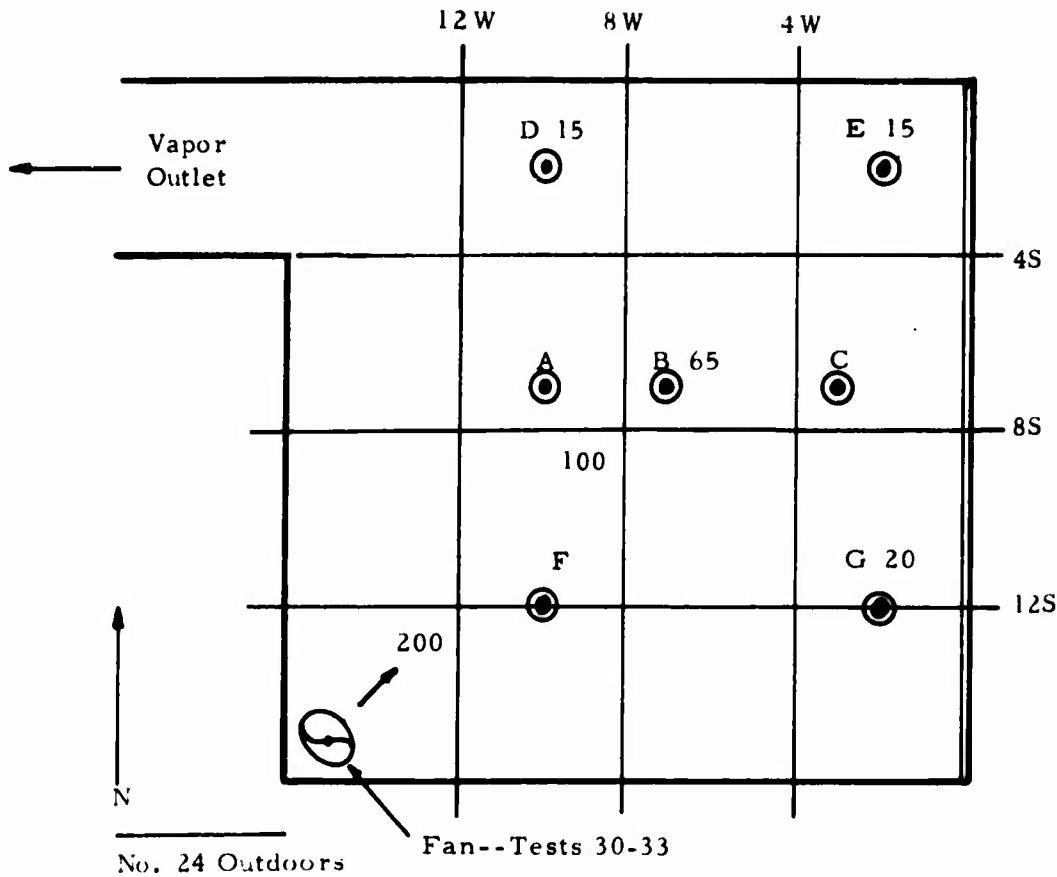
No. 24 Outdoors

Note:

Grid lines are at 4-ft intervals.

<u>Point No.</u>	<u>Location</u>	<u>Elevation, in.</u>	<u>Point No.</u>	<u>Location</u>	<u>Elevation, in.</u>
1	C	96	13	E	2
2	A	96	14	D	2
3	B	96	15	C	2
4	B	48	16	F	2
5	E	48	17	G	2
6	D	48	18	G	12
7	D	18	19	F	12
8	E	18	20	F	18
9	B	18	21	G	18
10	B	12	22	G	48
11	E	12	23	F	48
12	D	12	24	Outdoors	

FIGURE II-2. SAMPLE CONFIGURATION NO. 2
FOR TESTS 6 THROUGH 11

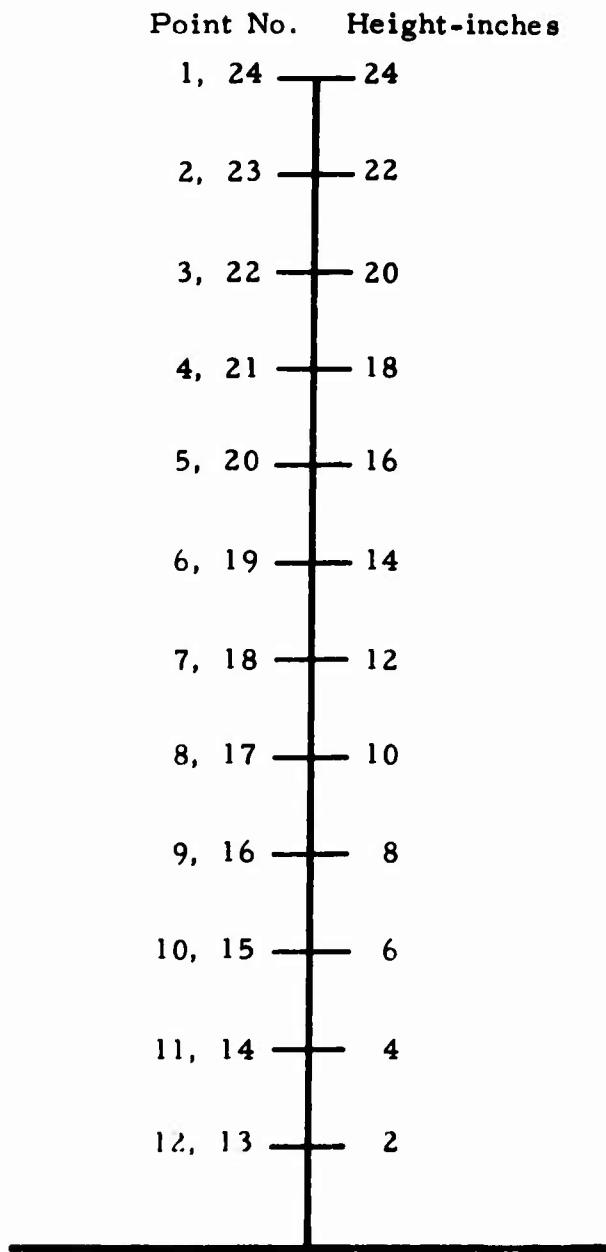


Note:

1. Sample configuration No. 3 differs from No. 2 only in wider spacing between D-E and F-G.
2. Grid lines are at 4-ft intervals. Numbers are air velocities in ft/min with fan at 13W, 13S operating during parts of tests 30-33.

<u>Point No.</u>	<u>Location</u>	<u>Elevation, in.</u>	<u>Point No.</u>	<u>Location</u>	<u>Elevation, in.</u>
1	C	96	13	E	2
2	A	96	14	D	2
3	B	96	15	B	2
4	B	48	16	F	2
5	E	48	17	G	2
6	D	48	18	G	12
7	D	18	19	F	12
8	E	18	20	F	18
9	B	18	21	G	18
10	B	12	22	G	48
11	E	12	23	F	48
12	D	12	24	Outside	

FIGURE II-3. SAMPLE CONFIGURATION NO. 3
FOR TESTS 12 THROUGH 22

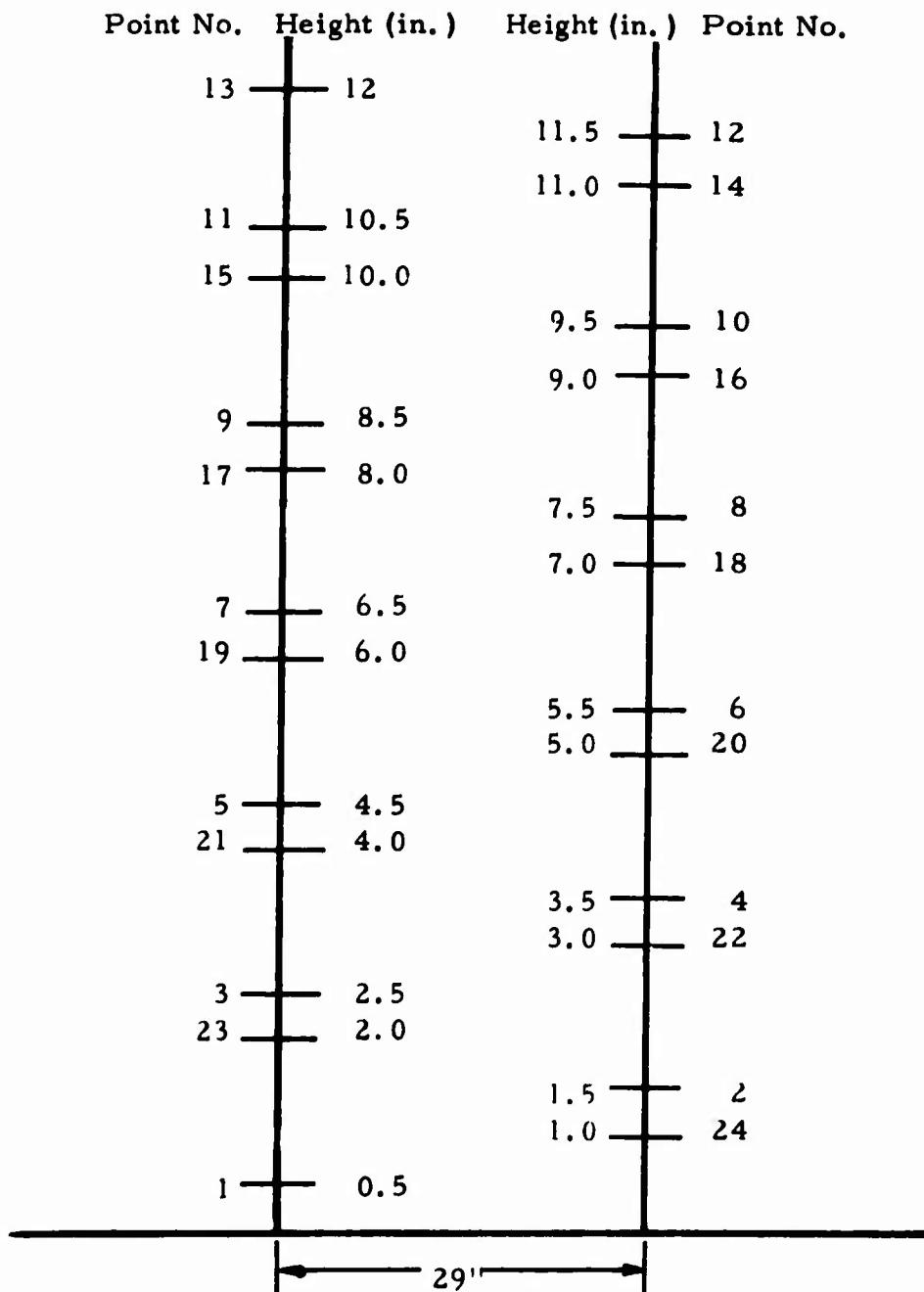


Tests 23 and 29

Note:

All sampling at center of room (7W, 7S). For tests 23 and 29, sample points are alternated 90° apart to reduce effect of sample air currents on vapor layer buildup.

**FIGURE II-4. VERTICAL PROFILE-SAMPLE-CONFIGURATION
NO. 4 FOR TEST NOS. 23 & 29**



Note:

Consecutive sampling points are separated 29 inches horizontally to minimize effects on vapor environment.

FIGURE II-5. VERTICAL PROFILE SAMPLINGS CONFIGURATION
NO. 5 FOR TESTS NOS. 34-37

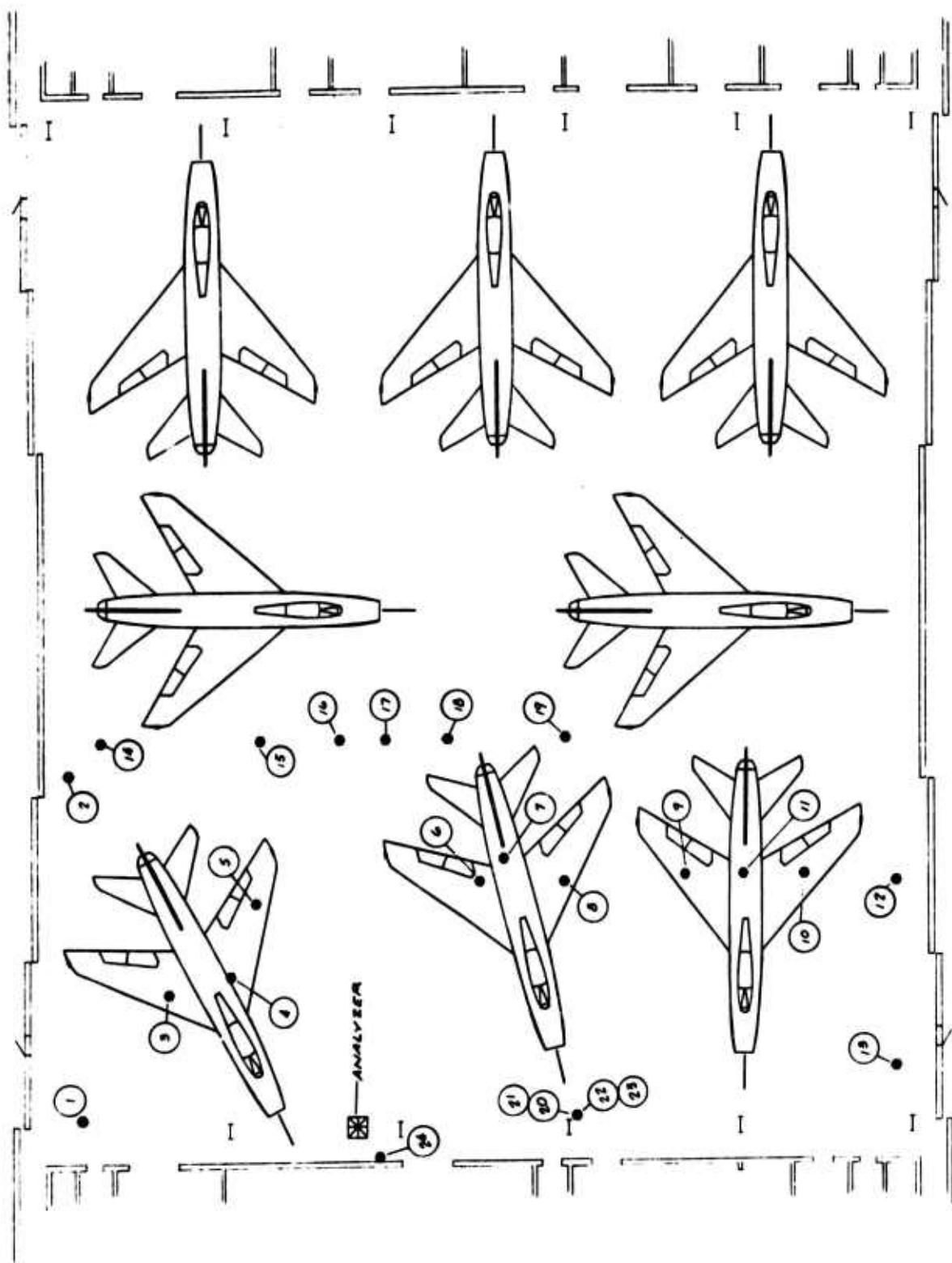


FIGURE II-6. SAMPLING CONFIGURATION FOR KELLY AFB TESTS 24 AND 25

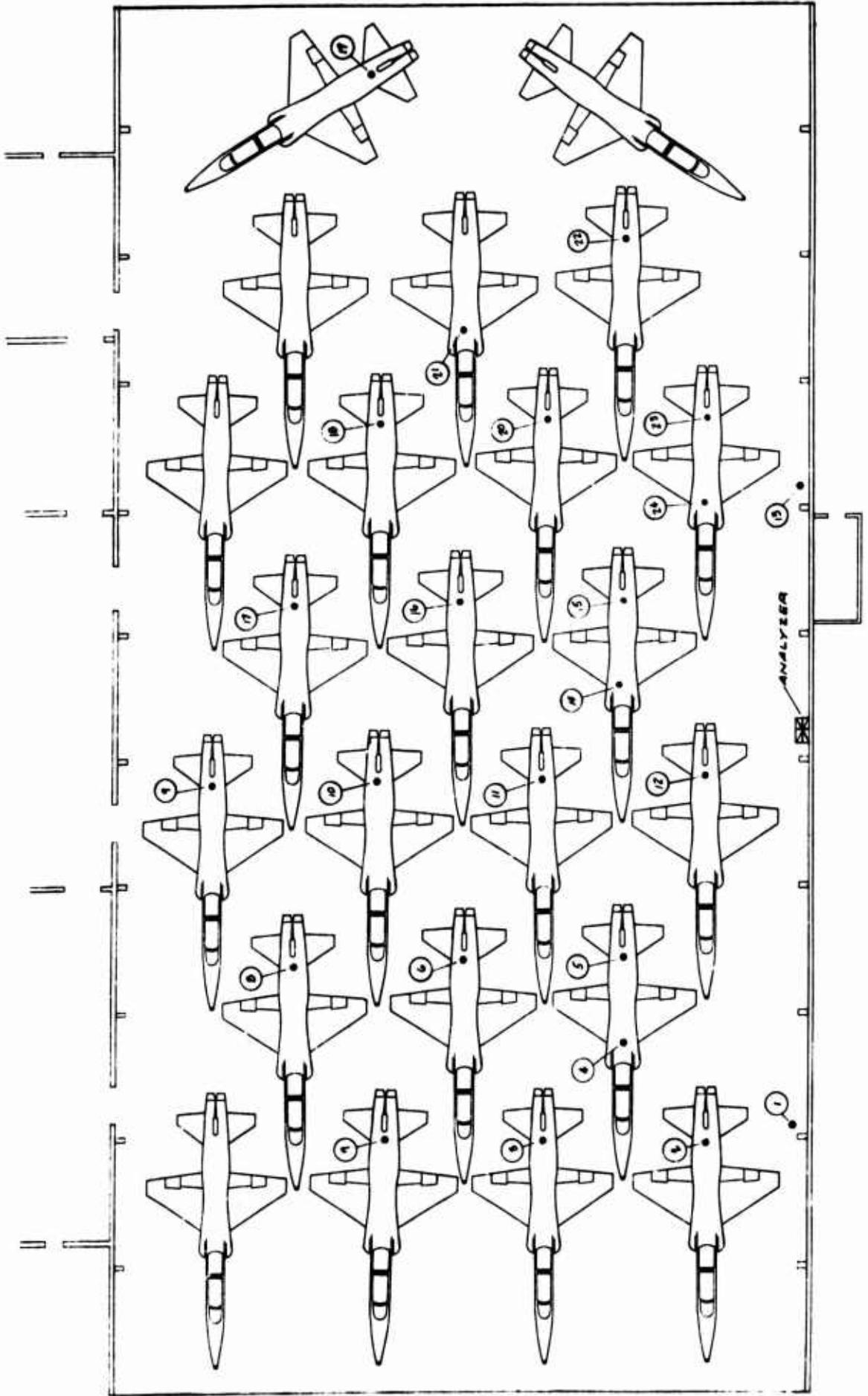


FIGURE II-7 SAMPLING CONFIGURATION FOR RANDOLPH AFB TEST 26

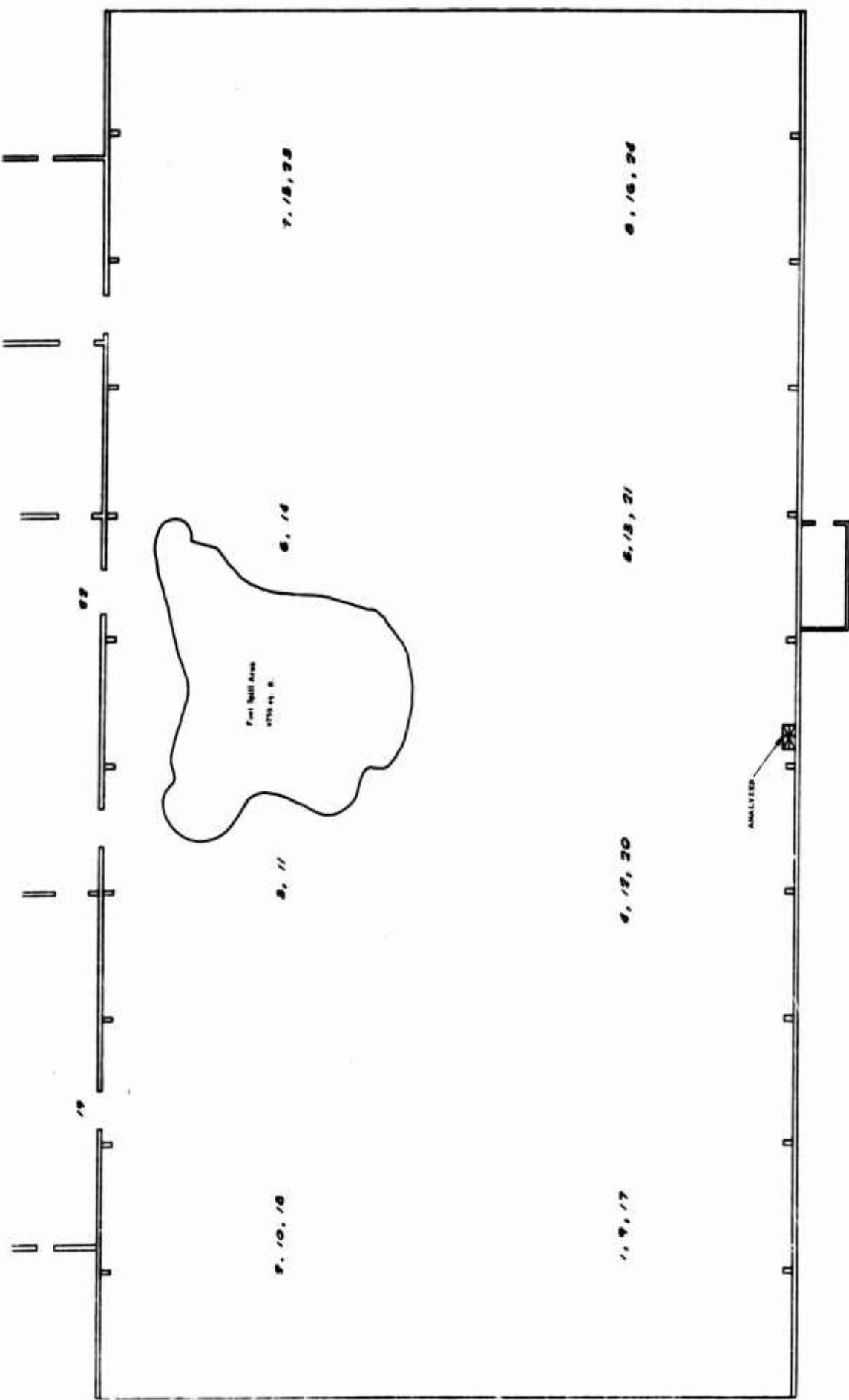


FIGURE II-8. SAMPLING CONFIGURATION FOR RANDOLPH AFB TEST 27

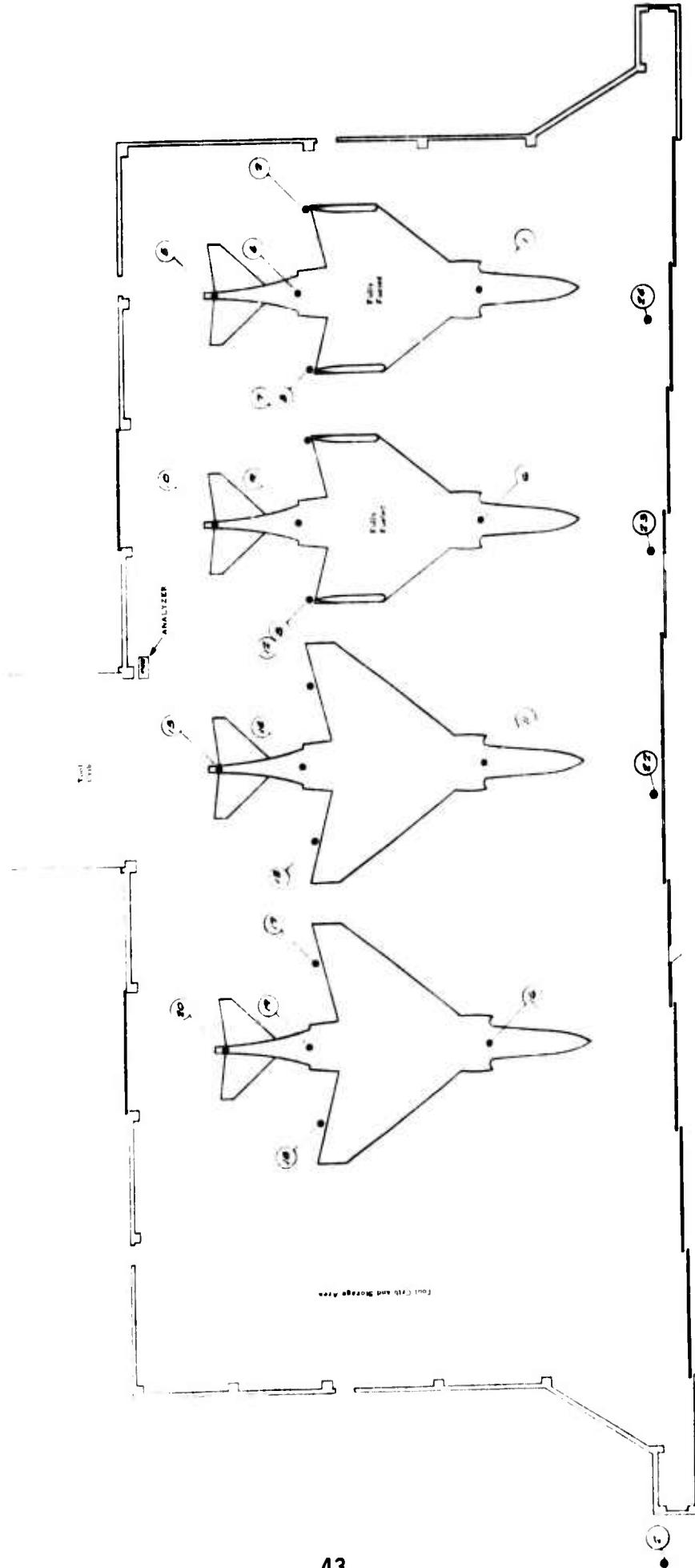


FIGURE II.9. SAMPLING CONFIGURATION FOR BERGSTROM AFB TEST 28

APPENDIX III
PLOTS OF THE TEST INFORMATION
ILLUSTRATIONS

<u>Figure</u>	<u>Run</u>	<u>Fuel</u>	<u>Temp. °F</u>	<u>Condition</u>
III-1	1	Avgas	71	1 gal in 6-sq ft pan
III-2	2	JP-4	73	1 gal in 6-sq ft pan
III-3	3	Avgas	62	2 gal in 5-sq ft pan
III-4A	4A	Avgas	64	Fuel from Test 3 spilled on floor
III-4B	4B	Avgas	63	Continue 4A-floor fan started
III-5	5	JP-4	66	2 gal in 5-sq ft pan w/fan
III-6	6	Avgas	71	2 gal in 5-sq ft pan
III-7	7	JP-4	75	2 gal in 5-sq ft pan
III-8	8	Avgas	72	2 gal dripped from 5 ft
III-9	9	JP-4	54	2 gal dripped from 5 ft
III-10	10	JP-4	71	4 gal dripped from 5 ft
III-11	11	Avgas	79	4 gal dripped from 5 ft
III-12	12	Avgas	52	4 gal spilled on floor
III-13	13	Avgas	98	4 gal spilled on floor
III-14	14	JP-4	97	4 gal spilled on floor
III-15	15	Avgas	52	4 gal spilled on floor
III-16	16	Avgas	60	10 gal spilled on floor
III-17	17	JP-4	50	4 gal spilled on floor
III-18	18	JP-4	64	10 gal spilled on floor
III-19	19	Avgas	67	4 gal spilled on floor
III-20	20	JP-4	67	4 gal spilled on floor
III-21	21	JP-4	65	4 gal spilled on floor
III-22	22	JP-4	77	4 gal spilled on floor
III-23	23	JP-4	62	4 gal spilled on floor (vertical profile run)
III-24	29	Avgas	69	4 gal spilled on floor (vertical profile)
III-25	30	Avgas	82	4-gal spill, w/fan
III-26	31	JP-4	89	4-gal spill, w/fan
III-27	32	Avgas	90	4-gal drip, w/fan
III-28	33	JP-4	85	4-gal drip, w/fan

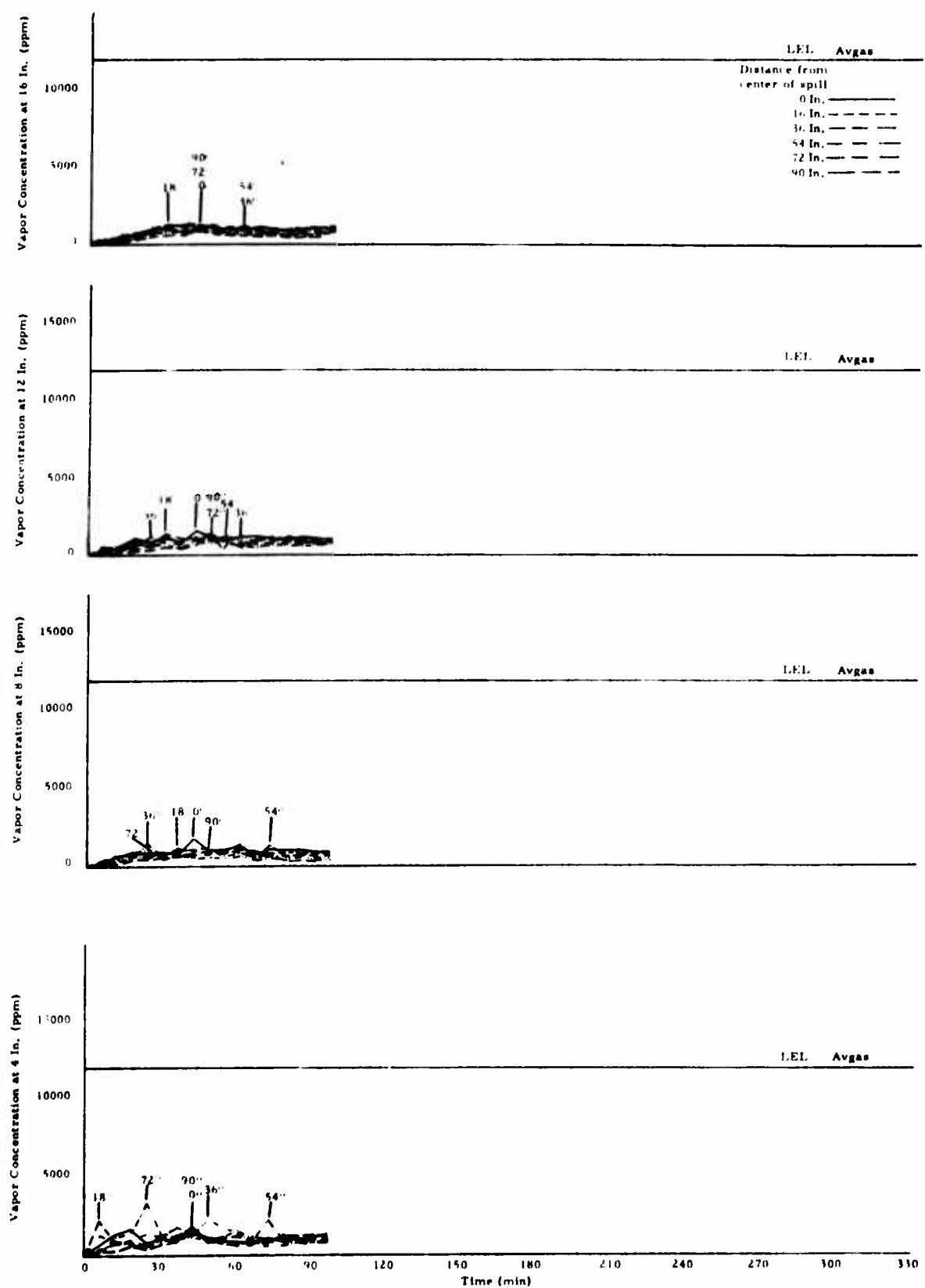


FIGURE III-1. TEST NO. 1—ONE GALLON AVGAS IN A 2' X 3' PAN

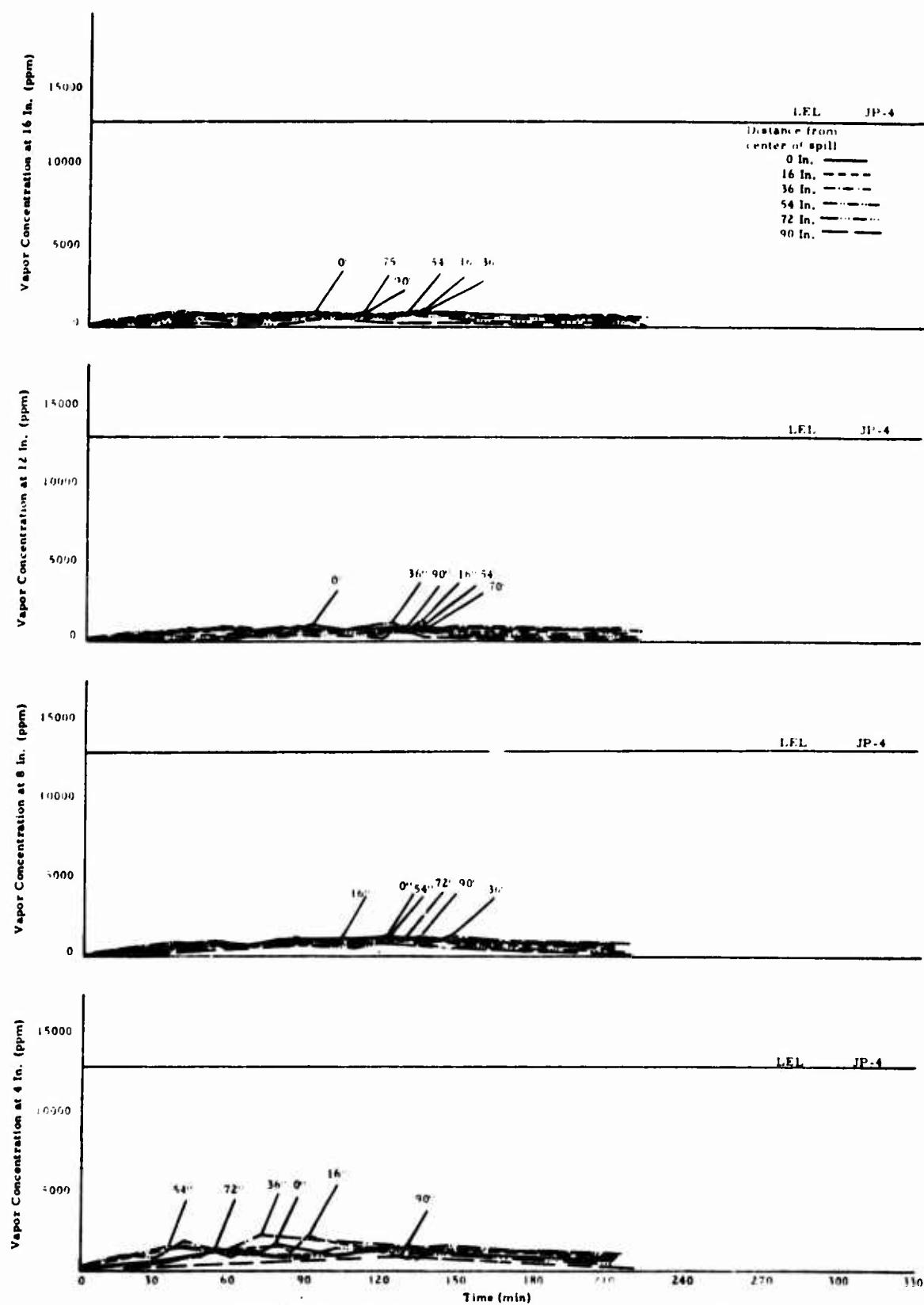


FIGURE III-2. TEST NO. 2 - ONE GALLON OF JP-4 IN A 2' X 3' PAN

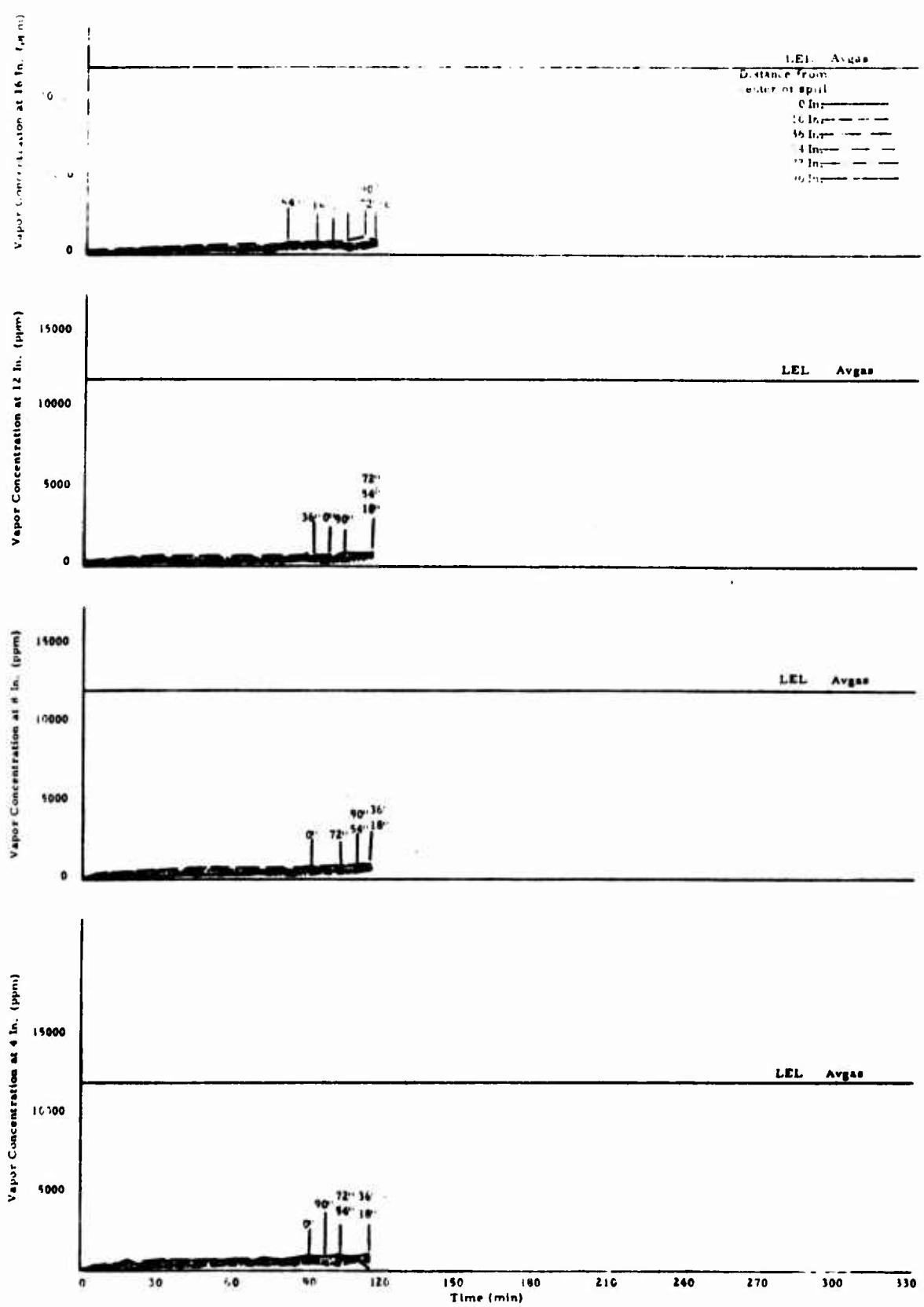


FIGURE III-3. TEST NO. 3-TWO GALLONS AVGAS IN A 2' X 3' PAN

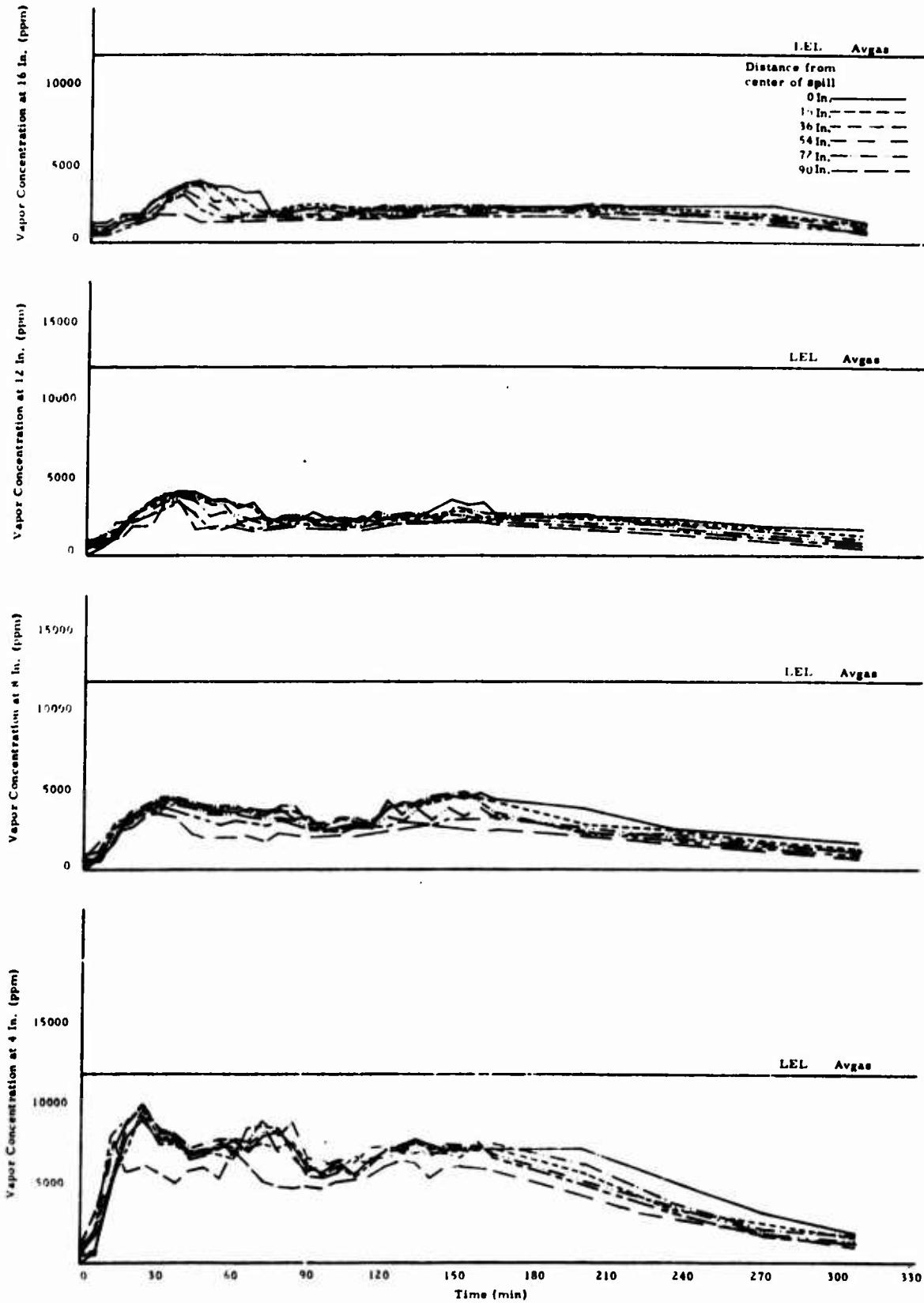


FIGURE III-4A. TEST NO. 4A - FUEL FROM TEST 3 SPILLED ON THE FLOOR

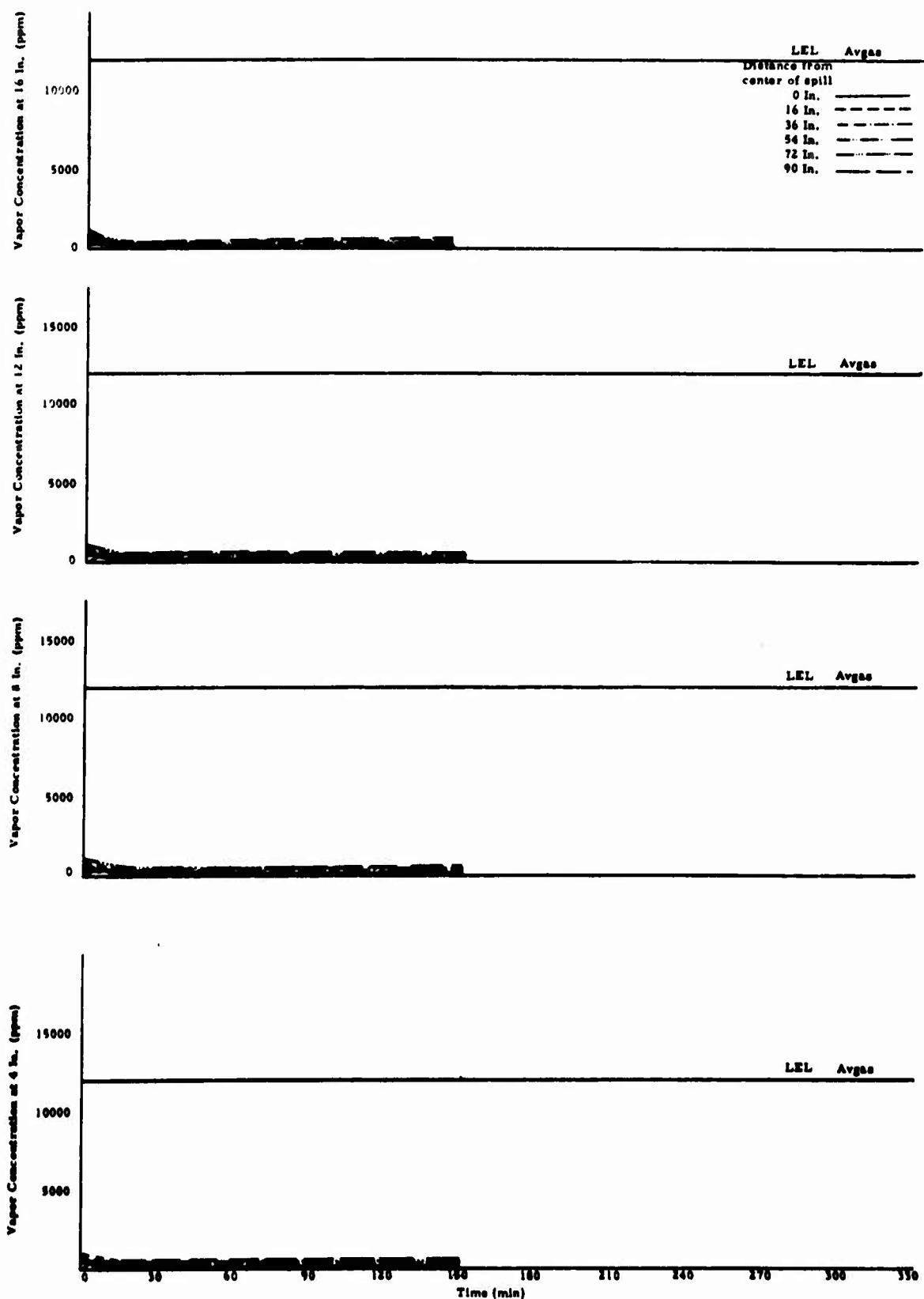


FIGURE III-4B. TEST NO. 4B-TWO GALLONS AVGAS SPILL IN CENTER OF ROOM WITH BLOWERS ON

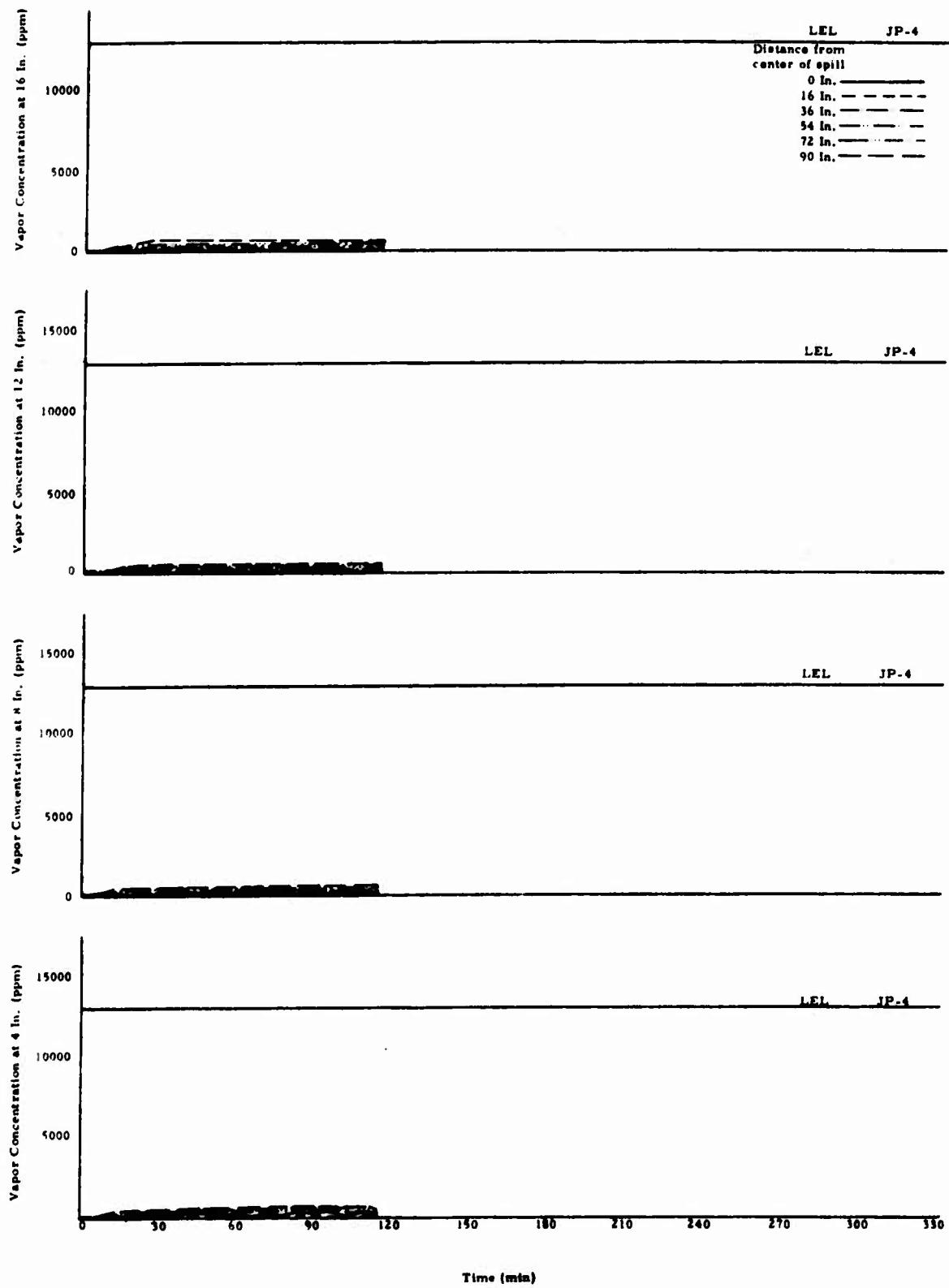


FIGURE III-5. TEST NO. 5 - TWO GALLONS JP-4 IN A 2' X 3' PAN

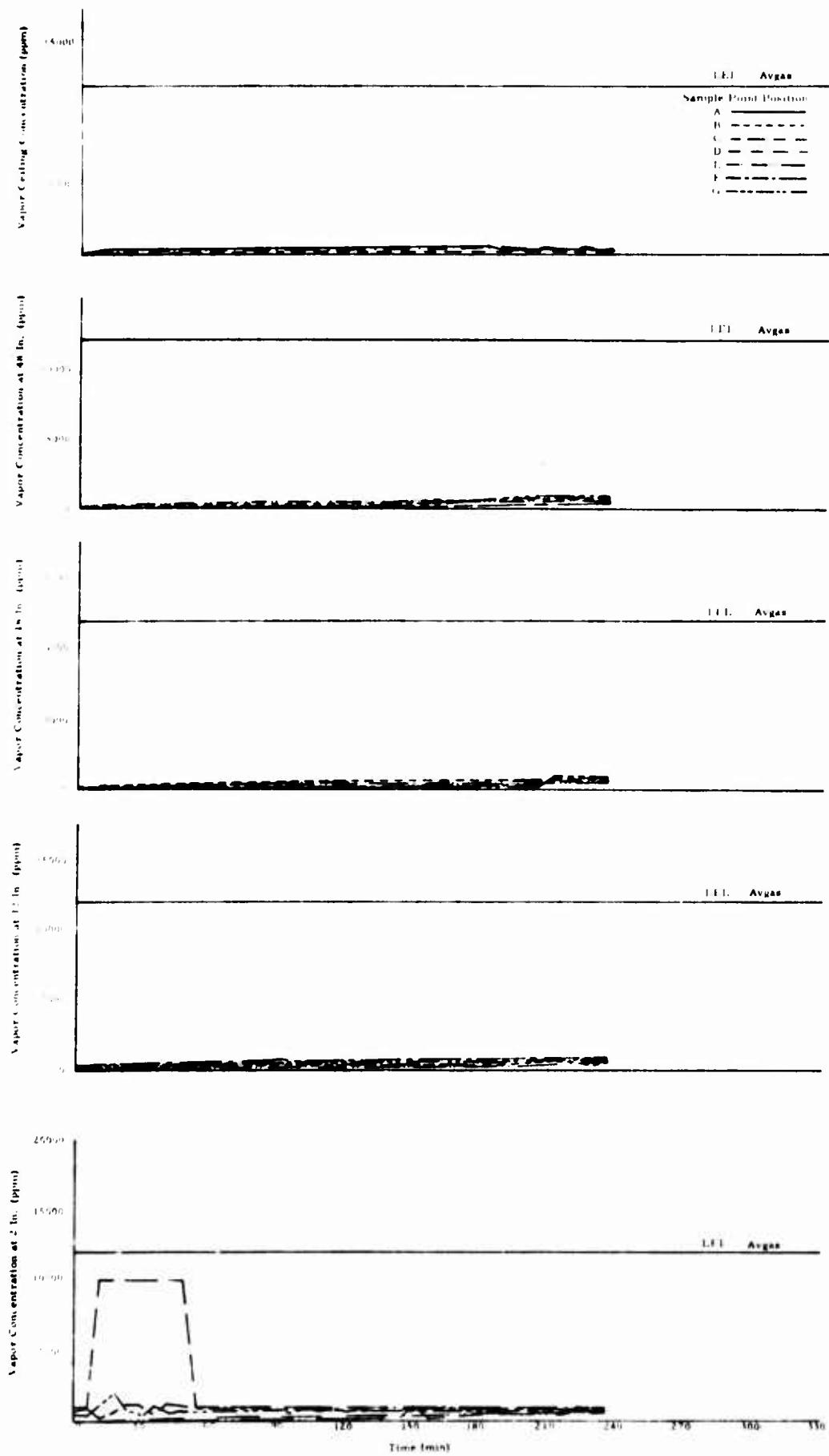


FIGURE III-6. TEST NO. 6 TWO GALLONS OF AVGAS IN A 24" X 30" X 2" PAN

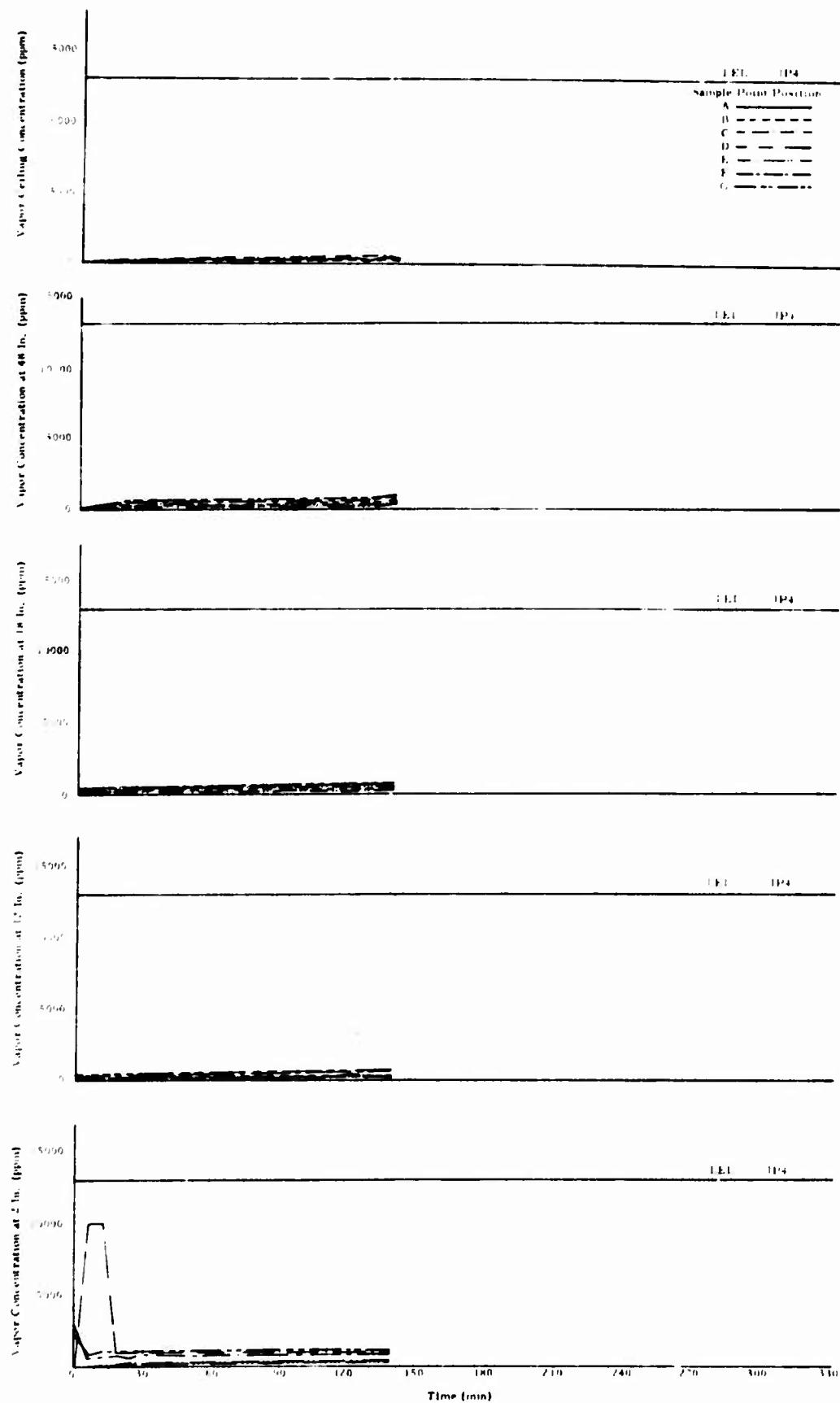


FIGURE III-7. TEST NO. 7 TWO GALLONS OF JP-4 IN A 24" X 30" X 2" PAN

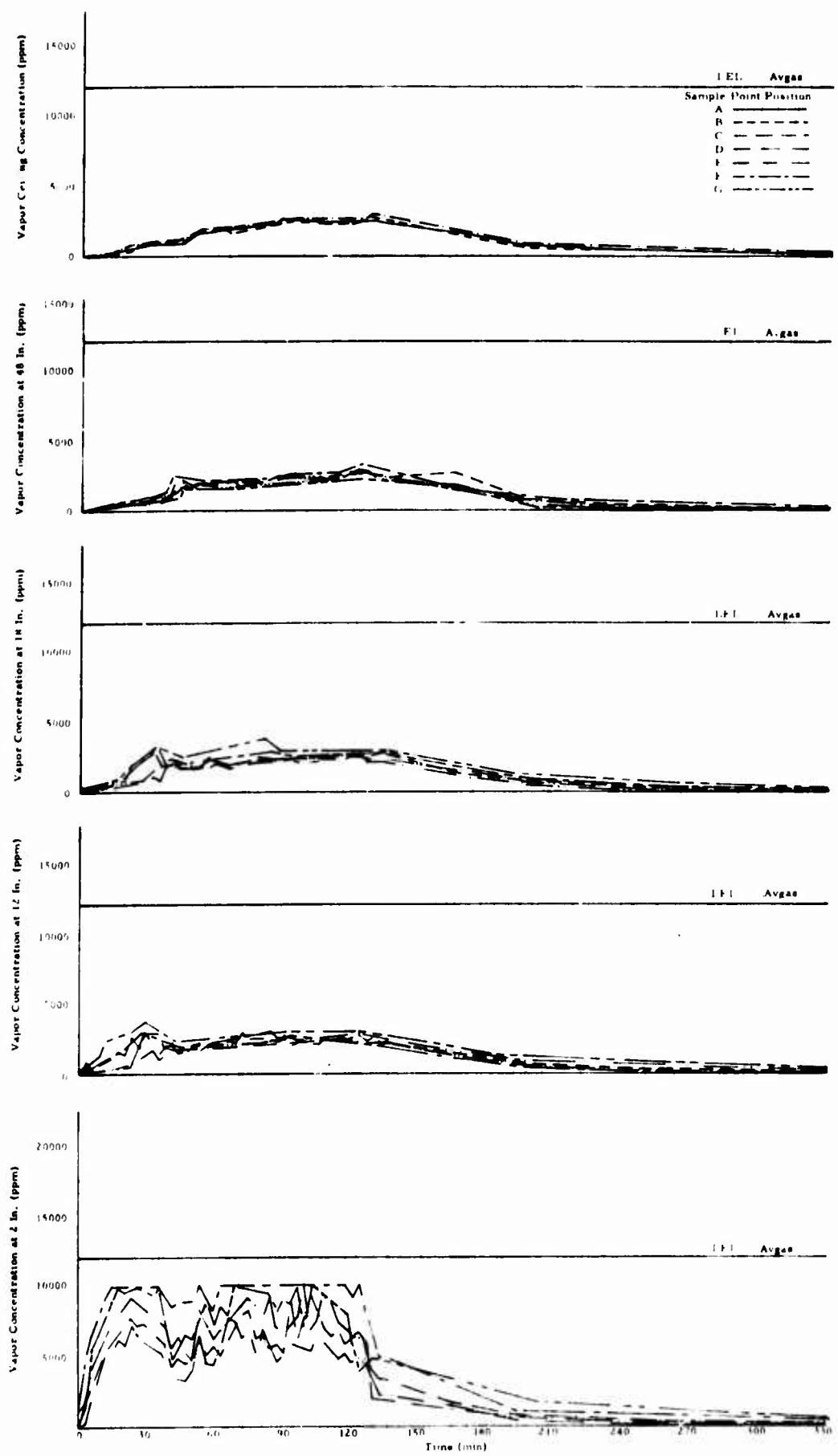


FIGURE III-8. TEST NO. 8-TWO GALLONS OF AVGAS IN DRIP TEST

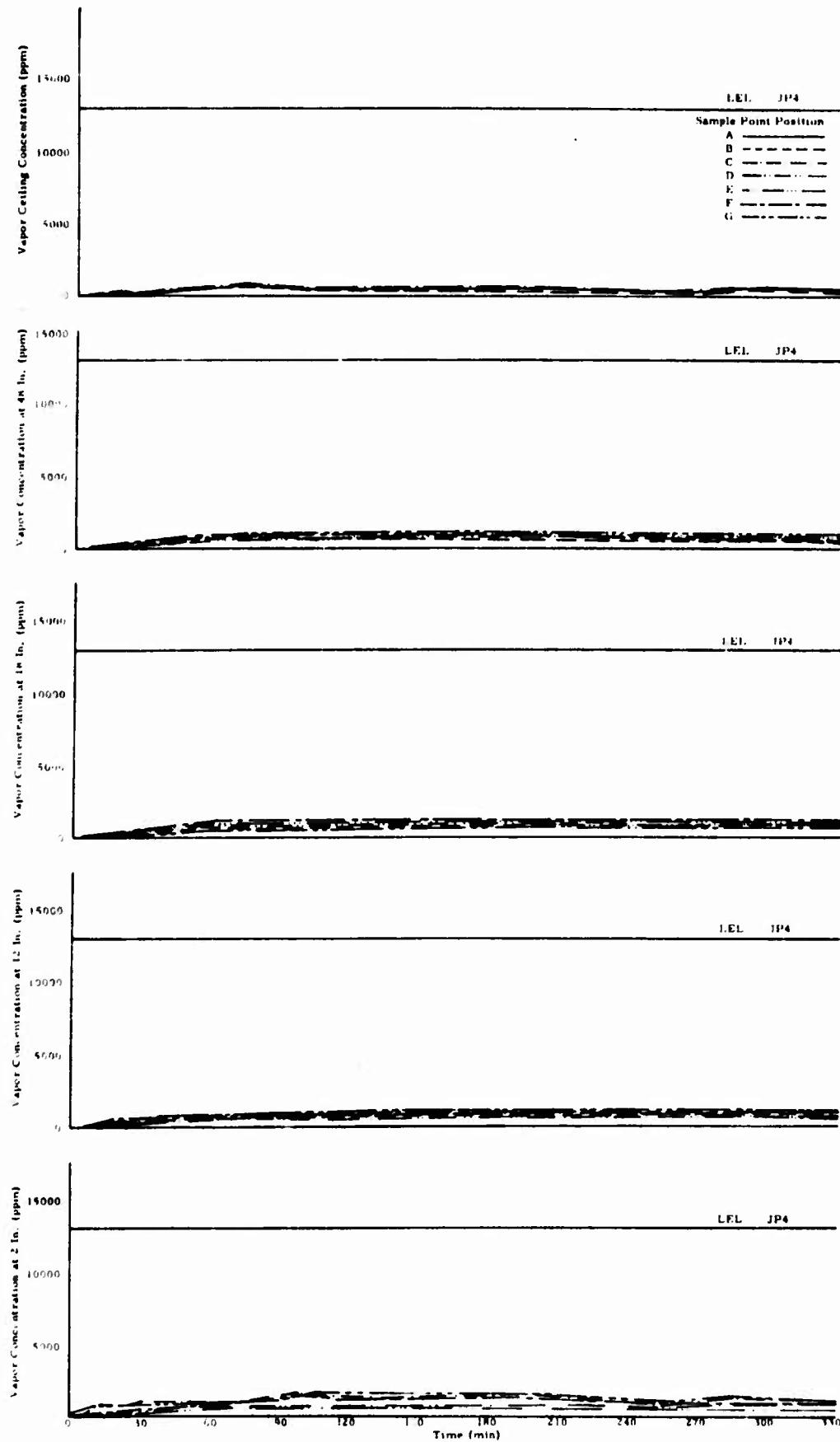


FIGURE III-9. TEST NO. 9-TWO GALLONS OF JP-4 IN DRIP TEST

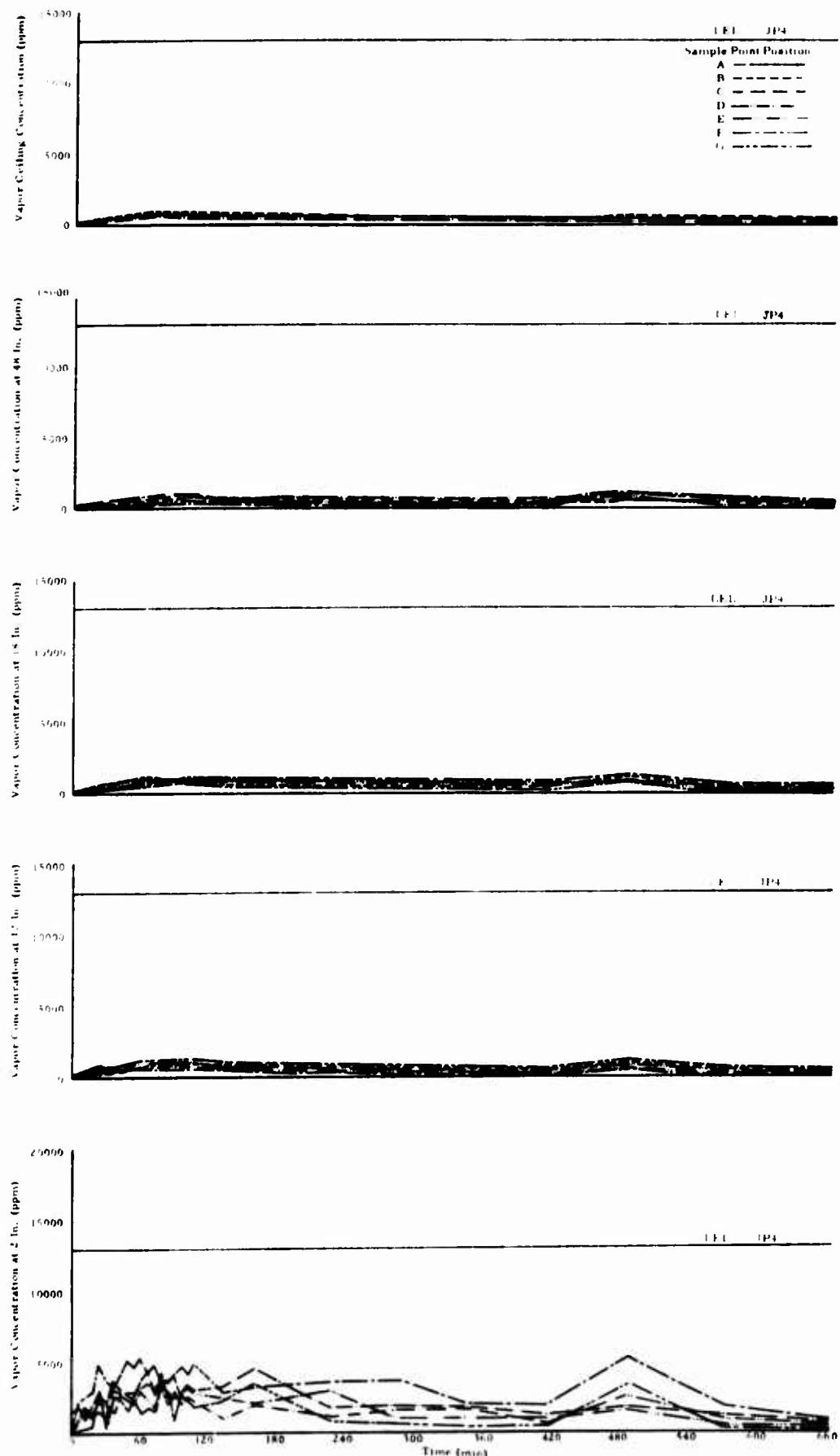


FIGURE III-10. TEST NO. 10—FOUR GALLONS OF JP-4 IN DRIP TEST

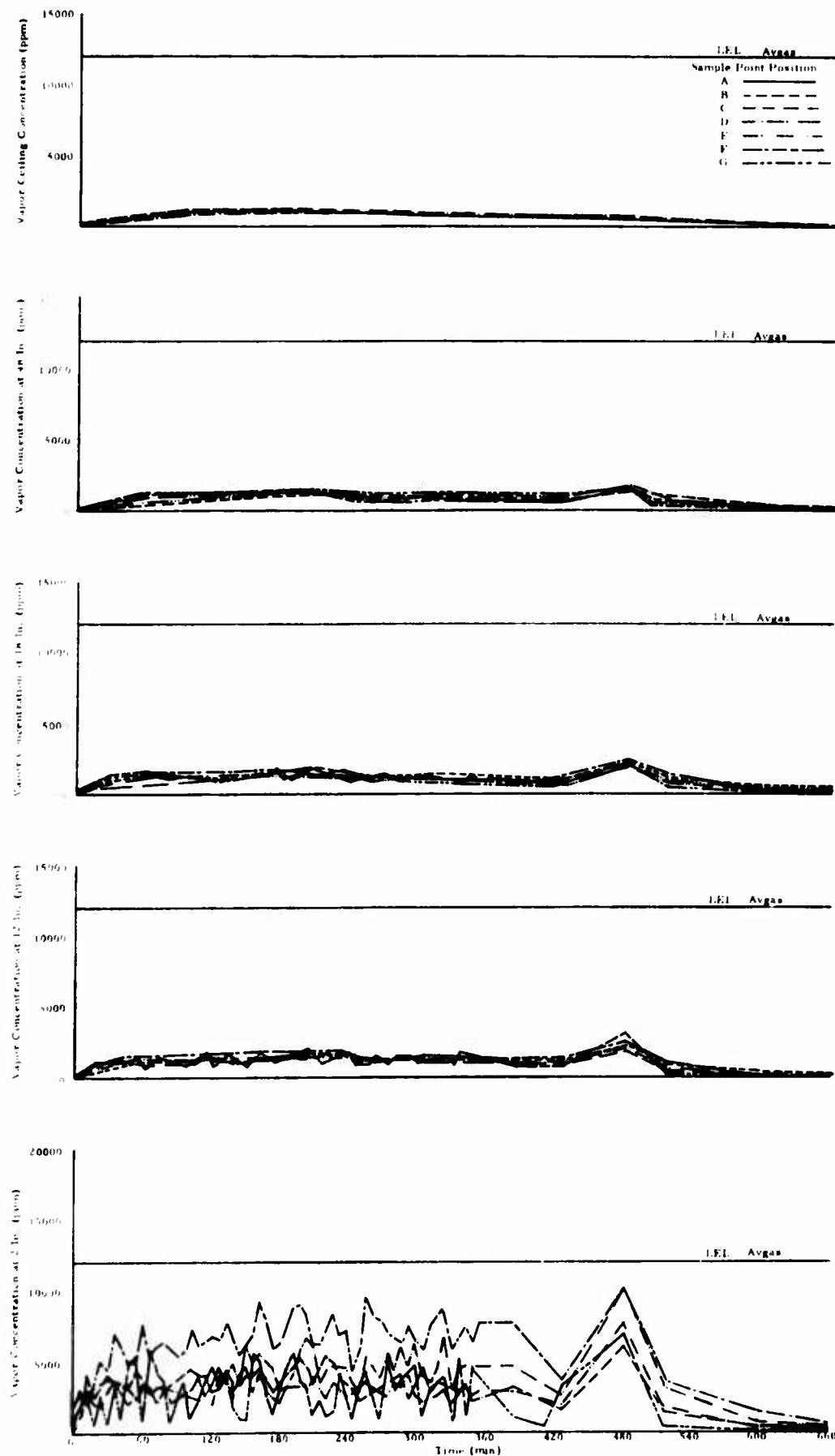


FIGURE III-11. TEST NO. 11—FOUR GALLONS OF AVGAS IN DRIP TEST

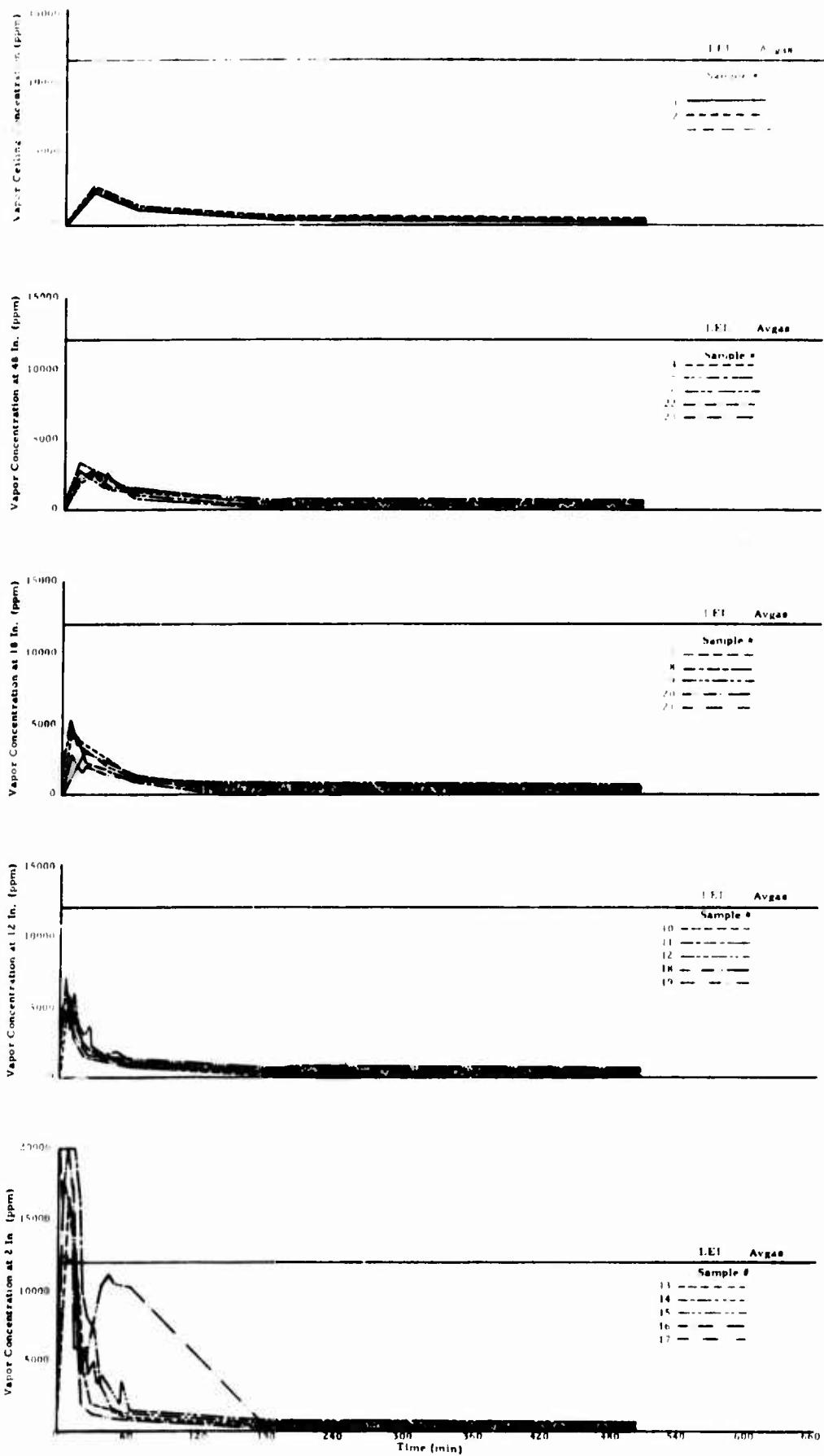


FIGURE III-12. TEST NO. 12 - FOUR GALLONS OF AVGAS IN A SPILL TEST

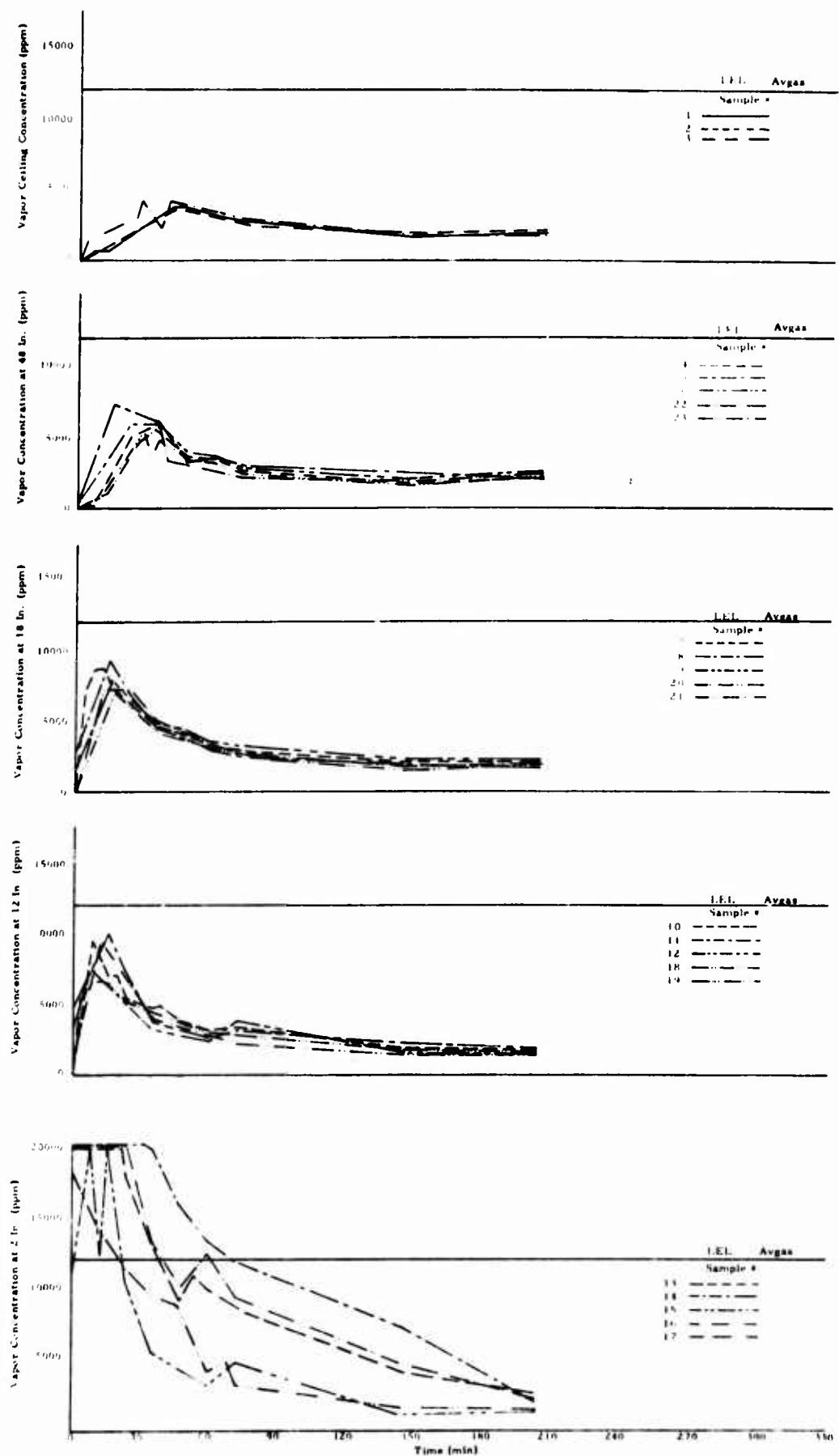


FIGURE III-13. TEST NO. 13 - FOUR GALLONS OF AVGAS IN A SPILL TEST

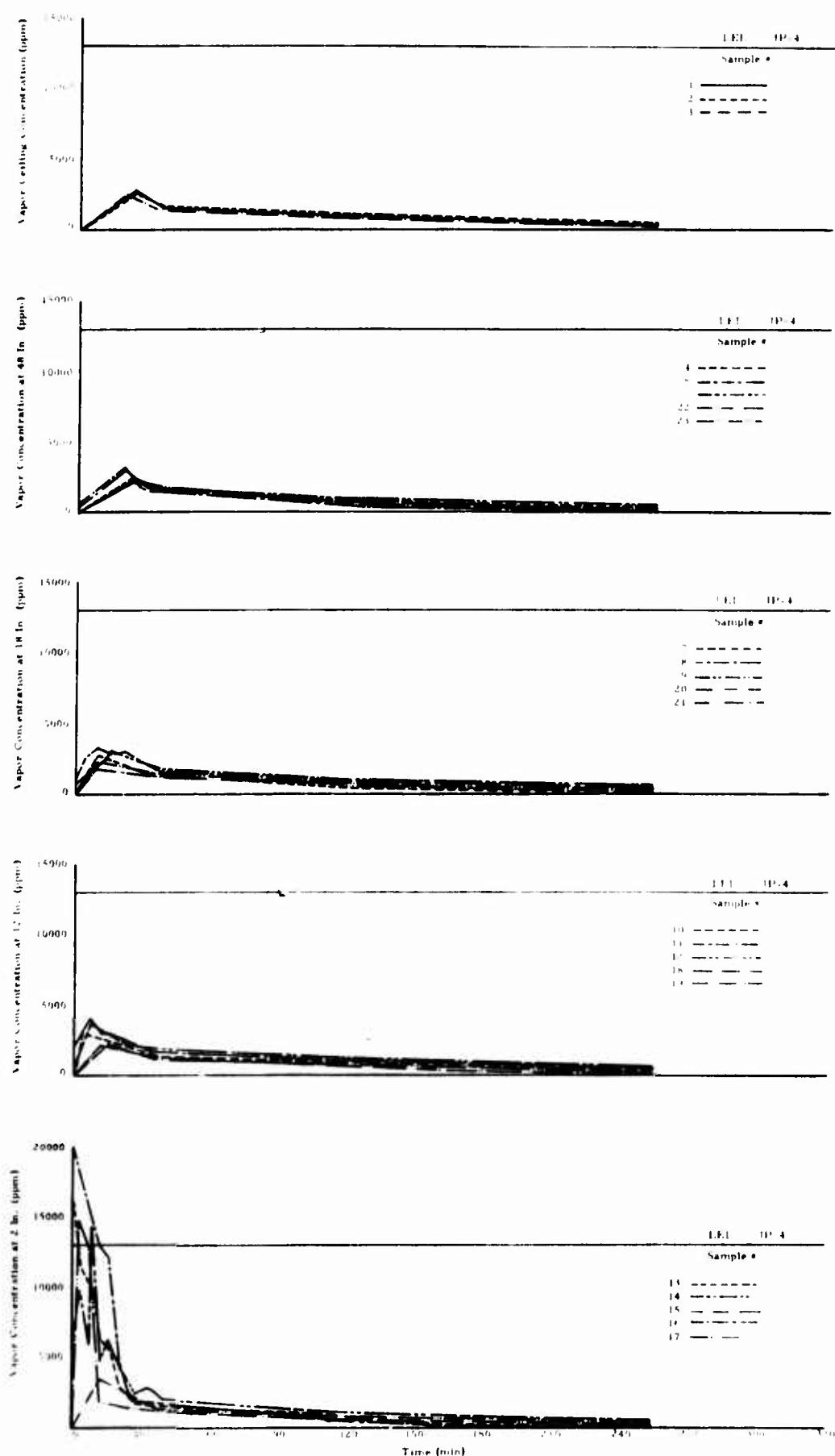


FIGURE III-14. TEST NO. 14-FOUR GALLONS OF JP-4 IN A SPILL TEST

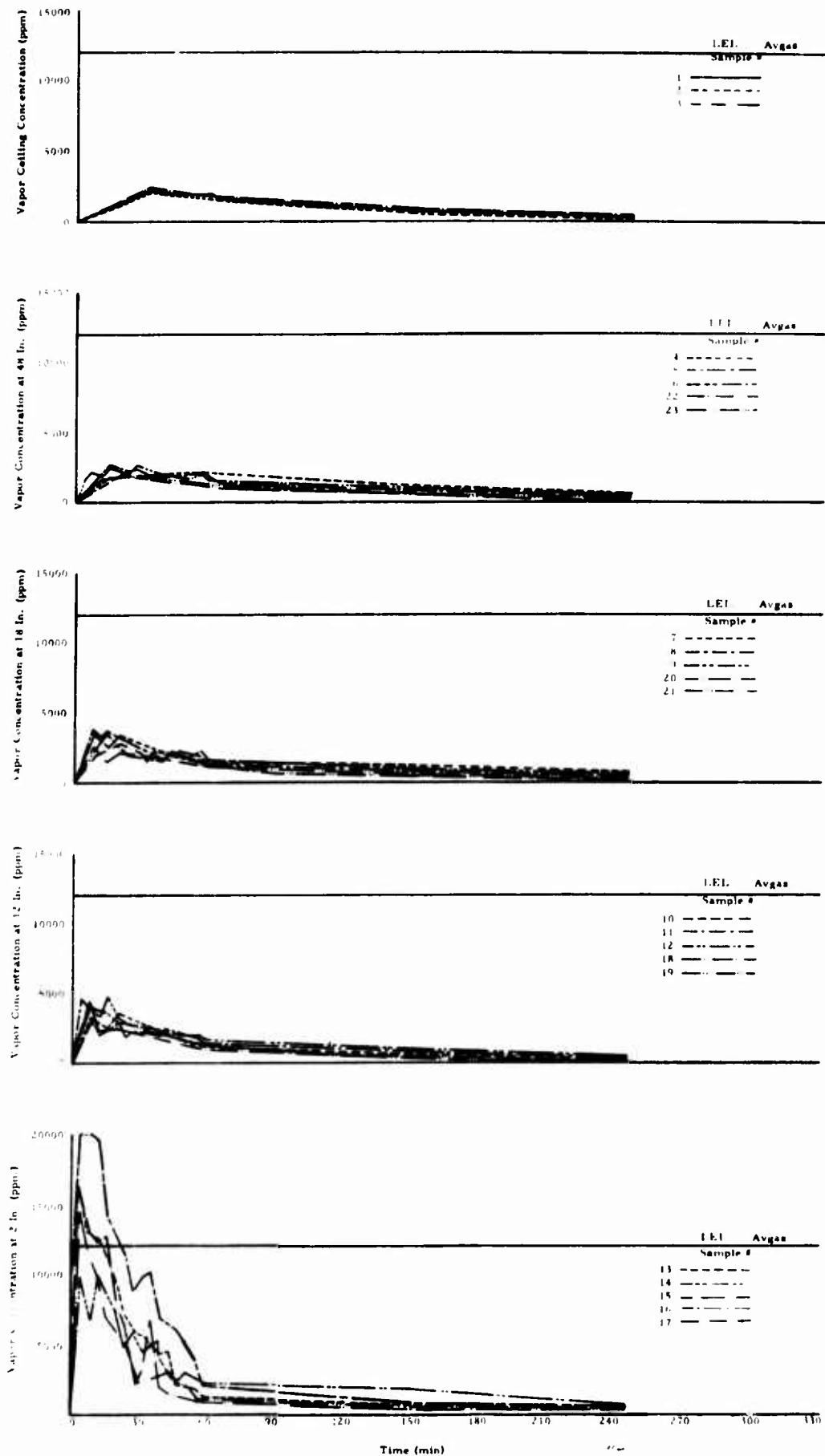


FIGURE III-15. TEST NO. 15—FOUR GALLONS OF AVGAS IN A SPILL TEST

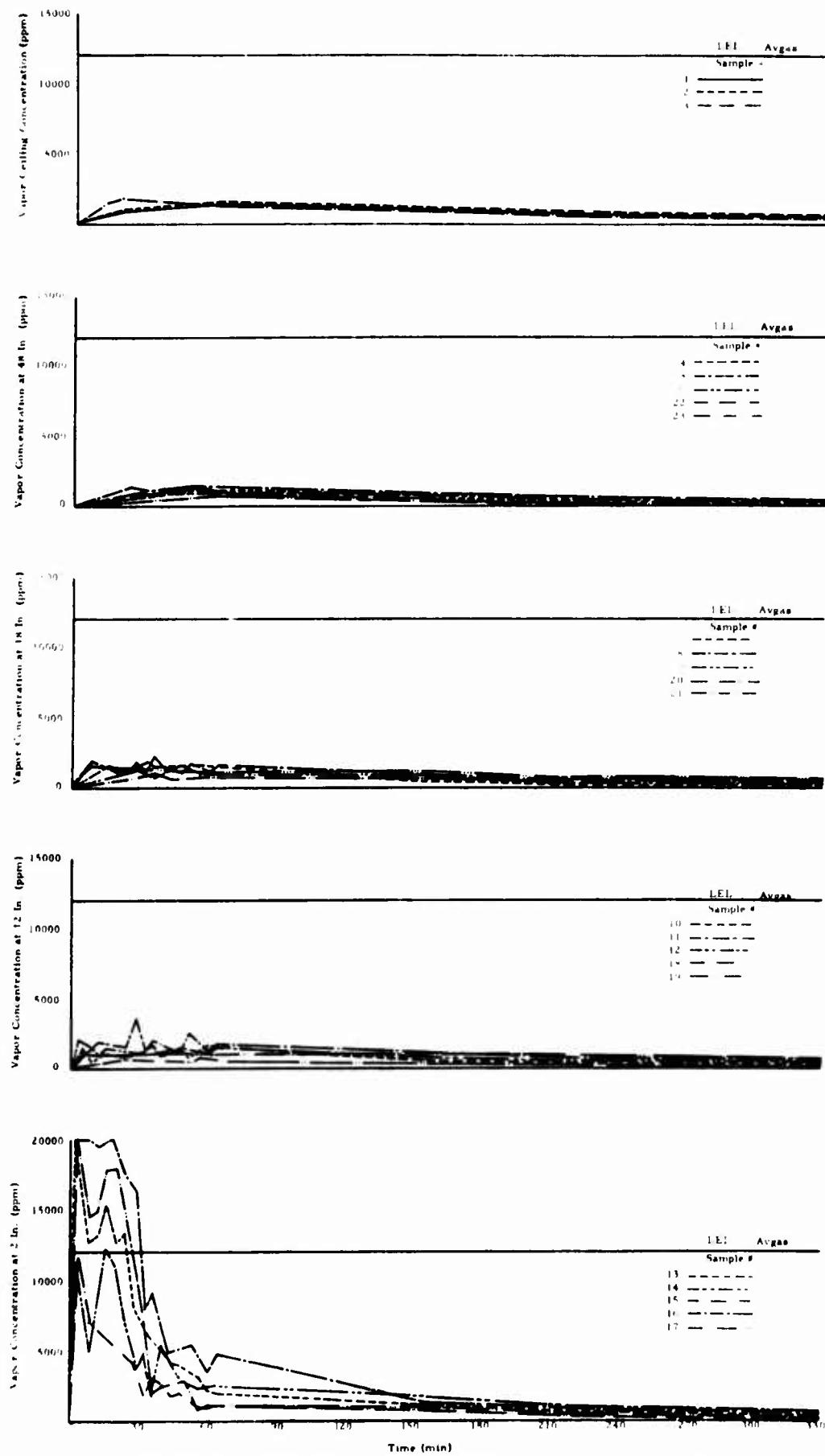


FIGURE III-16. TEST NO. 16—TEN GALLONS OF AVGAS IN A SPILL TEST

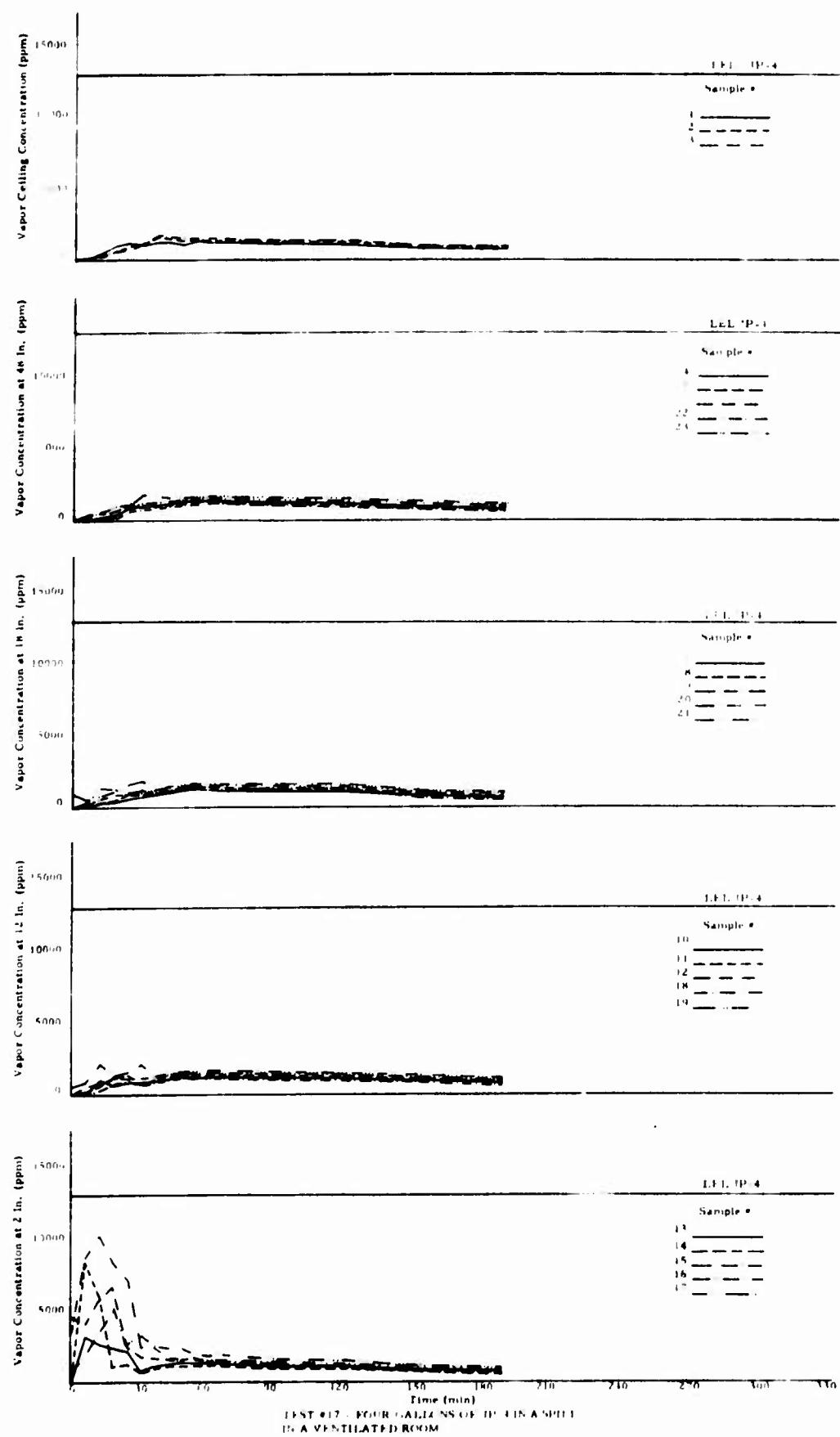


FIGURE III-17. TEST NO. 17--FOUR GALLONS OF JP-4 IN A SPILL TEST

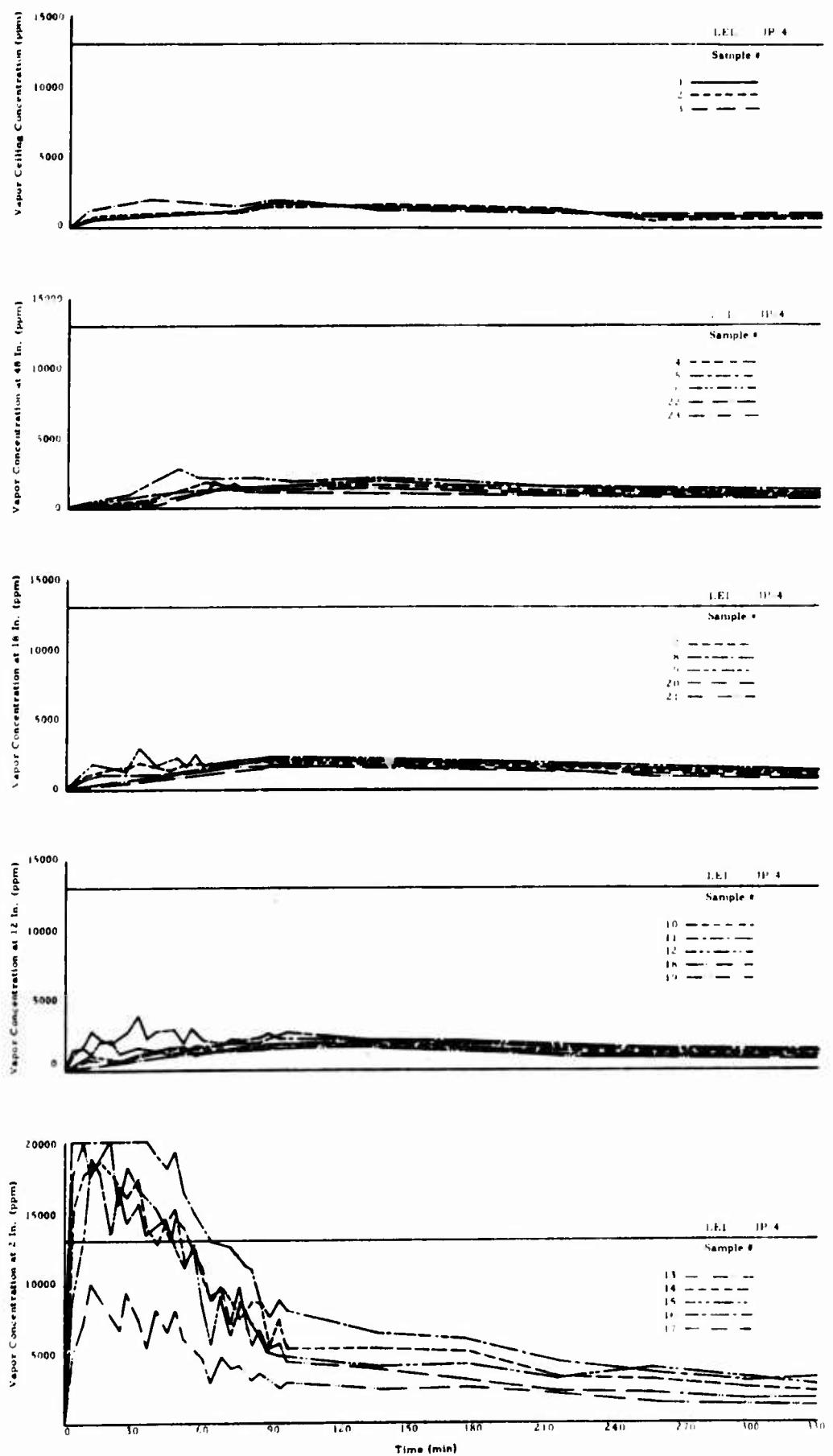


FIGURE III-18. TEST NO. 18—TEN GALLONS OF JP-4 IN A SPILL TEST

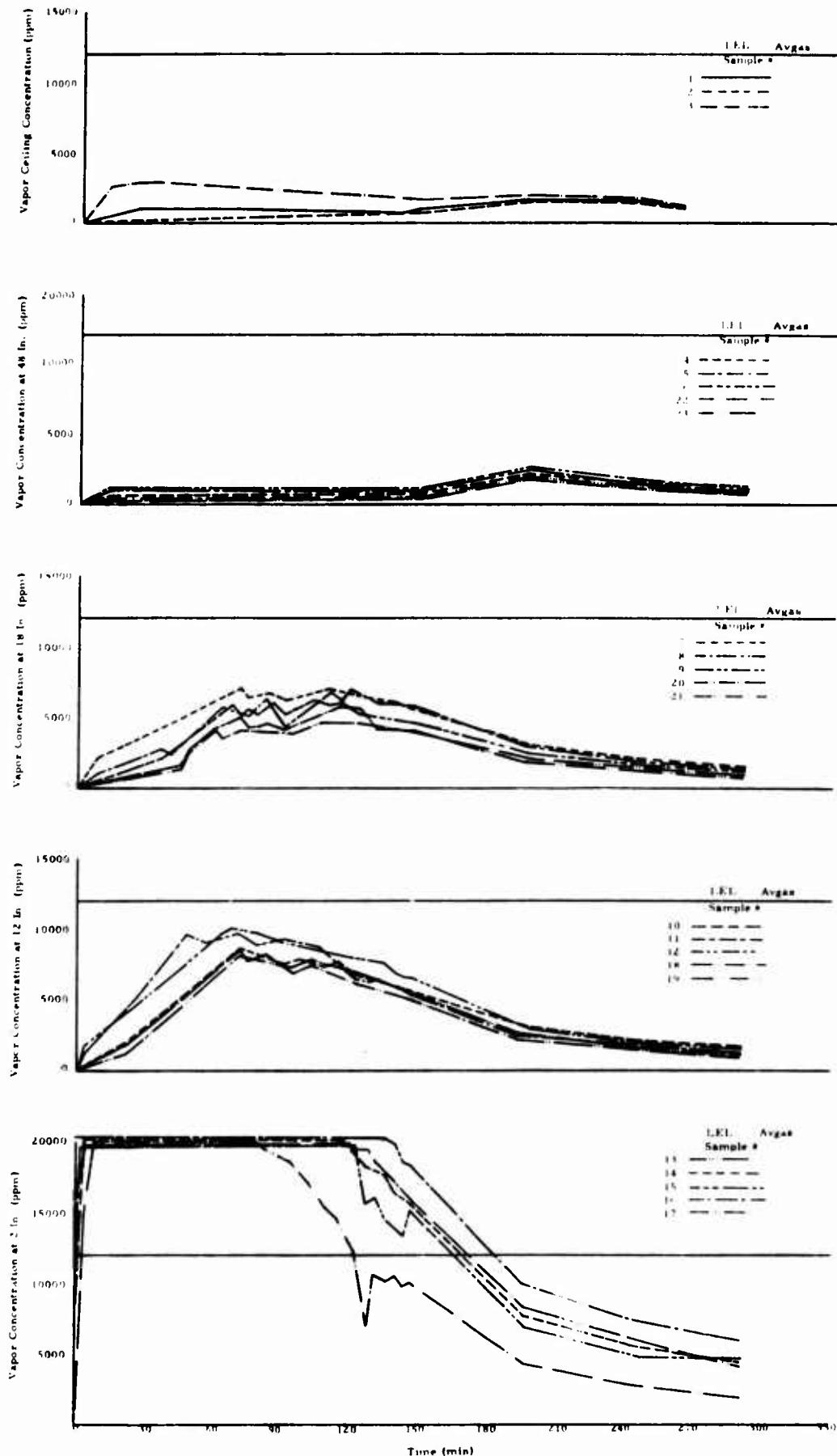


FIGURE III-19. TEST NO. 19—FOUR GALLONS OF AVGAS IN A SPILL TEST

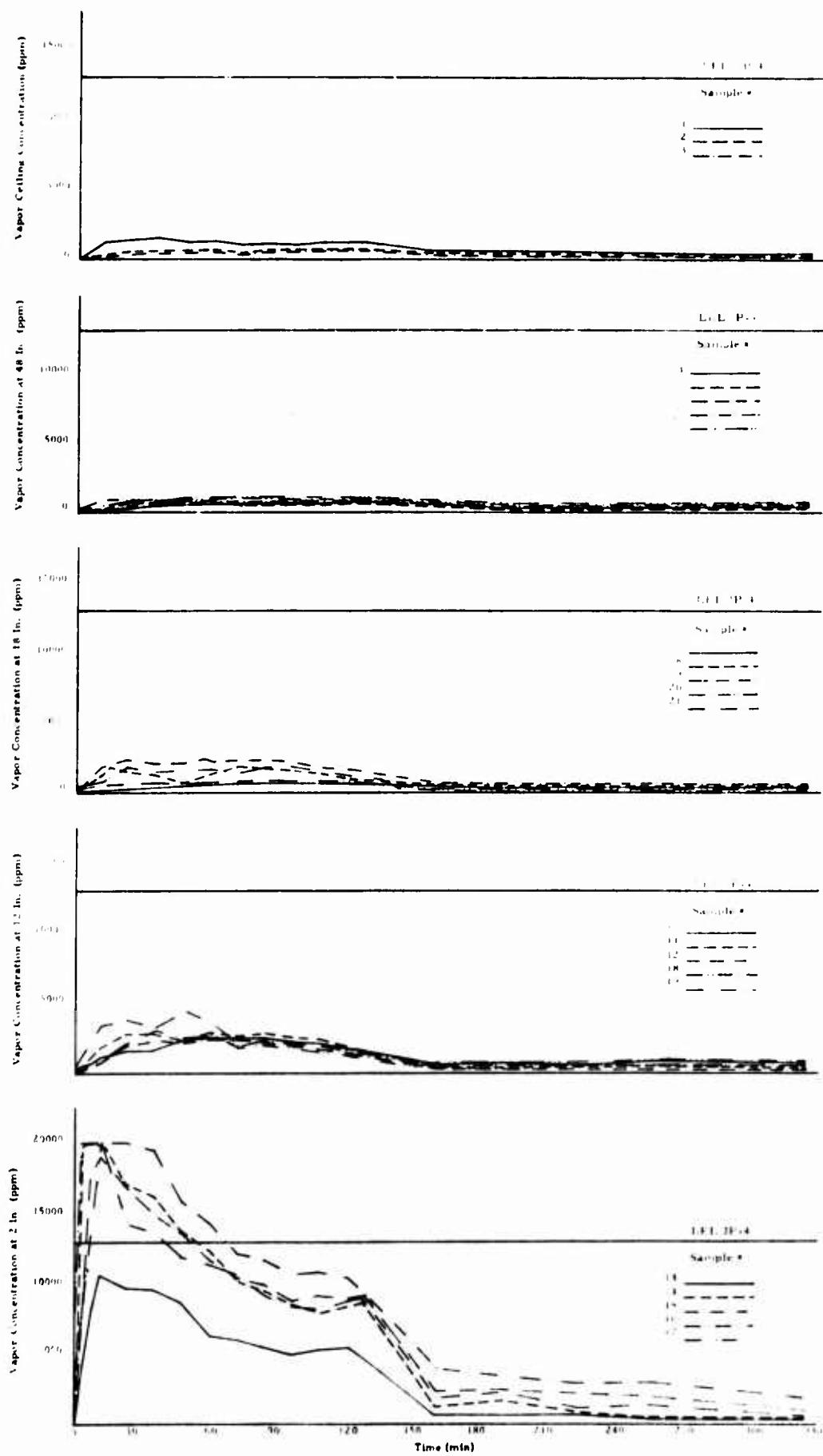


FIGURE III-20. TEST NO. 20 - FOUR GALLONS OF JP-4 IN A SPILL TEST

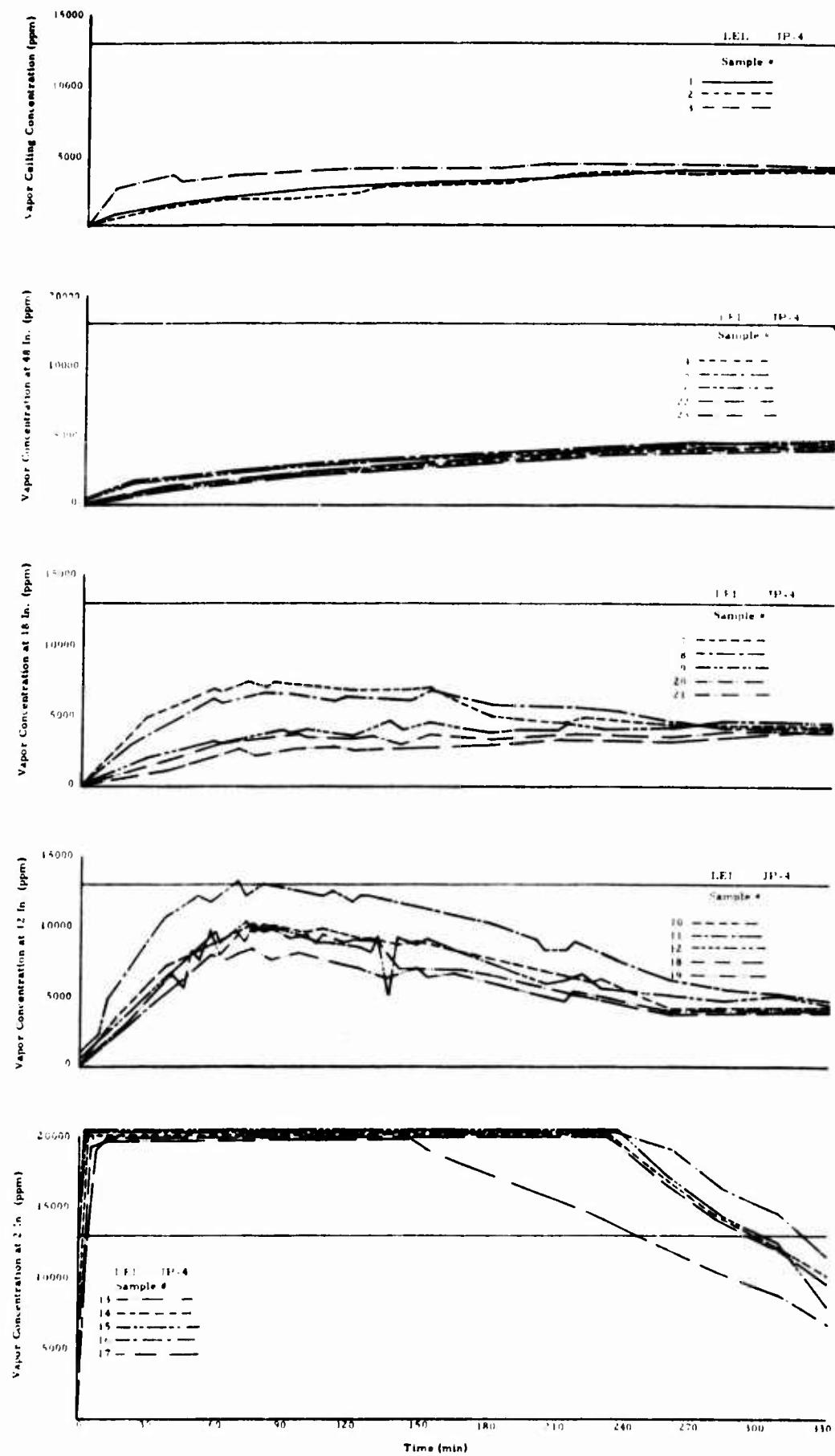


FIGURE III-21. TEST NO. 21 - FOUR GALLONS OF JP-4 IN A SPILL TEST

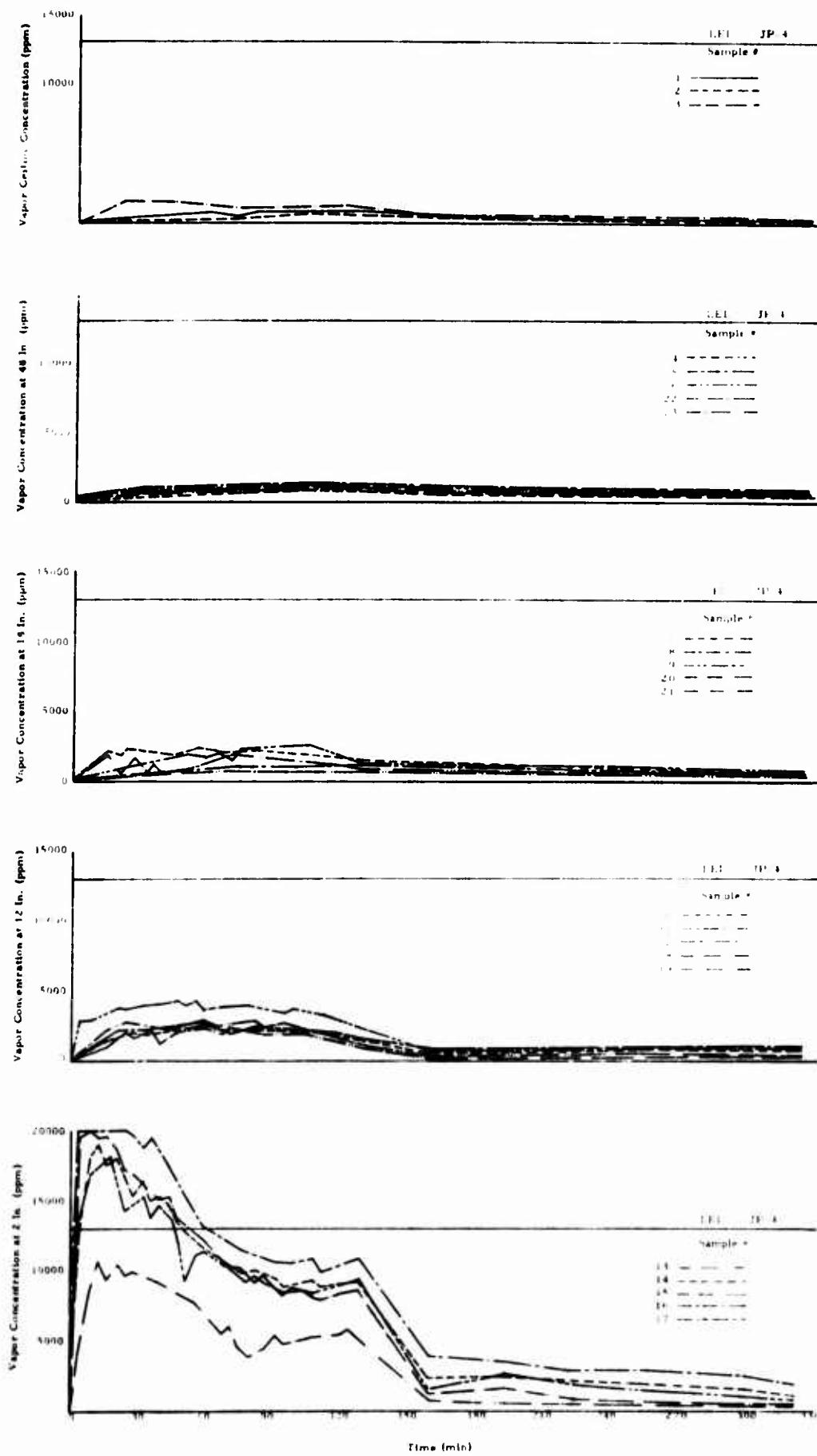


FIGURE III-22. TEST NO. 22 FOUR GALLONS OF JP-4 IN A SPILL TEST

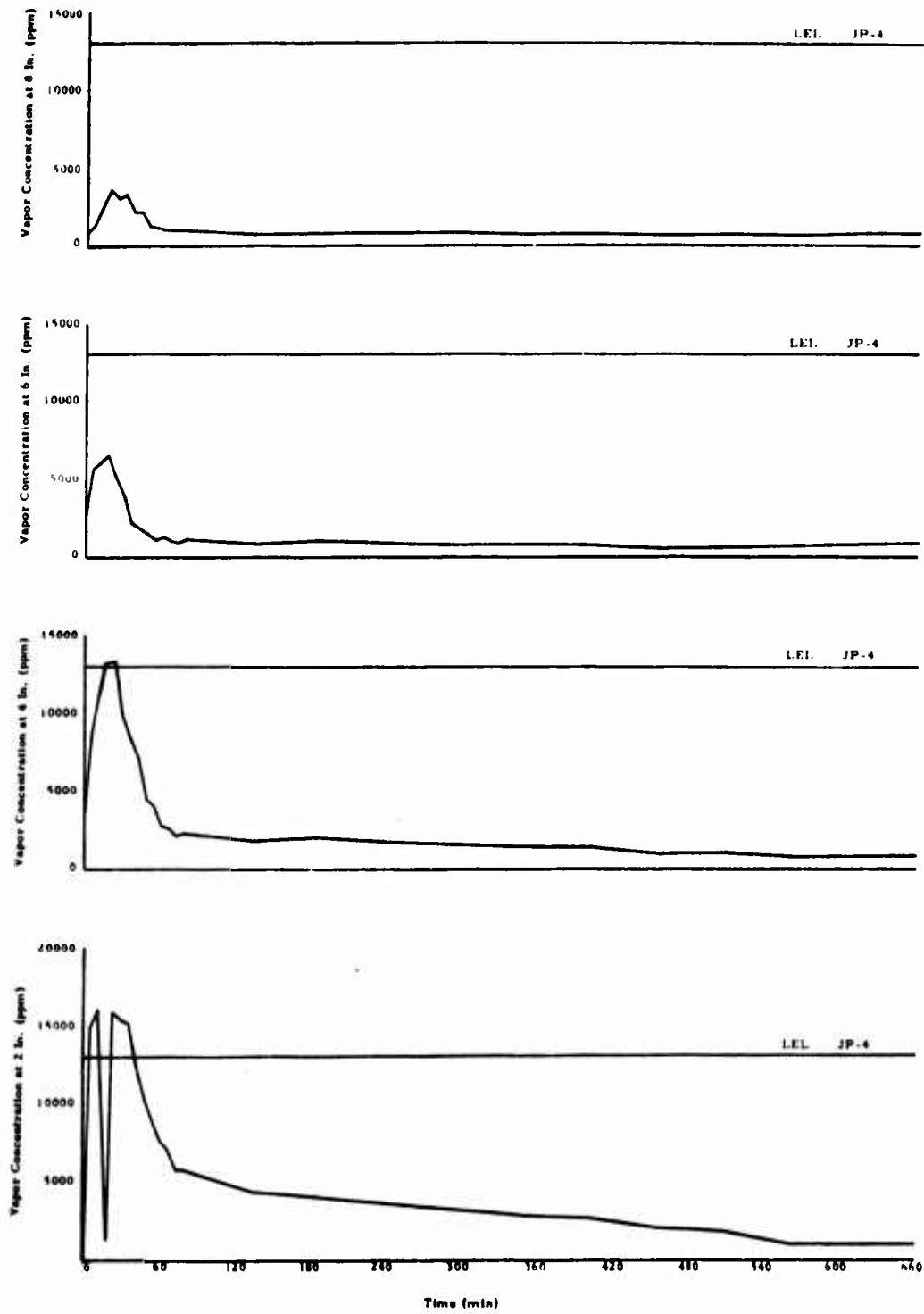


FIGURE III-23. TEST NO. 23 - FOUR GALLONS OF JP-4 IN A SPILL TEST

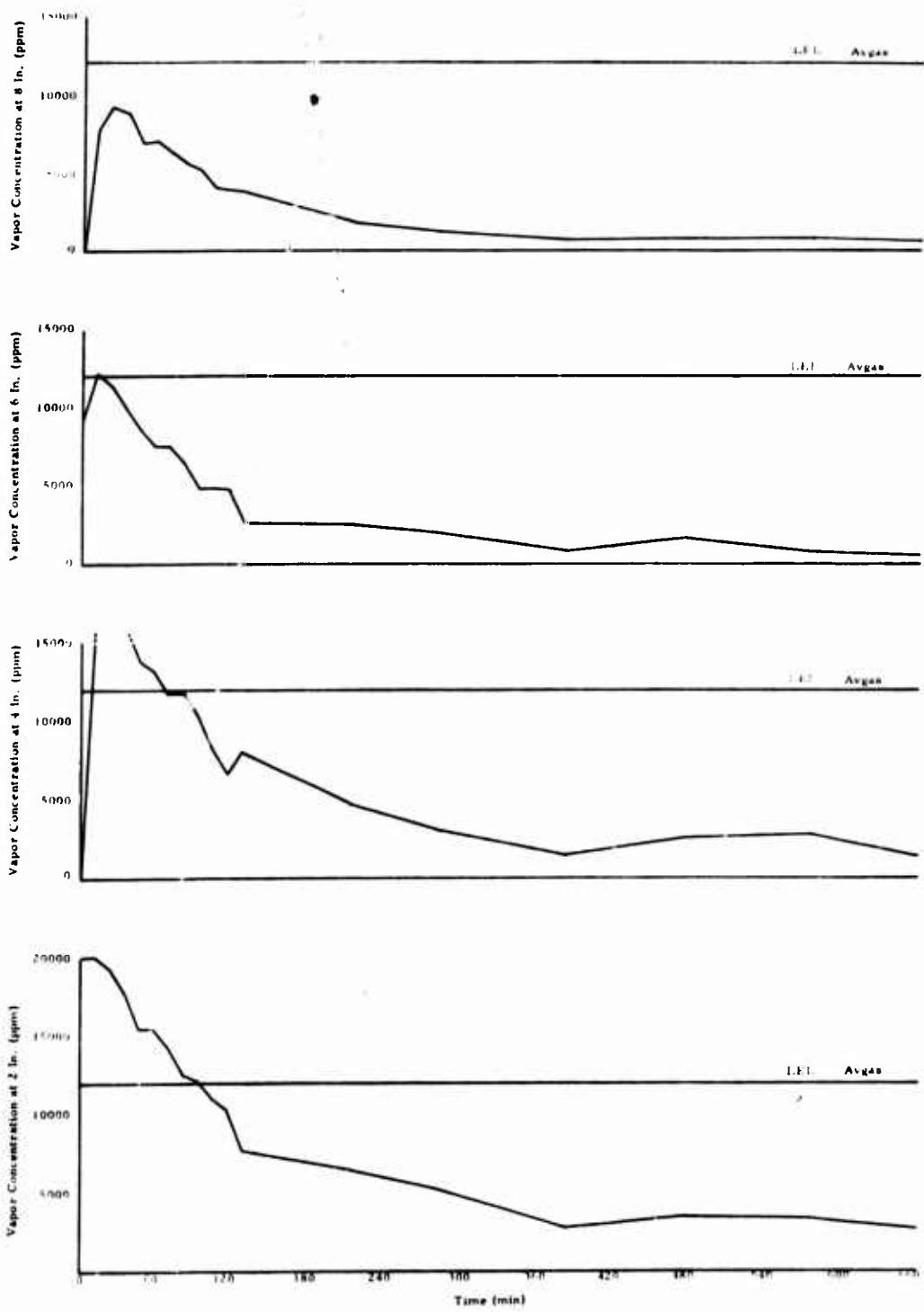


FIGURE III-24. TEST NO. 29—FOUR GALLONS OF AVGAS IN A SPILL TEST

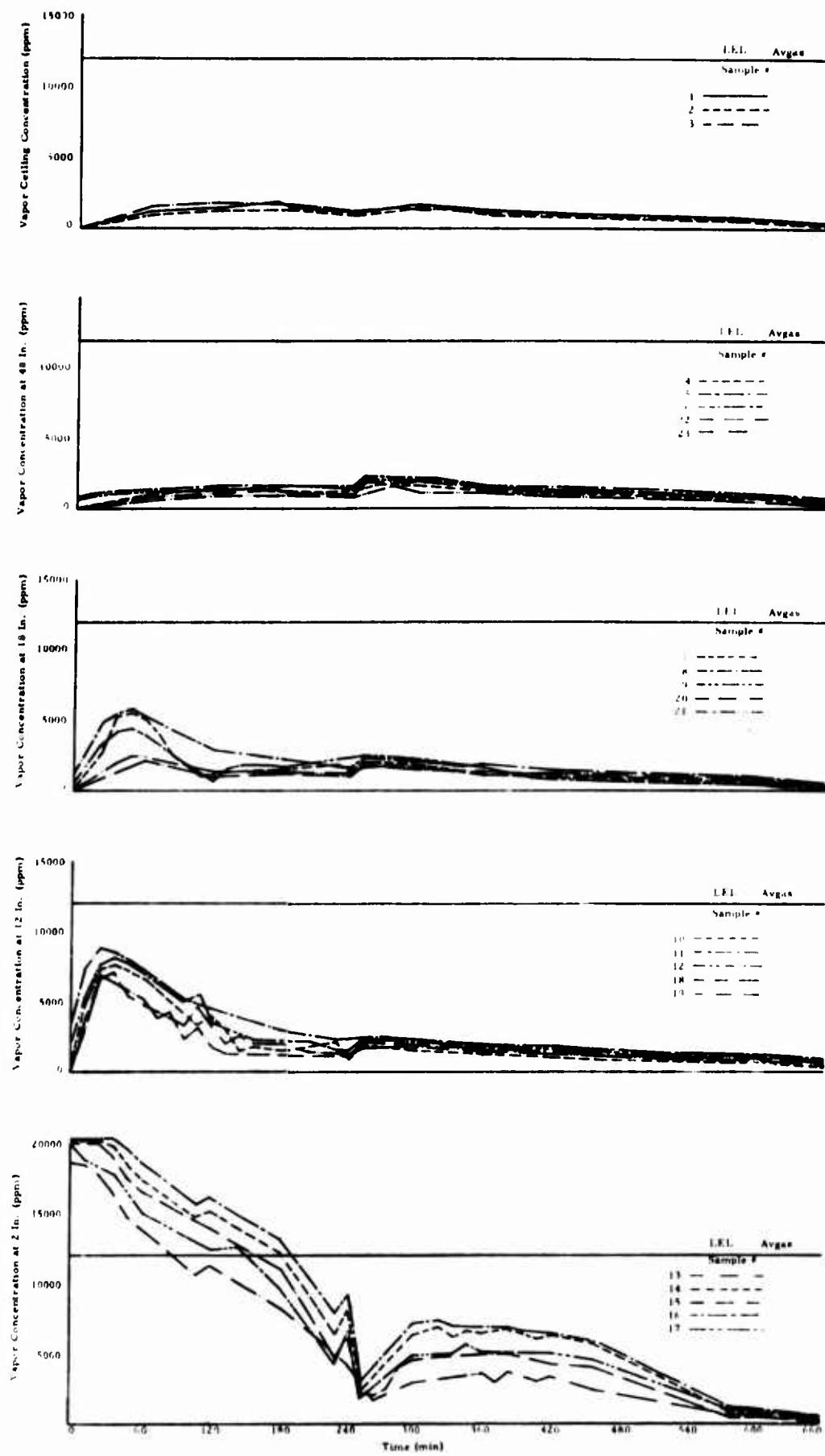


FIGURE III-25. TEST NO. 30—FOUR GALLONS OF AVGAS IN A SPILL TEST

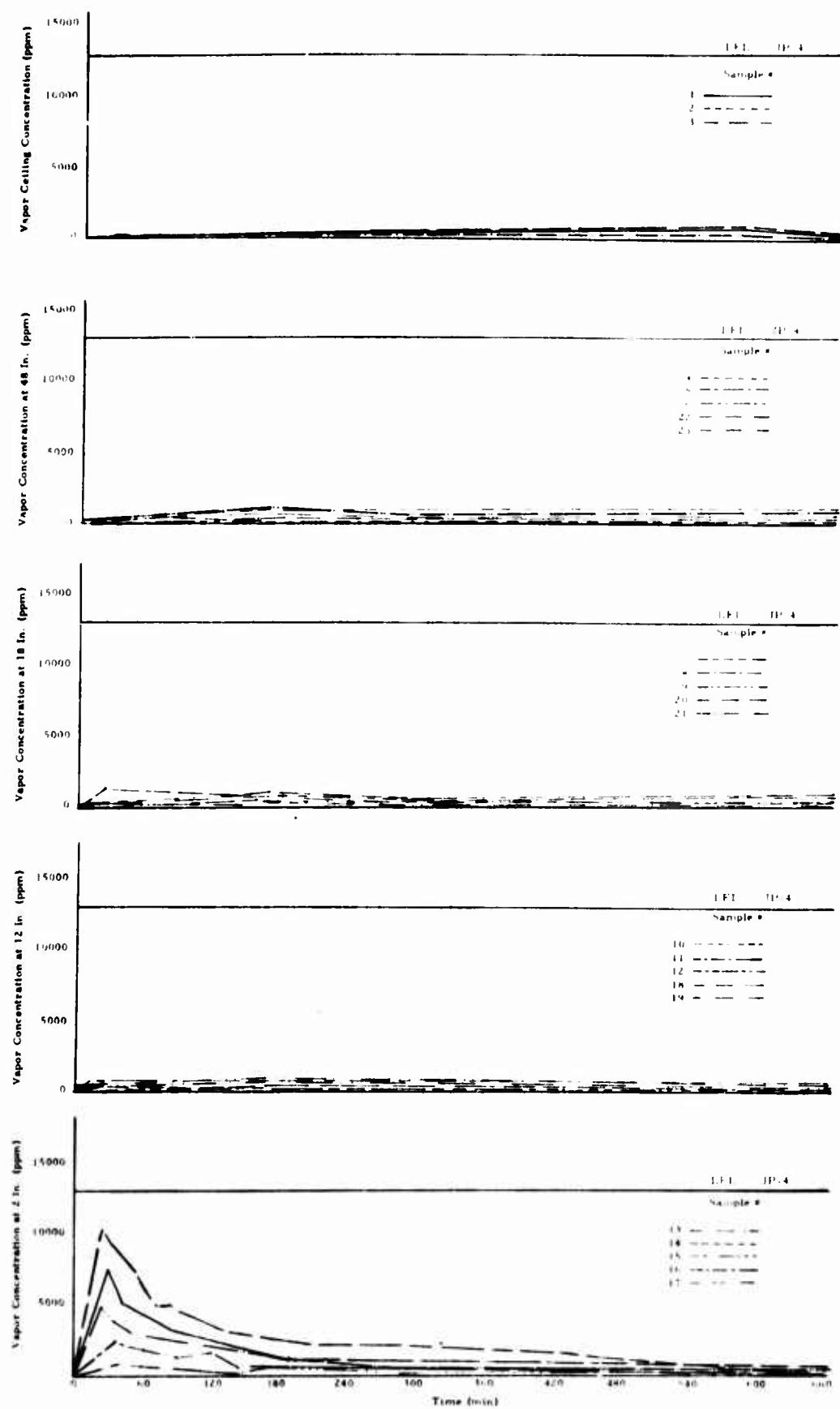


FIGURE III-26. TEST NO. 31-FOUR GALLONS OF JP-4 IN A SPILL TEST

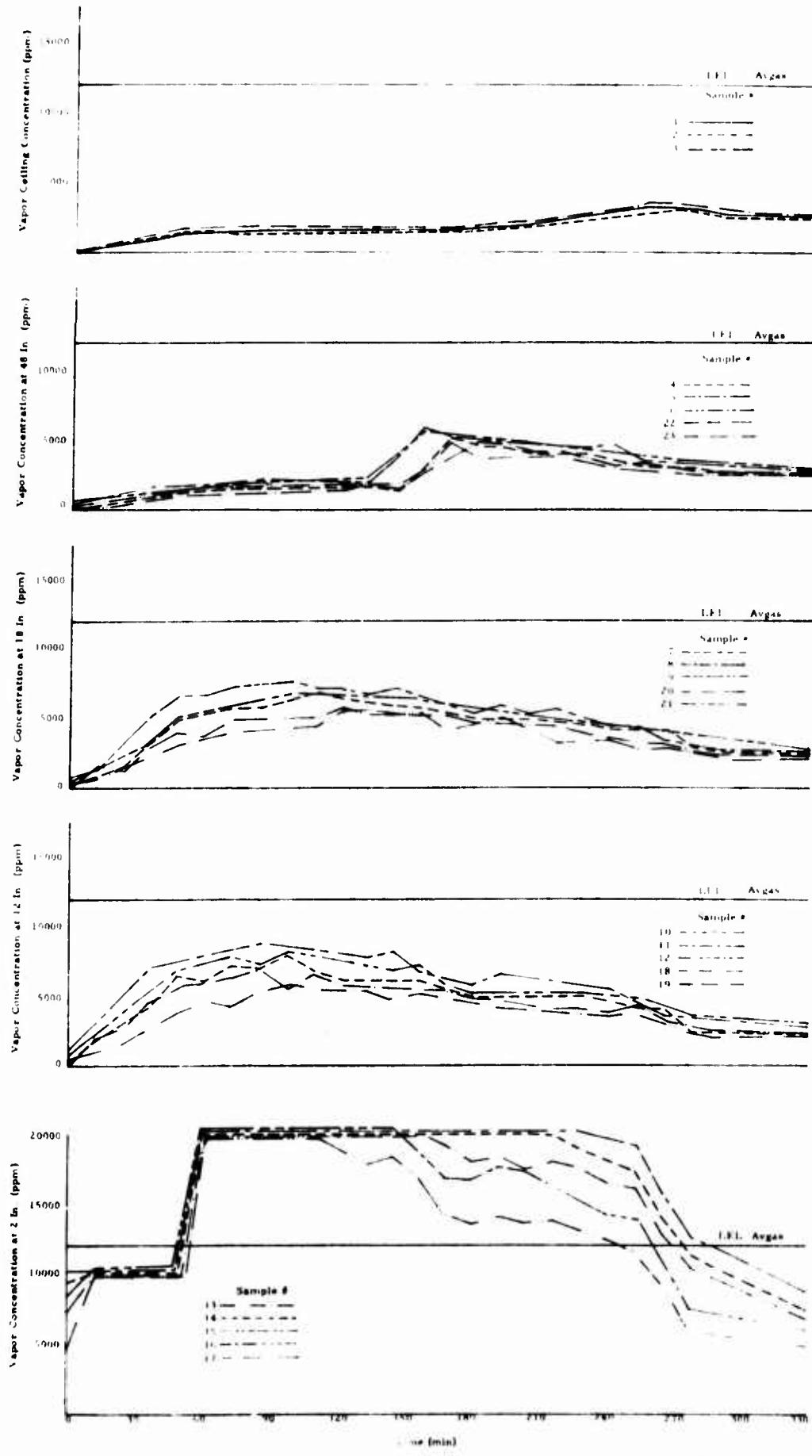


FIGURE III-27. TEST NO. 32-FOUR GALLONS OF AVGAS IN A DRIP TEST

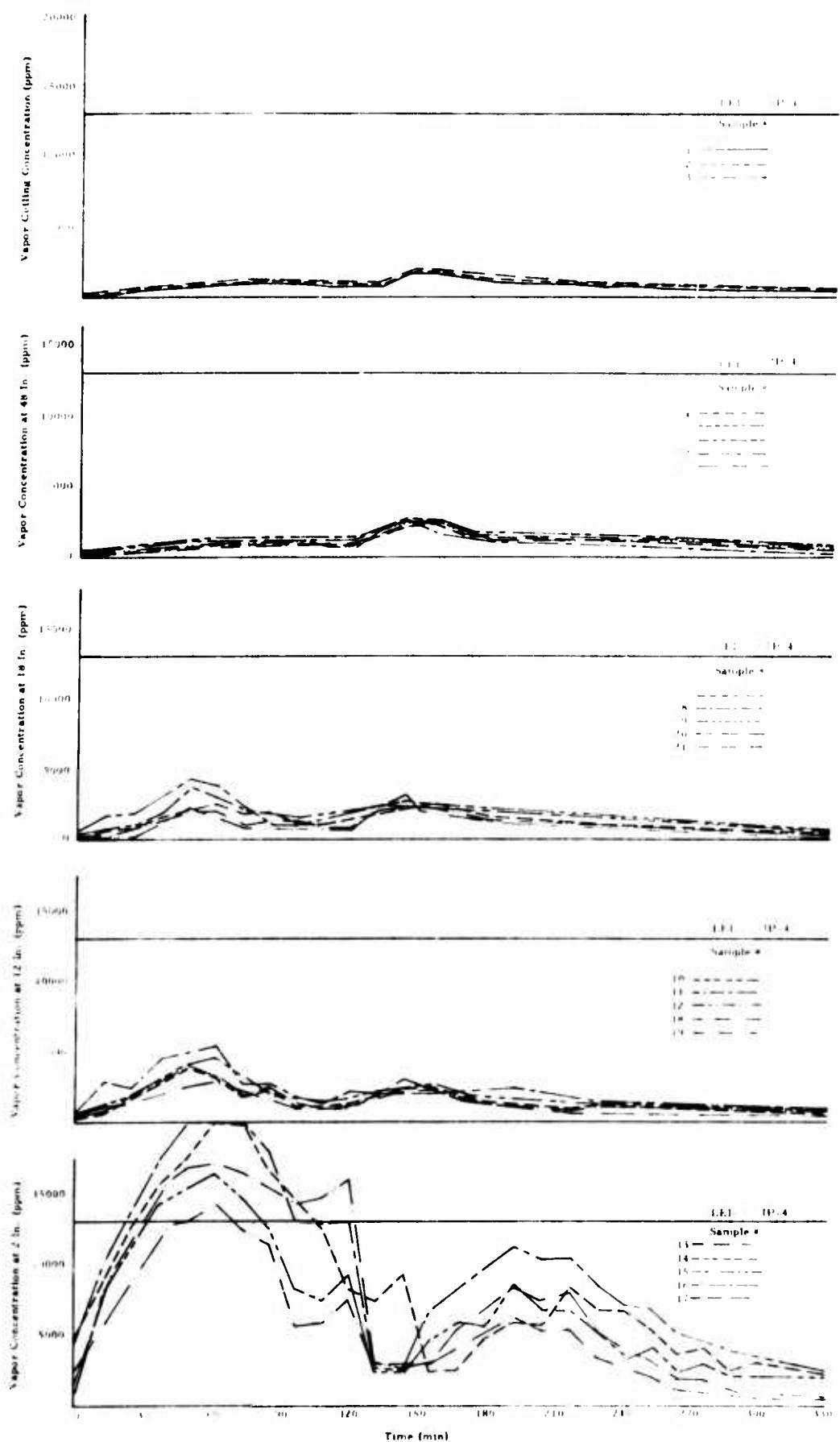


FIGURE III-28. TLST NO. 33. FOUR GALLONS OF JP-4 IN A DRIP TEST

APPENDIX IV

TABLES OF TEST RESULTS

TABLES

Table	Run	Fuel	Temp. °F	Condition
IV-1	1	Avgas	71	1 gal in 6-sq ft pan
IV-2	2	JP-4	73	1 gal in 6-sq ft pan
IV-3	3	Avgas	62	2 gal in 5-sq ft pan
IV-4A	4A	Avgas	64	Fuel from Test 3 spilled on floor
IV-4B	4B	Avgas	63	Continue 4A-floor fan started
IV-5	5	JP-4	66	2 gal in 5-sq ft pan w/fan
IV-6	6	Avgas	71	2 gal in 5-sq ft pan
IV-7	7	JP-4	75	2 gal in 5-sq ft pan
IV-8	8	Avgas	72	2 gal dripped from 5 ft
IV-9	9	JP-4	54	2 gal dripped from 5 ft
IV-10	10	JP-4	71	4 gal dripped from 5 ft
IV-11	11	Avgas	79	4 gal dripped from 5 ft
IV-12	12	Avgas	52	4 gal spilled on floor
IV-13	13	Avgas	98	4 gal spilled on floor
IV-14	14	JP-4	97	4 gal spilled on floor
IV-15	15	Avgas	52	4 gal spilled on floor
IV-16	16	Avgas	60	10 gal spilled on floor
IV-17	17	JP-4	50	4 gal spilled on floor
IV-18	18	JP-4	64	10 gal spilled on floor
IV-19	19	Avgas	67	4 gal spilled on floor
IV-20	20	JP-4	67	4 gal spilled on floor
IV-21	21	JP-4	65	4 gal spilled on floor
IV-22	22	JP-4	77	4 gal spilled on floor
IV-23	23	JP-4	62	4 gal spilled on floor (vertical profile run)
IV-24	24	JP-4	45-66	Hangar 935, Kelly AFB
IV-25	25	JP-4	47-78	Hangar 935, Kelly AFB
IV-26	26	JP-4	45-69	Hangar 5, Randolph AFB
IV-27	27	JP-4	57	55-gal spill, Randolph AFB
IV-28	28	JP-4	46-66	Hangar 4337, Bergstrom AFB
IV-29	29	Avgas	69	4 gal spilled on floor (vertical profile)
IV-30	30	Avgas	82	4-gal spill w/fan
IV-31	31	JP-4	89	4-gal spill w/fan
IV-32	32	Avgas	90	4-gal drip w/fan
IV-33	33	JP-4	85	4-gal drip w/fan
IV-34	34	Avgas	75	4-gal spill (vertical profile)
IV-35	35	JP-4	88	4-gal spill (vertical profile)
IV-36	36	Avgas	88	4-gal spill (vertical profile)
IV-37	37	Avgas	76	4-gal drip (vertical profile)

TABLE IV-1. FUEL VAPOR CONCENTRATIONS IN PPM

Time min*	Sample Point Number ^a																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
6	700	300	200	200	2250	450	600	500	450	150	150	200	1200	250	200	250	200	200	250	200	250	250	250	250
12	1400	600	550	550	950	400	700	750	350	400	400	900	450	600	550	1200	750	550	350	300	250	250	400	650
18	1550	900	1050	900	950	950	500	900	950	600	650	800	800	750	750	1500	1050	550	550	600	600	600	550	550
24	850	850	900	1100	700	600	700	750	1450	1500	1250	1050	700	750	700	950	3350	1100	750	600	650	600	550	750
30	1000	950	1250	1150	1050	800	1250	1350	1200	850	850	1150	1000	800	900	850	1400	850	1100	1000	700	750	750	850
36	850	850	900	900	1650	1250	1200	1250	1250	800	950	1150	1150	1250	1100	900	1000	1350	850	1050	1050	850	850	850
42	1900	1800	1600	1400	1450	1050	1150	1150	1400	850	1100	1150	1250	1150	1050	1050	1250	850	1100	1200	900	850	850	1100
48	300	1050	1250	1200	1050	950	1100	1150	2250	400	1100	1200	1150	1200	1100	1050	850	750	1200	900	1000	1000	1150	1150
54	950	1100	1150	1200	1050	950	1200	1050	1850	1050	1000	1100	1150	950	1200	1000	1050	900	1000	1150	950	950	1000	1100
60	950	1400	1200	1050	1250	1250	850	1150	1350	1400	1250	1300	1550	900	850	1150	850	850	900	800	800	900	900	650
66	450	900	1250	1250	950	1000	1000	1100	900	850	950	950	850	950	1000	850	900	950	1100	800	850	1000	1000	1000
72	1050	1150	1100	1150	950	900	1100	1100	800	900	900	900	950	2300	1400	800	850	800	750	1050	1050	900	950	1000
78	450	1050	1000	1100	1050	950	1200	950	1300	900	1000	950	850	850	950	950	850	850	1150	900	900	1000	950	950
84	1000	1100	1200	1150	1050	950	950	950	950	950	900	900	900	900	900	900	900	900	1150	1100	900	950	950	1050
90	110	1000	1150	1200	1000	950	950	950	1200	900	950	950	900	950	1000	900	850	850	900	1100	900	900	400	1050
96	1250	1000	1100	1130	1000	950	1150	1050	950	1000	900	900	1000	950	950	950	950	950	1100	1100	1100	1100	1100	1100

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min).

TABLE IV-2 FUEL VAPOR CONCENTRATIONS IN PPM

Time minute	Fuel JP-4		Temperature 71°F RH 24%		Sample Configuration No 1		One gallon JP-4 poured into a 6-qt ft pan in the center of the room. 11/4/71.																	
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0																								
4	150	170	200	100	140	140	250	200	140	100	200	140	100	140	100	50	50	50	50	50	50	50	50	50
12	320	350	420	430	460	420	360	170	610	470	1000	550	460	400	400	450	550	550	550	550	550	550	550	550
18	730	430	470	470	470	680	530	450	450	470	1000	550	460	400	400	450	550	550	550	550	550	550	550	550
24	630	600	400	400	400	1050	550	450	450	400	700	540	540	540	540	450	500	450	500	450	500	450	500	450
30	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570	570
36	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830	830
42	1110	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750
48	1300	550	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740	740
54	1360	1050	820	760	1250	540	850	850	1000	810	850	1100	760	770	770	770	770	770	770	770	770	770	770	770
60	850	790	740	1060	780	790	740	1710	800	720	750	400	700	650	780	780	780	780	780	780	780	780	780	780
66	1350	750	630	750	1470	800	300	970	1620	820	700	700	1300	720	720	720	720	720	720	720	720	720	720	720
72	1150	840	820	740	1430	660	750	700	2300	960	750	1100	870	800	850	1250	700	700	700	700	700	700	700	700
78	11700	1100	900	830	1150	910	850	960	1730	940	850	850	850	850	850	850	850	850	850	850	850	850	850	
84	1200	950	850	850	850	1750	1130	940	700	2060	930	770	780	920	950	950	950	950	950	950	950	950	950	950
90	1030	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950	950
96	1100	830	300	300	2370	1130	610	600	1450	600	1460	1000	660	1260	900	1050	1050	1050	1050	1050	1050	1050	1050	1050
102	960	840	820	800	1360	1120	960	450	1240	880	740	1260	770	780	780	780	780	780	780	780	780	780	780	780
108	1300	970	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850
114	1150	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960	960
120	11510	1150	1000	800	1390	930	940	950	1380	1120	1010	940	1120	1120	1120	1120	1120	1120	1120	1120	1120	1120	1120	1120
126	1370	920	860	860	1460	320	870	810	1400	950	960	960	1220	860	860	860	860	860	860	860	860	860	860	860
132	1170	900	900	900	900	1320	1150	1250	1100	1400	950	950	910	900	900	900	900	900	900	900	900	900	900	900
138	1050	1040	960	960	960	300	1440	960	920	900	1240	900	940	1450	400	840	840	840	840	840	840	840	840	840
144	900	900	900	900	900	1220	540	540	540	540	1680	1680	1680	1680	1680	940	940	940	940	940	940	940	940	940
150	800	740	730	500	800	800	450	810	730	800	450	800	750	810	800	800	800	800	800	800	800	800	800	800
156	902	400	890	790	1110	540	750	780	250	350	140	780	750	780	780	780	780	780	780	780	780	780	780	780
162	902	400	890	790	1110	540	750	780	250	350	140	780	750	780	780	780	780	780	780	780	780	780	780	780
210	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650

^aThe time shown corresponds to Sample Point No 1. Each sample point beyond No 1 is spaced 15 sec (e.g. Sample Point No 2 is 30 sec. Sample Point No 20 is 300 sec or 5 min)

Test 3 Conditions: Fuel - avgas. Temperature - 62°F R.H. - 60% Sample Configuration No. 1. Two gallons of avgas poured into a 5-sq ft pan in the center of the room. 11/8/71.

TABLE IV-3 FUEL VAPOR CONCENTRATIONS IN PPM
Sample Point Numbers

Time (min)	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	450	0	650	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	100
6	450	50	0	0	0	50	0	50	0	0	50	0	50	50	50	50	50	50	50	50	50	50	50	100
12	250	100	50	200	50	50	50	50	50	100	50	100	100	100	100	100	100	100	100	100	100	100	100	
18	685	170	200	180	170	180	165	190	205	190	215	185	170	175	215	210	210	205	230	220	220	225	225	
24	300	320	255	265	260	255	260	220	235	250	210	230	230	265	265	305	280	270	255	300	245	245	245	285
30	545	275	550	300	315	305	305	300	310	325	310	320	320	340	345	345	275	270	270	300	300	300	300	300
36	625	320	310	320	305	290	275	290	320	325	285	270	310	305	285	300	325	310	305	310	335	320	320	330
42	740	315	320	335	330	345	335	300	325	290	290	340	340	350	335	315	350	330	315	295	355	345	345	345
48	580	355	425	370	375	365	365	370	350	370	375	375	375	370	330	350	345	355	325	375	355	355	355	355
54	725	335	320	365	335	335	325	345	330	340	350	365	365	365	345	375	380	415	370	320	340	340	340	400
60	570	375	380	425	505	395	390	415	430	425	420	355	400	380	410	460	420	410	355	415	425	425	410	475
66	540	400	405	420	510	440	430	435	435	440	440	480	425	435	420	180	470	435	465	510	490	510	495	515
72	420	525	470	545	475	465	450	450	475	450	445	445	470	460	415	495	470	495	470	425	530	575	570	540
78	505	420	515	500	460	440	440	460	465	475	520	470	465	495	500	530	470	515	520	435	52	500	500	500
84	720	450	480	495	530	500	515	490	470	485	505	465	460	470	510	555	475	470	435	495	43	545	560	
90	1000+	605	475	530	565	510	515	685	510	515	505	505	515	515	515	515	500	555	500	535	535	510	510	500
96	355	550	510	480	455	460	515	490	515	470	445	465	415	420	460	520	485	440	505	585	585	470	470	435
102	1000+	500	435	575	475	495	500	510	505	490	540	540	555	555	555	555	560	570	555	560	555	715	730	
108	925	580	605	585	670	540	555	570	540	505	530	710	555	535	535	535	530	540	545	545	545	545	545	
114	1000+	550	555	580	1000+	615	615	560	560	525	515	525	515	525	515	515	530	500	500	500	500	500	500	500

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 15 sec or 5 min.)

VAPOR CONCENTRATIONS IN ppm

Two stations of avian weathering front were dumped onto the floor of the particle saturation No. 4 at K 14 51%.

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TABLE IV-4b FUEL VAPOR CONCENTRATIONS IN PPM

Test 4B Conditions: Fuel - avgas. Temperature - 53°F. R.H. - 75%. Sample Configuration No. 1. Fans were turned on at the end of Test 4A in which two gallons of avgas that had weathered in Test 3 were dumped onto the floor. 11/8/71.

Time (min.)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	920	900	950	950	900	850	850	800	800	750	700	700	700	660	690	680	635	555	560	565	555			
6	535	545	550	550	510	500	490	475	465	445	465	435	425	415	410	380	370	360	355	295	320	315	311	
12	310	310	305	305	320	295	305	300	295	275	275	265	265	240	230	230	220	210	215	180	185	180	180	
18	200	185	180	185	200	185	170	195	175	175	175	165	175	160	150	155	145	140	135	130	115	105	115	105
24	130	120	120	120	135	120	110	110	130	110	110	110	105	95	95	100	95	90	95	85	75	80	80	
30	100	90	90	95	95	90	90	105	90	105	95	95	80	90	90	80	70	70	80	75	70	75	70	
36	90	80	80	80	90	85	85	80	90	95	85	75	90	85	85	80	80	75	70	70	70	70	70	
42	85	75	80	80	100	80	85	85	80	80	85	80	80	85	70	70	75	80	70	70	70	70	70	
48	80	75	75	70	80	70	70	70	80	70	75	65	80	70	70	70	70	65	60	55	60	55		
54	75	65	70	65	70	60	60	60	70	60	65	70	70	65	65	65	65	65	50	55	50	55		
60	60	55	55	60	50	50	50	50	50	50	55	50	45	40	45	40	40	40	40	40	40	40		
66	50	50	50	50	50	45																		

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min.)

TABLE IV-5 FUEL VAPOR CONCENTRATIONS IN PPM

Test 5 Conditions: Fuel - JP-4, Temperature - 66°F, R H - 76% Sample Configuration No. 1. Two gallons of JP-4 in 5-eq ft pan in the center of the room, the fuel was not dumped onto the floor, but the blowers were turned on.

Time (min)*	Sample Point Number																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
6	5	5	10	10	5	5	5	10	10	5	5	0	0	0	0	0	0	0	0	0	0	0	0	0
12	110	200	50	355	30	30	35	65	40	35	30	40	45	50	60	50	70	45	30	30	50	50	50	50
18	105	40	45	55	50	35	45	40	25	40	40	40	55	50	35	35	65	45	35	55	70	60	70	70
24	130	100	60	60	70	60	45	70	50	45	65	55	70	60	45	60	85	60	45	45	95	80	75	85
30	260	120	95	70	55	75	65	75	90	95	60	100	95	70	65	55	90	70	90	70	90	100	95	100
36	265	70	75	75	95	95	75	80	70	80	90	100	110	105	70	110	105	70	60	110	100	85	105	85
42	410	135	90	95	80	70	90	90	120	95	95	95	110	115	90	90	120	90	105	70	120	115	105	120
48	335	65	75	60	70	85	90	95	95	100	80	75	100	85	65	55	115	95	70	80	120	110	90	80
54	125	90	80	95	135	115	100	75	110	115	75	75	85	120	100	100	95	140	125	105	100	140	125	105
60	405	85	80	80	115	125	95	85	120	100	85	95	95	130	105	95	75	130	90	95	70	120	115	105
66	180	110	80	85	140	125	100	95	140	145	60	70	120	100	90	100	125	110	105	105	135	85	120	165
72	355	185	95	85	135	135	130	90	155	120	75	65	135	120	85	90	125	115	70	95	105	105	110	110
78	250	110	80	95	120	105	75	70	85	90	90	95	110	80	70	105	115	105	110	75	120	115	95	115
84	410	145	85	65	95	100	85	85	105	115	125	90	120	80	40	60	135	110	70	90	125	115	105	100
90	365	115	105	135	225	125	100	85	90	80	90	110	100	100	90	50	85	40	40	45	100	100	95	100
96	475	155	80	55	155	120	60	60	200	70	65	65	125	115	100	95	100	100	70	75	105	90	65	95
102	150	60	55	55	110	115	185	60	110	100	85	65	130	105	80	90	130	115	100	105	150	150	75	85
108	370	220	150	105	190	80	75	30	115	105	105	75	135	95	70	55	110	60	60	55	110	100	100	105
114	195	100	75	80	150	110	110	105	105	75	40	60	100	55	75	80	75	85	85	85	85	85	85	85

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec or 5 min)

TABLE IV 6 FUEL VAPOR CONCENTRATIONS IN PPM

Test 6 Conditions Fuel - avgas Temperature - 71°F RH - 41%. Sample Configuration No. 2. Two gallons of avgas in a 5-sq ft pan in the center of the room, the run was made to coordinate the sample configuration with that used in Tests 1-5 11/10/71.

Time (min.)	Sample Point Number													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
6	160	250	50	0	50	0	0	0	0	0	0	0	0	0
12	100	150	100	50	100	50	50	50	50	50	50	50	50	50
18	150	150	150	100	100	50	50	100	50	100	100	100	100	100
24	150	200	150	100	150	100	100	100	100	100	100	100	100	100
30	200	250	200	150	150	150	150	150	150	150	150	150	150	150
36	200	250	150	200	200	150	150	200	200	150	150	150	150	150
42	250	300	250	250	250	200	200	150	200	150	150	150	150	150
48	250	250	250	250	250	250	250	250	250	250	250	250	250	250
54	250	300	300	310	310	310	310	310	310	310	310	310	310	310
60	300	420	320	365	365	320	325	310	320	320	320	320	320	320
66	335	300	360	395	395	355	355	355	355	355	355	355	355	355
72	370	410	310	405	375	365	330	360	320	320	320	320	320	320
78	350	325	400	400	410	375	360	320	310	350	330	365	310	375
84	325	430	330	425	425	390	365	365	360	340	330	355	290	435
90	315	365	310	425	425	405	3845	325	350	335	330	315	365	275
96	335	370	355	370	415	415	400	375	375	355	355	360	360	355
102	345	350	375	430	430	410	410	410	405	375	375	350	350	345
108	375	395	340	455	475	440	360	380	355	320	360	315	395	335
114	350	375	360	400	455	440	405	390	330	310	365	315	340	375
120	365	375	365	400	425	440	425	470	340	375	360	355	395	415
126	380	375	385	480	460	425	425	425	370	350	425	365	370	425
132	375	385	375	480	465	450	415	415	345	345	405	405	425	515
138	340	405	405	445	445	440	440	475	375	375	445	445	445	445
144	335	415	405	485	550	475	395	455	425	425	445	435	475	495
150	400	400	405	405	510	500	460	450	430	430	430	400	400	400
156	435	435	430	440	570	535	515	450	450	450	450	450	450	450
162	470	470	490	530	540	530	500	470	470	470	470	470	470	470
168	435	480	465	425	525	575	575	435	435	435	435	435	435	435
174	460	405	405	445	445	445	445	445	435	435	435	435	435	435
180	455	505	510	585	550	415	520	500	455	415	500	470	500	420
186	500	470	58	545	515	510	530	520	500	445	430	520	520	425
192	475	470	545	545	625	545	545	545	545	545	545	545	545	545
198	475	510	500	500	550	510	510	510	510	510	510	510	510	510
204	505	505	505	505	570	685	685	575	575	575	575	575	575	575
210	495	515	500	560	620	705	705	645	645	645	645	645	645	645
216	440	500	485	785	605	525	620	610	600	570	565	585	585	605
222	520	520	445	650	700	720	145	610	610	580	580	580	580	580
228	445	515	625	640	650	585	585	620	620	620	620	620	620	620
234	440	450	455	620	615	640	640	640	640	640	640	640	640	640

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec or 5 min.)

TABLE IV / FUEL VAPOR CONCENTRATIONS IN PPM

Test 7 Conditions: Fuel - JP-4. Temperature - 75°F. R.H. - 39%. Sample Configuration No. 2. Two gallons of JP-4 in 5-eq ft pan in the center of the room. the run was made for the same purpose as Test 6 using JP-4. 11/10/71.

Time (min)*	Sample Point Number																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	0	200	0	0	0	0	0	0	0	0	0	100	150	200	100	0	
6	0	0	0	0	0	0	0	0	100	50	50	0	0	0	0	0	0	0	0	50	0	0	0	0	
12	120	100	110	175	120	210	225	200	205	170	165	140	160	190	1000+	650	1000+	370	290	280	340	335	280	50	
18	195	170	150	180	160	215	215	255	275	255	220	220	185	185	1000+	830	1000+	355	350	370	340	390	445	50	
24	240	200	180	335	195	270	255	265	285	270	250	255	215	260	1000+	590	1000+	415	290	340	385	305	430	50	
30	260	230	210	335	250	375	290	305	305	290	285	275	270	270	1000+	1000+	1000+	365	330	380	435	485	360	55	
36	290	260	230	310	335	355	300	300	355	315	330	265	315	310	1000+	915	1000+	550	370	440	430	420	370	60	
42	260	250	240	380	335	365	350	340	345	340	350	350	330	380	1000+	915	1000+	450	370	455	490	475	470	60	
48	305	325	315	340	335	355	355	355	380	360	355	340	345	360	1000+	820	745	460	390	420	520	440	480	60	
54	345	340	410	325	385	400	385	380	395	385	375	375	355	385	1000+	795	735	515	455	455	495	425	560	60	
60	345	345	340	360	405	430	405	415	410	385	390	385	385	385	1000+	985	705	450	455	435	445	500	560	65	
66	380	370	365	475	450	460	415	415	465	460	405	395	405	415	1000+	815	775	435	375	375	480	510	535	65	
72	420	410	400	455	450	475	405	420	415	400	410	355	420	435	1000+	790	835	525	425	490	585	510	575	60	
78	410	410	390	400	405	435	430	440	455	455	430	410	430	440	1000+	905	630	665	470	455	495	480	460	60	
84	390	395	390	435	460	470	425	450	440	475	420	370	425	435	1000+	970	950	515	490	520	480	540	475	60	
90	420	360	365	490	385	490	440	455	525	415	425	420	420	440	1000+	885	510	430	425	550	445	500	60		
96	410	425	415	420	445	405	430	445	450	460	390	410	415	425	1000+	950	1000+	475	455	455	535	545	530	60	
102	390	360	350	480	420	455	460	470	480	455	445	415	425	435	1000+	865	1000+	530	480	520	475	445	540	60	
108	365	360	340	475	505	480	435	445	460	455	435	425	435	455	1000+	1000+	905	1000+	515	470	515	535	585	580	60
114	400	420	410	495	480	545	490	480	460	435	435	470	455	490	1000+	930	535	485	495	570	475	500	60		
120	405	430	415	445	440	470	460	515	455	475	495	490	435	460	1000+	905	1000+	515	470	515	535	585	580	65	
126	395	405	550	555	540	470	455	450	435	445	460	460	400+	690	890	520	510	540	600	505	520	520	55		
132	450	455	440	415	510	485	425	500	485	465	435	455	455	425	1200+	1000+	625	480	575	605	525	605	60		
138	410	415	415	570	540	550	490	530	500	490	470	465	485	495	1000+	840	960	750	665	520	555	645	730	65	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min).

TABLE IV-8. FUEL VAPOR CONCENTRATIONS IN PPM

Test & Conditions: Fuel - avgas. Temperature - 72°F. R.H. - 39%. Sample Configuration No. 2. Two gallons of avgas in a can suspended 5 ft above the floor just east of the center of the room and allowed to drip steadily. 11/10/71.

Time (min)*	Sample Point Number													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	0	0	0	0	0	0	0	0	250	400	0	0	0	0
6	0	0	0	50	50	100	150	750	150	50	300	1950	1650	1400
12	50	50	200	150	100	300	200	350	150	2150	4500	1850	650	250
18	100	150	300	350	250	100	200	300	200	3250	5450	2950	6500	300
24	300	300	450	300	300	200	250	400	800	350	300	5350	7900	6500
30	400	400	350	400	350	350	350	650	1100	500	400	5200	7100	850
36	550	600	550	450	400	400	400	650	1500	500	6350	7750	6650	1000*
42	600	650	550	550	450	500	550	600	1300	600	550	9500	7000	1000*
48	700	750	550	550	600	650	1750	2550	850	650	7200	9200	10500	1050
54	800	750	900	650	600	650	700	900	2050	1850	1900	1050	8600	7050
60	850	850	750	650	650	650	950	1050	2400	2800	2950	1400	6200	8150
66	900	850	800	850	750	850	1100	1100	500	400	5200	7100	850	1000*
72	1000	900	900	900	800	850	900	1900	2850	2900	1700	5550	7850	6600
78	1000	900	950	900	1050	1050	1300	2300	2000	1900	1700	4900	7040	9000
84	1050	900	1050	1050	1350	1150	2150	2400	2000	1880	2150	1500	3550	4300
90	1200	1000	1100	2100	2000	1600	2150	2400	2050	1950	1900	1900	4450	4900
96	1350	1300	1350	1900	1650	1750	2100	1650	2100	1700	1650	1750	3250	3200
102	1650	1650	1750	1800	1750	1700	1900	1650	1800	1700	4000	4650	8800	8800
108	1650	1700	1700	1800	1850	1800	1700	1750	2100	1700	6450	8350	6150	1000*
114	1750	1750	1800	1800	1800	1800	1800	1850	2350	2000	1750	4600	7040	9000
120	1950	1950	1850	1800	1750	1850	2200	2050	2050	1950	1900	4450	7000	5550
126	2000	1900	1900	1900	1850	1900	1950	1950	1900	1950	5700	7500	5050	1000*
132	1950	2000	1900	1900	1900	1850	1900	1950	1900	1950	1900	1950	8600	3000
138	2100	2050	1950	2000	1950	2000	1950	2050	2000	2000	2000	2000	8000	8000
144	2100	2100	2050	2000	2000	1950	2050	2100	2250	2150	2050	2050	3200	3250
150	2150	2300	2100	2100	2000	2000	2100	2100	2150	2150	2050	1900	9700	3450
156	2200	2300	2150	2100	2100	2100	2150	2100	2150	2150	2100	2100	3100	2700
162	2250	2200	2150	2100	2150	2200	2200	2200	2250	2200	2200	2200	3100	2700
168	2450	2450	2300	2400	2450	2300	2500	2450	2300	2300	2300	2300	5800	7200
174	2450	2500	2500	2450	2450	2350	2350	2350	2350	2400	2400	2400	4650	6900
180	2550	2500	2450	2400	2400	2350	2350	2400	2450	2500	2450	2450	5150	6350
186	2550	2500	2500	2450	2450	2500	2500	2450	2450	2500	2450	2450	5800	6300
192	2500	2400	2350	2300	2300	2350	2400	2450	2300	2450	2350	2350	5750	7800
198	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	2500	6300	6300
204	2500	2450	2400	2350	2400	2450	2500	2450	2400	2450	2500	2500	5600	5600
210	2450	2400	2450	2350	2350	2250	2250	2100	2150	2400	2300	2300	5450	6950
216	2400	2400	2400	2450	2350	2350	2350	2400	2450	2500	2400	2400	5150	6400
222	2500	2500	2500	2450	2450	2450	2500	2500	2500	2500	2500	2500	5750	9600
228	2600	2550	2550	2550	2550	2500	2500	2500	2500	2500	2500	2500	5550	8700
234	2550	2550	2600	2550	2550	2500	2500	2500	2500	2500	2500	2500	4850	7400
240	2500	2550	2550	2700	2600	2550	2600	2500	2550	2500	2500	2500	5600	7050
246	2550	2550	2650	2600	2600	2550	2700	2700	3000	2200	2200	2200	6450	6250
252	2550	2550	2600	2550	2600	2550	2300	2500	2400	2400	2400	2400	6700	7050
258	2700	2650	2600	2550	2550	2300	2300	2700	2600	2200	2150	2150	6700	6700
264	2500	2450	2500	2500	2300	2350	2150	2100	2350	2200	2200	2200	3250	4850
270	2400	2450	2400	2450	2400	2250	2250	2150	2250	2100	2100	2100	4800	2750
330	1650	1650	1700	1450	1400	1450	1450	1400	1450	1300	1250	1200	3300	4800
390	850	800	900	900	800	750	750	750	750	700	650	700	1400	1400
450	500	500	500	500	500	500	500	500	500	400	400	400	900	900
510	300	300	300	300	300	300	300	300	300	250	250	250	1050	1050
570	150	150	150	150	150	150	150	150	150	150	150	150	150	150
630	100	100	100	100	100	100	100	100	100	100	100	100	100	100
690	100	100	100	100	100	100	100	100	100	100	100	100	100	100
750	50	50	50	50	50	50	50	50	50	50	50	50	50	50
810	50	50	50	50	50	50	50	50	50	50	50	50	50	50

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 3 is 30 sec or 5 min).

TABLE IV 9 FUEL VAPOR CONCENTRATIONS IN PPM

Test 9 Conditions: Fuel - JP-4. Temperature 54°F R.H. 77%. Sample Configuration No. 2. Two gallons of JP-4 in a can suspended 5 ft above the floor just east of the center of the room and allowed to drip steadily. 11/11/71.

Time (min)*	Sample Point Numbers													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
6	0	0	0	0	0	0	0	0	0	0	0	0	0	0
12	115	135	135	85	80	75	70	75	70	75	70	60	60	450
18	200	225	225	145	145	170	150	155	220	290	175	200	160	140
24	330	340	360	255	235	245	230	245	235	260	240	240	230	220
30	425	395	385	325	320	310	315	335	310	345	315	360	345	320
36	515	480	485	420	400	385	410	425	460	415	405	440	435	400
42	640	610	600	530	515	520	475	485	495	500	485	495	510	500
48	720	690	700	635	605	580	575	580	585	500	575	580	585	500
54	790	750	735	680	635	670	630	630	720	685	625	685	670	600
60	745	690	710	690	705	695	665	680	685	645	670	630	670	660
66	835	730	750	740	730	705	725	705	685	705	680	720	715	700
72	850	790	800	780	760	745	725	750	690	660	650	650	680	770
78	78	700	700	650	670	600	650	650	700	650	600	600	600	700
84	700	650	650	750	700	650	650	650	650	700	650	650	650	650
90	700	700	800	700	750	700	700	700	700	700	700	700	700	700
96	650	650	650	750	700	600	700	600	600	650	650	700	700	700
102	650	650	600	700	700	700	800	750	700	750	700	1200	1150	1200
132	700	700	650	850	800	850	750	750	750	750	750	1500	1550	800
162	600	600	600	750	750	800	750	800	750	750	750	1300	1650	850
192	650	600	600	950	900	900	900	950	750	800	850	1200	1550	900
222	500	550	500	900	900	900	900	900	1050	750	850	900	1200	1450
252	500	450	400	850	850	850	850	850	850	850	850	850	850	850
282	600	600	600	950	950	950	1000	850	850	850	850	850	850	850
312	550	600	550	900	850	950	850	950	850	850	850	850	850	850
342	400	350	400	700	650	700	700	700	650	600	650	650	650	650
372	250	350	350	550	500	500	500	500	500	550	550	550	550	550
402	200	200	200	350	400	450	350	350	350	350	350	400	400	400
432	150	200	150	300	350	300	300	300	300	300	300	300	300	300
462	150	200	150	150	250	250	250	250	250	250	250	250	250	250
492	150	150	200	250	285	310	285	275	285	275	280	275	275	275
522	270	290	250	320	325	345	325	325	325	315	320	410	335	320
552	335	335	325	335	350	360	340	320	325	310	320	345	420	340
582	270	290	290	265	275	285	295	300	300	295	280	285	305	305
612	270	260	265	260	255	250	255	260	260	260	260	260	320	320
642	235	240	245	240	245	245	245	245	245	245	245	245	245	245
672	225	225	225	225	220	220	220	220	225	225	225	225	225	225
732	190	195	200	200	190	190	185	190	185	190	190	190	190	190
792	175	190	190	185	185	185	185	185	185	185	185	185	185	185
852	115	120	125	120	120	115	120	115	120	115	105	90	115	115
912	95	100	105	105	105	105	105	105	105	105	105	105	105	105
972	80	85	85	85	85	85	85	80	80	80	70	70	70	70
1032	65	65	70	65	65	65	65	60	65	55	55	55	55	55
1092	55	50	60	60	60	60	60	60	60	55	45	45	45	45
1122	40	40	45	45	40	40	40	40	40	40	35	30	40	40
1380	20	25	25	25	25	25	25	20	20	20	15	15	30	30

*The time shown corresponds to Sample Point No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min)

TABLE IV-10. FUEL VAPOR CONCENTRATIONS IN PPM

Test 10 Conditions: Fuel - JP-4. Temperature - 71°F. R.H. - 67%. Sample Configuration No. 2. Four gallons of JP-4 in the same location as Test 9. 11/15/71.

Time (min)*	Sample Point Number																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
6	6	0	0	0	50	100	150	200	250	300	350	400	450	500	550	600	650	700	750	800	850	900	950	1000
12	150	150	100	250	200	100	200	250	300	350	300	250	200	150	100	2450	1000	1750	250	300	200	150	200	0
18	250	250	250	300	300	300	350	300	250	300	350	300	300	350	300	300	300	350	350	300	300	400	400	0
24	350	350	400	350	350	350	350	300	300	300	300	300	300	300	300	300	300	300	300	300	300	450	450	0
30	450	450	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	0
36	450	450	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	0
42	500	450	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	500	0
48	650	650	600	600	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	0
54	650	650	650	700	650	600	600	600	600	600	600	600	600	600	600	600	600	600	600	600	600	600	600	0
60	700	700	750	800	750	700	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	0
66	700	750	700	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	750	0
72	750	750	750	800	750	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
78	700	750	750	800	750	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
84	650	700	650	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
90	650	700	700	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
96	700	700	750	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
102	750	750	800	800	850	800	800	800	850	850	850	850	850	850	850	850	850	850	850	850	850	850	850	0
108	700	750	700	800	750	800	800	800	850	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
132	500	600	600	700	650	650	700	700	750	700	750	700	650	600	550	500	450	400	350	300	250	200	150	0
168	650	700	700	800	800	800	800	800	850	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
228	500	550	550	650	750	800	650	700	700	700	700	700	700	700	700	700	700	700	700	700	700	700	700	0
288	450	450	450	650	650	600	600	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	650	0
348	400	450	450	500	500	500	500	500	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	0
414	350	400	450	450	500	500	500	500	550	550	550	550	550	550	550	550	550	550	550	550	550	550	550	0
486	550	550	650	700	800	800	850	900	900	800	800	800	800	800	800	800	800	800	800	800	800	800	800	0
570	250	300	300	300	250	300	300	300	350	350	350	350	350	350	350	350	350	350	350	350	350	350	350	0
690	100	100	100	100	100	100	100	100	150	150	150	150	150	150	150	150	150	150	150	150	150	150	150	0
876	65	70	75	75	75	75	65	100	110	70	70	55	25%	135	70	75	80	80	80	80	80	80	80	0
1056	50	55	60	60	60	60	50	45	65	65	45	45	45	45	45	45	45	45	45	45	45	45	45	0
1236	35	40	45	45	50	40	35	50	45	30	35	30	35	30	35	30	20	20	20	20	20	20	20	0
1398	30	30	35	35	35	35	30	30	30	30	30	30	30	30	30	30	20	20	20	20	20	20	20	0

*The time shown corresponds to Sample Point No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min).

TABLE IV-11. FUEL VAPOR CONCENTRATIONS IN PPM

Fuel Classification	Fuel (mls.)	Sample Classification No. 2													
		Sample Number	Percent Vapor	Percent Oxygen	Percent Hydrogen	Percent Carbon	Percent Sulfur	Percent Nitrogen	Percent Water	Percent Ash	Percent Residue	Percent Ozone	Percent Dust	Percent Dust	Percent Dust
Fuel Aromatic	2	4	5	6	7	8	9	10	11	12	13	14	15	16	17
Fuel B	0	5	5	5	10	10	10	10	10	10	10	10	10	10	10
Fuel C	0	0	0	0	100	150	150	150	150	150	150	150	150	150	150
Fuel D	12	40	50	50	150	150	150	150	150	150	150	150	150	150	150
Fuel E	16	250	250	250	750	750	750	750	750	750	750	750	750	750	750
Fuel F	24	500	400	400	700	750	750	750	750	750	750	750	750	750	750
Fuel G	33	400	400	400	600	600	600	600	600	600	600	600	600	600	600
Fuel H	36	500	500	500	500	500	500	500	500	500	500	500	500	500	500
Fuel I	42	750	600	600	600	600	600	600	600	600	600	600	600	600	600
Fuel J	48	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel K	54	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel L	61	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel M	65	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel N	72	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel O	76	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel P	80	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel Q	84	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel R	88	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel S	92	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel T	96	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel U	102	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel V	108	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel W	114	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel X	120	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel Y	126	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel Z	132	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel AA	136	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel BB	142	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel CC	148	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel DD	154	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel EE	160	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel FF	166	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel GG	172	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel HH	178	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel II	184	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel JJ	190	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel KK	196	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel LL	202	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel MM	208	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel NN	214	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel OO	220	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel PP	226	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel QQ	232	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel RR	238	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel SS	244	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel TT	250	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel UU	256	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel VV	262	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel WW	268	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel XX	274	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel YY	280	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel ZZ	286	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel AA'	292	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel BB'	298	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel CC'	304	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel DD'	310	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel EE'	316	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel FF'	322	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel GG'	328	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel HH'	334	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel II'	340	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel KK'	346	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel LL'	352	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel MM'	358	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel NN'	364	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel OO'	370	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel PP'	376	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel QQ'	382	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel RR'	388	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel SS'	394	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel TT'	400	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel UU'	406	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel VV'	412	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel WW'	418	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel XX'	424	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel YY'	430	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel ZZ'	436	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel AA''	442	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel BB''	448	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel CC''	454	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel DD''	460	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel EE''	466	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel FF''	472	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel GG''	478	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel HH''	484	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel II''	490	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel KK''	496	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel LL''	502	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel MM''	508	750	750	750	750	750	750	750	750	750	750	750	750	750	750
Fuel NN''	514	750													

TABLE IV 12 FUEL VAPOR CONCENTRATIONS IN PPM

Time (min)*	Sample Configuration No. 3. Four gallons of avgas in a spill at the center of the east wall. 11/19/71.																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	100	100	100	100	100	100	100	100	200	400	1700	400	5200	20000*	1700	20000*	7900	2900	3100	2400	1800	900	900	1300	
4	800	500	600	700	500	700	1800	2400	2600	4300	4100	5700	17600	16400	16000	20000*	12300	7000	4900	4300	3300	1600	1500	400	
8	1300	700	800	1500	1400	1600	2700	2500	4100	5400	3800	4600	11900	20000*	16500	20000*	12100	3500	6100	4400	5200	2500	2400	400	
12	1800	1000	1000	1900	1800	2100	1600	2300	3200	4600	3100	2900	15200	16900	14500	20000*	12300	5900	4100	4000	3500	3300	2800	400	
16	2100	1700	1600	2200	1600	2400	1600	2700	3000	2500	2700	2200	5800	7900	9300	16500	5900	3700	3300	2600	2400	3200	2600	400	
20	2400	1900	2100	2000	2300	2000	2000	2100	1800	2600	1800	5900	2000	4400	10000	4400	3000	2600	2300	2200	2200	2100	2100	300	
24	2400	2500	2400	2100	2100	1900	2700	2000	1900	2100	1800	5200	1900	2700	8200	4250	3450	2850	2550	2500	2250	2100	1950	200	
28	2350	2250	2300	2000	1900	1600	1800	1800	1600	1600	1600	1800	1350	2050	7250	5050	2250	2650	2250	2100	1850	1950	200	200	
32	2200	2200	2200	1700	1600	1750	1650	1550	1700	1700	1550	1550	1150	2100	7350	3550	2050	2400	2150	2150	2100	2550	1750	200	
36	2250	2250	2200	1650	1500	1600	1500	1500	1600	1400	1400	1350	1150	1950	3400	4050	1600	1600	1600	1600	1850	2150	2350	200	
40	2050	2100	2100	1600	1600	1600	1600	1600	1600	1600	1600	1600	1650	1650	2500	3600	1600	2000	2100	2350	1700	2050	2000	200	
44	1950	2050	1600	1600	1650	1500	1500	1450	1650	1400	1650	1400	1550	1550	1700	1700	3550	1700	1700	1850	1600	1650	1900	150	
48	1900	1850	1900	1700	1650	1700	1600	1600	1600	1400	1400	1400	1150	1400	1400	1750	1750	1550	1550	1450	1450	1450	1650	150	
52	1600	1550	1650	1600	1550	1500	1500	1500	1500	1400	1450	1350	1500	1200	1450	1750	1950	1500	1500	1400	1400	1600	1600	150	
56	1500	1550	1500	1500	1450	1400	1550	1200	1350	1350	1350	1250	1350	1050	1300	1350	1350	1350	1200	1200	1100	1100	1300	100	
60	1300	1350	1350	1350	1350	1400	1100	1350	1100	1350	1200	1100	1100	1100	1100	1350	900	1050	1200	1250	1150	1200	1150	50	
64	1350	1350	1350	1350	1350	1350	1350	1350	1450	400	400	450	400	450	400	400	400	435	710	460	410	455	455	40	
68	450	450	450	500	450	350	450	400	400	450	300	295	325	280	330	265	345	330	385	305	310	425	330	35	
72	335	355	350	335	340	270	315	300	295	325	280	250	275	255	290	285	315	290	285	315	270	200	170	225	205
76	360	290	300	305	310	295	260	260	260	260	210	205	185	195	165	205	120	155	185	445	270	200	170	225	205
80	450	215	215	215	215	215	215	215	215	215	210	205	205	205	205	205	205	205	205	205	205	205	205	205	205
84	150	150	150	220	220	210	210	210	210	210	205	205	205	205	205	205	205	205	205	205	205	205	205	205	205

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV 13 FUEL VAPOR CONCENTRATIONS IN PPM

Time (min)*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	400	500	700	1100	18000	20000+	20000+	11400	3800	4900	2900	1400	500	500	500	500	
4	1300	400	200	100	400	6100	5200	7000	7100	5100	6400	15600	20000+	20000+	15300	5700	6800	8000	6100	1300	1000	1000	600	500	
8	1600	600	400	400	300	6700	6500	3500	9300	6400	7900	13000	20000+	20000+	20000+	7500	7100	7700	7200	1700	2700	800	800	800	
12	1900	700	600	1700	900	1000	7200	6000	8600	8200	6000	9300	1420	20000+	20000+	12400	6700	7600	8300	7400	3500	6700	1100	1100	
16	2300	1000	800	3800	4000	3700	6600	6900	7400	7000	6500	8800	17100	20000+	20000+	1900	7000	7000	10000	9200	7600	5700	7300	1300	
20	2800	1400	1300	4500	4600	2400	4600	7200	5300	7800	7100	5800	8600	13100	20000+	20000+	13600	5400	8200	7500	6100	5400	7100	1200	1200
24	2900	1800	1700	5100	3800	4000	7100	5800	6000	5400	5200	6800	11400	20000+	17800	20000+	10500	4800	7200	6500	6000	7000	1100	1100	1100
28	4100	2400	2500	5700	5400	5500	4500	5600	5900	5000	5300	10100	18900	15100	20000+	9800	3700	6600	6200	5600	5800	6200	1000	1000	1000
32	3900	3000	3300	5800	3600	3700	5200	5400	5800	5600	4800	4300	9800	15900	15000	20000+	3600	3800	4500	4800	4500	5500	6000	6000	1000
36	2300	3400	3500	5300	4800	5700	5000	4200	4600	4700	4100	4000	9500	13200	13300	19800	5400	3200	3900	4400	4100	5300	5600	900	900
40	4000	3800	3800	4000	3700	3400	4800	4800	4800	5100	4900	4700	4500	6500	13500	12400	19600	4900	4760	5000	4300	4600	4600	800	800
44	3900	3800	3700	3100	3400	3000	4600	4400	4800	4300	4000	4000	6200	11400	12700	16400	2600	4000	3900	4600	3600	3700	4100	800	800
48	3600	3400	3500	3600	3400	3400	3400	3900	4100	4100	3800	3500	4700	10300	9100	15900	5400	4000	3200	3800	4300	3700	3500	700	700
52	3600	3500	3500	3200	3300	3000	3600	3300	3700	4000	3600	3200	6700	10000	16000	5500	2700	3200	3700	3200	3500	3700	700	700	
56	3400	3400	3300	3300	3300	3200	3100	3300	3100	2900	2800	5300	10400	9500	14500	1800	2700	3000	2900	2500	3200	3600	3600	700	
60	3100	3000	2900	3400	3100	3200	3100	3000	3300	3200	2900	2900	4100	10500	9800	13300	3200	3200	3100	3000	3600	3500	600	600	
68	3000	3100	2900	2600	2700	2600	3000	2900	2900	2700	2700	2900	4800	8700	8600	12500	1800	3000	2600	2900	3100	3100	3100	600	
72	2700	2700	2600	2700	2800	2600	2600	2700	2700	2400	2900	4700	6600	10400	15100	5200	3000	3500	3200	2600	2900	2900	2800	600	
76	2900	2800	2800	2600	2700	2700	2300	2700	3300	2900	2200	3200	9400	8200	11900	4800	3800	3600	2800	2600	2500	2500	500	500	
144	1800	1800	1700	1800	1700	1700	1600	1800	1400	2000	1900	1500	1600	4700	4100	7300	1100	1800	2100	2000	1700	1600	1700	300	
204	1800	1900	2000	2100	2100	2200	2000	1900	1800	1800	1700	1900	1500	2200	3100	2000	1400	1800	1700	1700	1800	2100	1800	300	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec). Sample Point No. 20 is 200 sec.

TABLE IV-14. FUEL VAPOR CONCENTRATIONS IN PPM
 Test 14 Conditions: Fuel - JP-4. Temperature - 97°F. R.H. - 85%. Sample Configuration No. 3. Four gallons of JP-4 in a spill at the center of the east wall. 11/23/71.

Time (min)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	200	300	0	16000*	20000*	5600	2200	2500	1200	700	400	700	400	
4	700	200	100	400	100	700	300	600	1600	2900	1600	600	3700	14700	11600	18000	3100	4400	2600	1600	2000	1600	700	
8	1400	1100	600	1100	1200	1200	1000	1000	2500	2300	1900	1600	2900	12800	9900	14200	5900	3900	3700	2200	2000	2000	700	
12	1800	1600	1200	1700	1800	1800	1800	1700	2500	2500	2200	2100	3400	1900	6300	13100	4800	2900	2500	2400	2200	2300	700	
16	2200	2200	1900	2100	1800	2000	2200	1900	2600	2500	2300	1800	2100	1700	5600	12000	6200	2900	4100	2800	2900	2500	700	
20	2400	2300	2200	2100	2100	2000	1900	1800	2100	1800	1700	1600	30000	4900	4300	2600	3100	2700	2800	2900	2900	2900	700	
24	2400	2700	2600	2400	2300	2300	1900	1700	1800	1800	1700	1900	1800	1700	2400	2600	4200	2400	2200	2100	2200	2400	500	
28	2050	1950	1900	1900	1850	1850	1800	1750	1750	1650	1450	1450	1400	1350	1300	1700	1800	2400	2000	1650	1750	2000	1800	400
32	1600	1700	1750	1850	1800	1750	1650	1450	1450	1400	1400	1400	1300	1250	1500	1600	2850	1800	1550	1500	1650	1800	400	
36	1400	1550	1550	1650	1700	1600	1550	1400	1400	1400	1300	1300	1200	1250	1300	1600	2650	1750	1500	1500	1550	1800	400	
40	1400	1550	1500	1600	1600	1600	1400	1300	1300	1300	1250	1200	1150	1300	1450	2100	1550	1400	1400	1500	1650	1500	400	
108	800	850	900	950	900	850	800	800	800	750	750	700	700	800	900	800	850	800	850	850	900	850	300	
168	430	495	500	510	515	515	500	455	455	445	445	420	400	465	500	460	470	485	500	485	490	475	490	
228	340	390	400	410	410	390	360	360	360	350	340	315	305	340	350	430	380	365	400	425	485	490	140	
282	320	325	335	340	345	345	320	295	290	275	270	255	245	280	290	345	345	320	320	320	335	305	120	

*The time shown corresponds to Sample Point beyond No. 1 (i.e., sample 10 sec [e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec].

TABLE IV-15 FUEL VAPOR CONCENTRATIONS IN PPM

Test 15 Conditions: Fuel - avgas. Temperature - 52°F. R.H. - 74%. Sample Configuration No. 3. Four gallons of avgas in spill at the center of the east wall. 12/1/71.

Time (min)*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	2200	10000	1750	500	300	200	700	150	150	300	
4	350	150	150	0	0	0	0	650	1150	1350	2450	1600	700	14400	16000	14200	20000+	9800	2900	4600	2800	2700	1600	1400	1000
8	1500	600	600	900	900	900	1100	2600	2300	3600	3200	4000	11800	13100	13000	20000+	6800	4000	4100	3600	2900	2100	1900	900	
12	1600	800	600	1500	1500	1500	1700	1800	2000	3000	2700	2200	1700	9900	12300	12500	19500	9900	3400	4100	3500	3100	1900	2000	900
16	2100	1500	1000	1800	1700	1800	1600	2200	2200	2600	2500	2900	2400	7000	12700	11200	14300	8600	4600	3600	3600	2400	2500	900	
20	2200	1600	1500	1600	1700	1900	2200	2800	3400	3200	3000	3000	5900	8200	9400	14600	7500	3400	2900	2700	2800	2100	2500	700	
24	2300	1800	1800	1700	1700	1800	1800	2100	1800	2200	2600	2700	2500	2200	5300	6500	7300	11600	5000	2900	2400	2200	2100	600	
28	2300	1900	1900	1900	1900	1900	1900	2000	1900	2200	2400	2200	1500	1500	2200	6000	8900	5800	2600	2700	2400	2300	2600	600	
32	2400	2300	2200	1800	1600	1900	1900	2400	2100	2600	1900	2400	1900	1900	3200	5700	9900	4500	2700	2600	2300	2400	2100	2000	
36	2400	2300	2200	1900	1800	1900	1700	2100	2100	2000	1900	1500	1500	3700	6700	6000	10100	5100	2700	2100	1900	2100	2300	2000	
40	2300	2100	2100	1900	1800	1800	1500	2000	1900	1900	1900	1900	1400	1400	3700	2000	4300	6900	5300	2400	1900	1800	2000	1800	
44	2100	2000	2000	1900	1600	1500	1800	1700	1600	2100	1500	1500	3100	1500	5000	6700	2800	2350	2150	2250	1850	1800	400		
48	2100	2150	2100	1750	1650	1600	1800	1750	1600	1800	1600	1600	2450	1500	2250	6000	2400	2150	2150	2250	1850	1800	400		
52	2150	2150	2100	1700	1650	1600	1500	1700	1550	1450	1450	1450	1500	2200	1200	1850	5250	3050	2200	1900	2000	1750	2000	350	
56	1850	1950	1950	1600	1450	1500	1500	1450	1350	1400	1400	1400	1400	1350	1000	1800	3850	2650	2150	2000	1950	2000	2350	1900	2050
60	1900	2000	2000	1500	1350	1400	1300	1200	1250	1200	1300	1150	1300	900	1300	2200	1800	1500	1450	1600	1500	1600	1500	1750	
64	850	900	900	900	900	900	800	850	800	750	800	750	650	550	750	800	1800	1100	800	800	850	1050	800	50	
68	420	435	440	470	470	480	430	410	395	410	395	410	395	370	325	390	410	435	415	415	475	525	440	30	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV-16 FUEL VAPOR CONCENTRATIONS IN PPM
 Test 16 Conditions: Fuel - avgas. Temperature - 60°F. R.H. - 70%. Sample Configuration No. 3. Ten gallons avgas in large spill at the center of the east wall. 12/2/71.

Time [min] ^a	Sample Point Numbers												
	1	2	3	4	5	6	7	8	9	10	11	12	13
0	0	0	0	0	0	0	0	0	0	0	0	0	0
4	0	0	0	0	0	0	0	0	0	0	0	0	0
8	1400	600	400	300	200	1600	1800	1500	1300	1000	11600	20000*	11200
12	1400	700	600	400	300	600	400	700	1200	1400	1400	1400	1300
16	1600	900	800	600	400	800	500	600	1000	500	5300	14900	1100
20	1700	1000	900	800	600	800	1200	1100	800	500	4900	17700	15300
24	1600	1000	1000	800	800	800	1300	800	900	600	4600	17900	12600
28	1600	1000	900	800	800	800	1300	800	800	600	4300	14800	13400
32	1500	1100	1000	900	800	700	1000	1700	1600	1000	800	18500	7200
36	1300	1100	1100	1000	900	800	900	1800	1400	1000	700	10300	8100
40	1300	1050	1000	850	850	900	1000	1000	1500	1100	600	4200	1200
44	1200	1100	1000	1150	850	650	800	1400	1200	1050	800	1850	2500
48	1200	1200	1000	1050	700	1000	1000	1100	1100	1000	800	2000	2550
52	1350	1200	1200	1150	1050	750	1050	1150	900	1050	650	1250	4150
56	1300	1300	1200	1100	1200	1100	850	1100	1250	1050	900	500	5250
60	1250	1300	1250	1150	1150	750	1000	1100	1200	1000	900	3150	2400
68	1300	1350	1400	1150	1050	1100	850	1000	1100	1050	1150	750	1100
156	950	1000	900	950	900	850	850	900	950	750	950	800	850
216	600	600	600	600	650	550	600	600	600	450	500	550	850
306	300	300	300	300	300	300	300	300	300	200	250	250	300
396	200	200	200	200	200	200	150	150	150	150	150	150	150

^aThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV-17. FUEL VAPOR CONCENTRATIONS IN PPM

Test 17 Conditions: Fuel - JP-4. Temperature - 50°F. R.H. - 74%. Sample Configuration No. 3. Four gallons of JP-4 in a spill at the center of the east wall. 12/3/71.

Time [min]*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	4500	3500	400	600	900	0	0	0	0	0	
4	200	0	100	0	100	0	0	0	100	100	0	3100	8300	4000	8600	1900	600	900	500	400	300	300	300	200	
8	600	400	400	200	100	300	300	600	1000	600	400	2600	6000	5800	10200	3400	900	2100	900	1400	700	600	300	300	
12	1000	700	700	400	400	400	500	800	600	1200	700	2300	1000	6600	8300	5000	1200	1300	1200	1100	1000	800	800	300	
16	1200	1000	900	800	900	700	600	900	800	1300	800	2100	1100	2500	7100	2600	1100	1500	1600	1000	900	900	1000	300	
20	1100	1100	900	1000	800	700	600	900	800	800	800	700	1700	2400	3000	1200	2100	1800	1200	1100	1800	1800	1800	200	
24	1300	1600	1600	1000	.000	900	900	1000	900	900	1000	900	1100	900	1600	2400	1200	1400	1300	1100	1000	1600	1000	1000	
28	1300	1500	1500	1100	1100	1000	1200	1100	1200	1200	1000	1300	1100	1500	1700	2300	1300	1400	1400	1300	1300	1400	1000	1000	
32	1200	1400	1500	1300	1300	1250	1150	1300	1250	1200	1200	1150	1400	1150	1450	1600	2350	1550	1450	1400	1350	1400	1450	150	
36	1350	1450	1450	1400	1350	1350	1350	1350	1350	1350	1350	1350	1400	1150	1700	1400	1850	1400	1300	1350	1400	1450	1400	150	
40	1250	1350	1350	1400	1300	1200	1350	1300	1250	1300	1300	1350	1100	1350	1500	1850	1350	1250	1400	1300	1300	1300	1300	150	
44	1250	1350	1350	1350	1300	1300	1300	1300	1250	1200	1300	1100	1150	1150	1350	1350	1400	1350	1300	1450	1500	1400	1400	150	
90	1150	1200	1200	1250	1200	1200	1100	1100	1150	1100	1050	1050	1050	1050	1150	1150	1600	1400	1150	1200	1200	1200	1200	100	
120	1050	1100	1100	1100	1100	1050	1100	1050	1100	1100	1000	1100	950	1000	1000	1000	1150	1150	1000	1150	1200	1200	1200	100	
150	850	900	900	950	900	850	950	950	900	900	950	800	900	950	800	900	850	1000	850	850	900	950	850	100	100
180	725	780	780	815	800	755	845	820	800	830	735	815	665	725	740	925	895	740	745	840	870	775	775	775	120
186	705	760	770	775	790	780	710	780	770	715	775	665	730	580	655	680	730	690	695	730	775	775	775	775	105

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV-18 FUEL VAPOR CONCENTRATIONS IN PPM

TEST 16 Conditions: Fuel - JP-4. Temperature - 64°F. R.H. - 75%. Sample Configuration No. 3. Ten gallons of JP-4 in a large spill at the center of the east wall. 12/7/71.

Time [min]*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
4	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
8	1200	400	300	200	100	200	100	400	400	700	20000+	17600	15100	20000+	8600	900	1400	600	700	500	700	900	700	900	
12	1600	600	400	300	300	400	1400	1100	700	300	500	9700	17700	18100	20000+	18800	2800	1300	700	800	800	800	1100	1100	
16	1600	700	600	500	400	400	300	400	1300	800	600	500	700	18900	18500	20000+	17200	2300	2000	1100	1400	1100	1100	1100	
20	1700	700	600	500	400	400	500	400	1500	900	600	500	700	20000+	17200	17900	20000+	13600	20000	2200	1000	1300	900	1200	
24	1700	700	600	500	400	400	500	400	1400	700	700	600	6800	15600	17200	20000+	16800	2300	1100	1000	1300	900	900	1000	
28	1600	800	700	600	500	600	1600	1100	800	700	900	9200	18200	16100	20000+	14300	2700	1300	1000	1600	1000	1000	1000	1100	
32	1700	800	700	600	600	700	1900	1600	1100	800	700	7400	16600	17400	20000+	15600	3900	1700	1100	1300	1300	1300	1000	1000	
36	1800	800	700	600	700	700	1500	1500	800	800	700	5700	15800	14000	20000+	13400	2300	1300	1100	1000	1500	900	1000	1000	
40	1600	800	700	800	700	700	700	1400	900	1000	700	8000	15300	12800	13200	2800	1300	1100	1000	1100	1100	1000	1000	1000	
44	1700	900	800	800	900	800	800	1500	900	900	800	6600	13300	14300	18100	14500	2700	1200	1000	2000	1200	1200	1000	1000	
48	1700	900	800	900	800	800	700	800	800	700	800	7900	14500	15200	19200	12500	2900	1400	1200	2300	2800	1300	1000	1000	
52	1800	900	800	900	900	800	800	900	900	800	800	13800	11400	16400	11200	2000	1400	1300	1700	1400	1300	900	900	900	
56	1800	1000	1000	1000	1000	1000	1300	1100	1200	1100	1200	5200	12200	12400	14900	12600	3000	1700	1400	2500	2200	1300	900	900	
60	1700	1100	1000	1000	1000	1200	1200	1200	1300	1200	1200	4600	11000	10700	14700	8400	1600	1500	1700	2100	1500	1500	900	900	
64	1700	1100	1000	1000	1000	1500	1500	1500	1500	1500	1500	1300	1400	2800	9000	8700	13000	5600	2000	1600	1400	1600	1500	800	
68	1500	1000	1000	1300	1300	1300	1300	1300	1300	1300	1300	1300	1300	1300	1300	1300	9600	12000	9100	1600	1700	2100	1500	800	
72	1500	1000	1000	1300	1400	1200	1600	1400	1200	1300	1400	1400	1300	1300	1300	1300	3800	7500	8000	12500	6400	1700	1800	1900	
76	1700	1400	1200	1500	1700	1600	1300	1400	1500	1400	1400	4100	9700	7500	11100	8700	2000	2200	1700	1900	1900	1700	800	800	
80	1700	1400	1300	1500	1600	1600	1400	1400	1500	1700	1500	3100	5700	8000	10900	7100	2000	1900	1800	2200	1800	1800	700	700	
84	1800	1600	1500	1600	1600	1600	1600	1600	1600	1600	1600	3500	6600	8500	8700	6100	2000	1800	1900	1900	1900	1900	1900	1900	
88	1800	1700	1600	1700	1700	1700	1700	1700	1700	1700	1700	3100	5400	5300	7200	5300	2100	2600	2200	1800	1800	1800	1800	1800	
92	1700	1600	1600	1600	1600	1600	1700	1700	1700	1700	1700	2500	5600	7400	8700	4800	2100	2400	1800	1900	1900	1900	1900	1900	
96	1800	1700	1700	1700	1600	1600	1600	1600	1600	1600	1600	1700	1800	2800	4400	5400	8000	4600	2700	1900	2100	1900	1900	1900	1900
100	1500	1136	1700	1500	1700	1700	1700	1700	1700	1700	1700	1700	1700	1700	1700	1700	2400	3800	5400	6900	3900	2000	1900	2000	
104	1350	1250	1550	1300	1250	1550	1700	1600	1500	1500	1500	1500	1500	1500	1500	1500	1550	3250	5100	6050	4150	1800	2100	1900	1750
108	1214	1150	1350	1400	1400	1400	1400	1400	1400	1400	1400	1400	1400	1400	1400	1400	1350	2000	2250	3300	4400	3150	1600	1550	1450
112	256	900	850	800	1200	1150	1200	1150	1150	1050	1050	1000	1000	1000	1000	1000	1250	1150	1150	1250	1250	1250	1250	1250	
116	2296	900	850	800	1000	950	850	800	900	900	900	900	900	900	900	900	1000	1300	2550	2800	3000	3000	3000	1100	1100
120	336	600	750	750	750	950	950	950	950	950	950	950	950	950	950	950	950	1100	1700	2200	3100	3100	3100	1100	1100

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV 19. FULL CONCENTRATIONS IN PPM

Test 19 Conditions: Fuel - avgas. Temperature - 67°F R.H. - 90%. Sample Configuration No. 3. Four gallons of avgas in spill at the center of the east wall. 12/8/71.

Time [min] ^a	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23		
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0		
4	1,000	2,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000	1,000			
8	2,200	6,000	400	3,000	600	300	2,100	500	300	400	200	1,400	20,000+	20,000+	20,000+	20,000+	20,000+	22,000	22,000	600	400	300	400		
12	2,600	7,000	500	4,000	600	300	3,000	300	2,500	1,100	600	800	20,000+	20,000+	20,000+	20,000+	20,000+	28,000	32,000	1,000	900	900	900		
16	2,800	8,000	600	4,000	400	300	3,000	300	2,800	1,600	1,000	1,300	20,000+	20,000+	20,000+	20,000+	20,000+	35,000	37,000	1,000	1,000	1,000	1,000		
20	2,800	8,000	600	4,000	400	500	4,000	2,700	2,000	1,900	1,300	1,300	1,900	20,000+	20,000+	20,000+	20,000+	20,000+	39,000	41,000	1,000	1,000	1,000	1,000	
24	2,900	10,000	700	500	500	400	400	400	3,000	2,600	1,700	2,300	20,000+	20,000+	20,000+	20,000+	20,000+	4,300	5,000	1,400	1,400	1,400	1,400		
28	2,900	10,000	800	600	500	400	500	500	3,200	2,400	2,400	4,000	20,000+	20,000+	20,000+	20,000+	20,000+	5,700	6,800	1,800	2,000	2,000	2,000		
32	3,200	10,000	800	600	500	600	700	3,300	4,100	3,000	4,600	3,000	4,600	20,000+	20,000+	20,000+	20,000+	20,000+	6,800	8,000	1,800	2,000	2,000	2,000	
36	2,800	10,000	800	600	500	600	700	1,000	3,600	4,900	4,900	4,900	4,900	20,000+	20,000+	20,000+	20,000+	20,000+	7,000	8,300	2,000	2,000	2,000	2,000	
40	2,800	10,000	800	600	500	600	700	1,000	4,000	4,000	6,000	5,000	6,000	6,000	20,000+	20,000+	20,000+	20,000+	20,000+	8,000	8,100	2,000	2,000	2,000	2,000
44	2,700	10,000	800	700	600	600	1,300	1,600	4,400	6,300	5,100	5,100	5,100	5,100	20,000+	20,000+	20,000+	20,000+	20,000+	8,100	8,900	3,000	3,000	3,000	3,000
48	2,800	10,000	800	600	600	600	2,500	5,000	5,000	7,000	7,000	7,000	7,000	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,600	3,600	3,600	3,600	3,600	
52	2,700	10,000	800	600	600	600	3,000	2,700	5,600	7,400	7,300	7,900	7,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,500	9,500	4,700	4,500	4,500	4,500	
56	2,700	10,000	800	700	600	600	3,500	3,500	6,000	8,000	7,900	8,000	8,000	8,000	20,000+	20,000+	20,000+	20,000+	20,000+	9,600	9,100	5,100	4,900	4,900	4,900
60	2,600	10,000	800	600	600	600	3,500	4,000	6,400	7,900	7,900	7,900	7,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,800	9,600	5,100	4,800	4,800	4,800	
64	2,600	10,000	800	700	600	600	3,000	3,700	4,000	6,300	7,800	7,800	7,800	7,800	20,000+	20,000+	20,000+	20,000+	20,000+	9,800	9,600	5,600	5,700	5,700	5,700
68	2,600	10,000	800	700	600	600	4,200	4,100	6,700	8,200	8,200	8,200	8,200	20,000+	20,000+	20,000+	20,000+	20,000+	9,700	9,000	5,900	5,600	5,600	5,600	
72	2,500	10,000	800	700	600	600	4,200	5,200	7,000	8,600	8,100	8,100	8,100	8,100	20,000+	20,000+	20,000+	20,000+	20,000+	9,700	9,300	5,500	5,500	5,500	5,500
76	2,400	9,000	700	700	600	600	4,000	4,200	6,400	7,300	7,300	7,900	7,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,400	9,600	5,600	5,300	5,200	5,200	
80	2,400	9,000	700	700	600	600	4,000	4,400	6,500	8,100	7,700	8,200	8,200	8,200	20,000+	20,000+	20,000+	20,000+	20,000+	9,800	9,500	5,700	5,700	5,700	5,700
84	2,300	9,000	900	700	600	600	4,200	4,600	6,700	8,200	7,700	7,900	7,900	7,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,100	9,400	5,800	5,800	5,800	5,800
88	2,300	9,000	900	700	600	600	4,000	4,50r	6,600	8,000	7,500	7,500	7,500	7,500	20,000+	20,000+	20,000+	20,000+	20,000+	9,300	9,200	6,000	5,900	5,900	5,900
92	2,200	9,000	900	700	600	600	4,000	4,300	6,500	7,800	7,300	7,400	7,400	7,400	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,300	5,400	5,400	5,400	5,400
96	2,200	9,000	900	700	600	600	4,000	4,300	6,500	7,800	7,300	7,400	7,400	7,400	20,000+	20,000+	20,000+	20,000+	20,000+	8,800	9,000	5,600	5,600	5,600	5,600
100	2,200	9,000	900	700	600	600	4,000	4,400	6,600	7,600	7,100	7,200	7,200	7,200	20,000+	20,000+	20,000+	20,000+	20,000+	8,900	9,100	5,900	5,900	5,900	5,900
104	2,200	9,000	900	700	600	600	4,000	4,500	6,500	7,600	7,100	7,200	7,200	7,200	20,000+	20,000+	20,000+	20,000+	20,000+	9,100	9,300	5,600	5,600	5,600	5,600
108	2,100	9,000	900	700	600	600	4,000	4,600	6,500	7,500	7,000	6,900	6,900	6,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,100	5,600	5,600	5,600	5,600
112	2,100	9,000	900	700	600	600	4,000	4,600	6,500	7,500	7,000	6,900	6,900	6,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,100	5,600	5,600	5,600	5,600
116	2,100	9,000	900	700	600	600	4,000	4,600	6,500	7,500	7,000	6,900	6,900	6,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,100	5,600	5,600	5,600	5,600
120	2,100	9,000	900	700	600	600	4,000	4,600	6,500	7,500	7,000	6,900	6,900	6,900	20,000+	20,000+	20,000+	20,000+	20,000+	9,000	9,100	5,600	5,600	5,600	5,600
124	2,000	9,000	900	700	600	600	4,000	4,600	6,500	6,600	6,700	6,100	6,100	6,100	20,000+	19,500	20,000+	19,300	20,000+	7,900	6,500	5,300	5,300	5,300	5,300
128	1,900	8,000	900	700	600	600	4,000	4,400	5,200	6,500	6,300	6,300	6,300	6,300	20,000+	20,000+	20,000+	19,300	20,000+	7,400	6,300	5,500	5,500	5,500	5,500
132	1,800	8,000	900	700	600	600	4,000	4,300	5,200	6,400	6,200	6,100	6,100	6,100	20,000+	20,000+	20,000+	19,100	20,000+	7,000	6,000	5,400	5,400	5,400	5,400
136	1,800	8,000	900	700	600	600	4,000	4,100	5,100	6,200	6,000	5,900	5,900	5,900	20,000+	20,000+	20,000+	19,100	20,000+	6,700	5,600	4,600	4,600	4,600	4,600
140	1,800	8,000	900	700	600	600	4,000	4,200	5,100	6,100	6,000	5,800	5,800	5,800	20,000+	20,000+	20,000+	19,100	20,000+	6,400	5,300	4,300	4,300	4,300	4,300
144	1,800	900	700	700	600	600	4,000	4,400	5,100	6,000	5,700	5,600	5,600	5,600	20,000+	20,000+	20,000+	19,000	20,000+	6,100	5,000	4,000	4,000	4,000	4,000
148	1,700	900	700	700	600	600	4,000	4,000	5,000	5,000	5,000	5,000	5,000	5,000	20,000+	20,000+	20,000+	18,000	20,000+	5,700	4,600	3,600	3,600	3,600	3,600
152	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
156	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
160	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
164	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
168	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
172	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
176	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
180	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	1,600	2,000	
184	1,600	2,000	1,700	2,000	1,600	2,000	1,600	2,000	1,600</																

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec).

TABLE IV-20. FUEL CONCENTRATIONS IN PPM

Test 20 Conditions: Fuel - JP-4. Temperature - 67°F. R.H. - 100%. Sample Configuration No. 3. Four gallons of JP-4 in spill at the center of the east wall. 12/9/71.

Time (min)*	Sample Point Numbers																										
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24			
0	0	0	0	0	0	0	0	0	0	0	0	0	0	100	400	800	1400	700	200	100	0	0	0	0			
4	200	0	0	0	0	0	0	0	0	100	300	0	5100	16500	13200	12400	700	600	400	300	300	300	900	900			
8	900	200	100	100	100	0	0	0	800	400	300	11300	20000	18400	20000	16800	1100	1300	600	500	400	400	900	900			
12	1200	300	200	200	100	100	100	100	800	400	700	12300	20000	20000	20000	18500	1600	2200	800	700	400	400	500	1000			
16	1300	400	300	200	200	200	100	200	1400	1400	700	14200	20000	20000	20000	20000	2600	2700	1100	700	500	500	600	1100			
20	1500	500	300	200	200	200	200	200	1600	1900	1900	14000	20000	20000	20000	20000	2800	3600	1400	1000	600	600	600	1100			
24	1500	500	400	300	300	200	300	100	1900	2400	1800	2500	14600	20000	20000	20000	20000	3600	4200	1700	1200	600	600	600	1100		
28	1500	500	400	300	300	200	400	400	2000	2800	2200	2800	15700	20000	20000	20000	20000	3900	4600	1800	1400	600	600	600	1200		
32	1600	500	400	300	300	200	400	600	2200	3000	2400	3400	15900	20000	20000	20000	20000	4300	5200	1900	1500	600	600	600	1100		
36	1500	600	400	300	300	300	600	700	2300	3500	3700	3700	15700	20000	20000	20000	20000	4700	5700	2200	1800	700	700	700	1200		
40	1600	600	400	300	300	300	800	800	3200	3800	4000	4000	16000	20000	20000	20000	20000	5100	6200	2600	1900	700	700	700	1100		
44	1600	600	400	300	300	300	1000	1200	2800	4300	3500	4600	15300	20000	20000	20000	20000	5600	6800	2900	2100	700	700	700	1100		
48	1600	600	400	300	300	300	1400	1500	3100	4700	3900	5000	15100	20000	20000	20000	20000	6000	6800	3400	2500	700	700	700	1100		
52	1600	600	400	300	300	300	1700	1700	3400	4900	4300	5200	15500	20000	20000	20000	20000	6400	7100	3500	2700	700	700	700	1100		
56	1600	600	400	400	300	300	1900	1900	3500	5200	4400	5600	15200	20000	20000	20000	20000	6400	7300	3700	3000	700	700	700	1100		
60	1600	600	500	400	400	300	2100	2300	3900	5400	4800	5700	14700	20000	20000	20000	20000	6400	7500	4100	3200	800	700	700	1100		
64	1600	600	400	400	300	2500	2600	4400	5700	5000	5600	14200	1900	20000	20000	19000	6600	7500	4400	3700	800	700	700	1100			
68	1600	600	500	400	400	300	2600	2900	4300	5700	5300	5800	14400	19000	19000	19100	19100	6800	7700	4500	3900	800	700	700	1100		
72	1600	600	500	400	400	300	2900	3100	4700	5900	5000	6000	14400	19200	19300	20000	19400	7200	7700	4800	4100	800	700	700	1100		
76	1600	600	500	400	400	300	3000	3200	4900	6000	5500	6000	14000	18800	19000	20000	18600	7100	7800	4800	4200	800	700	700	1100		
80	1600	600	500	400	400	300	3100	3300	4900	6000	5500	5900	13800	18700	19000	20000	18600	7100	7800	5100	4300	800	700	700	1100		
84	1600	600	500	400	400	300	3200	3400	5000	6200	5500	6000	14000	18400	18500	20000	18400	7400	7800	5103	4600	800	700	700	1000		
88	1600	600	500	400	400	400	3400	3500	5200	6300	5700	6000	13900	1820	18500	20000	17600	6900	8000	4800	800	800	800	1000	1000		
92	1600	700	500	400	400	400	3500	3800	5400	6200	5500	6000	13100	1750	1740	20000	17100	7000	7500	5400	5000	800	800	800	1000		
96	1600	600	500	400	400	400	3600	4000	5400	6400	5700	6100	12600	1710	17300	19700	16900	7000	7500	5600	5000	900	700	700	1000		
100	1500	700	500	400	400	400	3700	3900	5400	6300	5800	6000	12500	16800	17300	19000	16800	6600	7300	5700	5000	900	800	800	1000		
104	1500	700	500	400	400	400	3700	4000	5400	5900	5600	5900	11900	16400	16800	18600	16400	6900	7200	5400	5100	900	800	800	1000		
108	1500	600	500	400	400	400	3700	3900	5300	5900	5400	5900	11700	16100	18300	15500	6900	7200	5300	5200	800	800	800	1000			
112	1500	600	500	400	400	400	3700	4000	5300	6000	5500	5900	11700	15800	17100	18000	17100	6800	7000	5100	5000	800	800	800	1000		
116	1500	700	500	400	400	400	3700	4000	5300	6100	5400	5800	11600	15200	16500	18000	15600	6800	7000	5100	5200	900	900	900	1000		
120	1600	800	600	500	500	500	3500	4000	5200	6300	5700	6100	11500	14500	15200	16500	14800	7300	7500	5200	5100	1000	1000	1000	1200		
124	1600	800	700	600	600	600	4000	4200	5500	6500	5800	6300	10400	13000	13600	14700	13500	7300	7600	5800	5400	1100	1000	1000	1200		
128	1600	800	800	700	700	700	4000	4200	5600	6300	5700	5900	9800	12000	12800	13700	12900	7100	7400	5500	5300	1100	1000	1000	1200		
132	1500	900	800	700	700	700	4000	4200	5600	5100	5200	8500	10400	11200	11800	11300	6500	6600	5000	4800	1100	1000	1000	1200			
136	1500	900	800	700	700	700	4000	4200	5600	5100	5200	8500	10400	10800	10900	10300	5700	5900	4500	4200	1000	1000	1000	1200			
140	1500	900	800	800	700	700	2700	3200	4200	5000	4600	4900	7500	9400	10100	10800	10300	5200	5400	3700	3400	1000	900	900	1000		
144	1500	900	800	800	700	700	2400	2600	3600	4500	4000	4200	7100	8800	9600	10000	9600	4700	5100	3300	2800	1000	900	900	1000		
148	1600	900	800	800	700	700	2100	2200	3000	3300	3000	3700	700	800	900	1000	900	400	400	800	600	500	500	500	800		
152	1600	900	800	800	700	700	1800	2000	2800	3000	2700	3200	6700	700	800	900	1000	900	400	400	800	600	500	500	500	800	
156	1600	900	800	800	700	700	1500	1700	2500	2700	2400	2900	6400	6700	700	800	900	900	400	400	800	600	500	500	500	800	
160	1600	900	800	800	700	700	1200	1400	2200	2400	2100	2600	6100	6400	6700	700	800	900	900	400	400	800	600	500	500	500	800
164	1600	900	800	800	700	700	900	1100	1900	2100	1800	2300	5800	6100	6400	6700	700	500	500	500	500	500	500	500	800		
168	1600	900	800	800	700	700	600	800	1600	1800	1500	1900	5500	5800	6100	6400	6700	500	500	500	500	500	500	500	800		
172	1600	900	800	800	700	700	300	500	1300	1500	1200	1600	5200	5500	5800	6100	6400	500	500	500	500	500	500	500	800		
176	1600	900	800	800	700	700	0	200	1000	1200	900	1300	5000	5300	5600	5900	6200	500	500	500	500	500	500	500	800		
180	1600	900	800	800	700	700	0	100	800	1000	700	1100	4800	5100	5400	5700	6000	500	500	500	500	500	500	500	800		
184	1600	900	800	800	700	700	0	0	600	800																	

TABLE IV-21. IUEL CONCENTRATIONS IN PPM

Test 21 Conditions: Fuel - JP-4 Temperature - 65°F. R.H. - 75% Sample Configuration No. 3. Four gallons of JP-4 in spill at the center of the east wall. 12/14/71.

Time (min)*	Sample Point Number											
	1	2	3	4	5	6	7	8	9	10	11	12
0	0	0	0	0	0	0	0	0	0	100	100	100
4	800	300	200	100	200	400	600	500	200	3900	1100	1500
8	2000	700	600	400	300	400	500	1900	1500	11300	20000*	20000*
12	2700	900	700	600	500	500	700	2200	2900	1800	1200	1000
16	2900	1100	900	700	600	600	700	1500	1500	2100	1500	1300
20	3100	1200	1000	800	700	900	900	1000	1200	1800	2000	1800
24	3200	1400	1200	900	800	800	1000	4300	5400	3800	20000*	20000*
28	3200	1400	1300	1000	900	1100	900	1200	4900	3900	20000*	20000*
32	3400	1600	1400	1100	1000	1000	1000	1500	4800	6700	5900	20000*
36	3500	1600	1400	1200	1000	1100	1800	4700	5200	6000	20000*	20000*
40	3300	1700	1500	1300	1100	1200	1200	1200	6000	6700	20000*	20000*
44	3400	1800	1600	1300	1200	1200	1400	2000	5800	8100	6200	5700
48	3400	1800	1700	1300	1400	1600	1800	1800	1200	5400	1200	1200
52	3400	1800	1700	1500	1300	1400	1400	1600	2000	6500	8100	7500
56	3400	2000	1800	1600	1500	1500	1800	2000	2000	6500	8000	7500
60	3400	2000	1800	1600	1500	1500	1800	2000	2000	7000	8000	7500
64	3500	2100	1900	1700	1600	1600	1800	2000	2000	7000	8000	7500
68	3500	2200	2000	1800	1600	1600	1800	2000	2000	7000	8000	7500
72	3600	2200	2100	1800	1700	1700	1800	2000	2000	7000	8000	7500
76	3600	2300	2100	1800	1700	1700	1800	2000	2000	7000	8000	7500
80	3600	2300	2200	1800	1700	1700	1800	2000	2000	7000	8000	7500
84	3800	2400	2300	1900	1800	1900	1900	2000	2000	7000	8000	7500
88	3800	2500	2400	2100	1900	2000	2000	2000	2000	7000	8000	7500
92	3800	2500	2400	2200	2000	2000	2000	2000	2000	7000	8000	7500
96	3800	2600	2400	2200	2000	2000	2000	2000	2000	7000	8000	7500
100	3900	2600	2500	2200	2100	2100	2100	2000	2000	7000	8000	7500
104	3900	2600	2500	2300	2100	2100	2100	2000	2000	7000	8000	7500
108	3900	2700	2500	2300	2100	2100	2100	2000	2000	7000	8000	7500
112	3900	2800	2600	2400	2300	2300	2300	2000	2000	7000	8000	7500
116	3900	2800	2600	2400	2300	2300	2300	2000	2000	7000	8000	7500
120	4000	2800	2700	2500	2400	2400	2400	2000	2000	7000	8000	7500
124	4000	2900	2700	2600	2400	2400	2400	2000	2000	7000	8000	7500
128	4000	2900	2800	2600	2500	2600	2700	2000	2000	7000	8000	7500
132	4100	3000	2800	2700	2600	2600	2700	2000	2000	7000	8000	7500
136	4100	3000	2900	2700	2600	2600	2700	2000	2000	7000	8000	7500
140	4100	3000	2900	2700	2600	2600	2700	2000	2000	7000	8000	7500
144	4000	3000	2900	2700	2600	2600	2700	2000	2000	7000	8000	7500
148	4100	3100	2800	2700	2600	2600	2700	2000	2000	7000	8000	7500
152	4100	3100	3000	2800	2700	2800	2900	2000	2000	7000	8000	7500
156	4100	3100	3000	2900	2800	2800	2900	2000	2000	7000	8000	7500
160	4100	3100	3000	2900	2800	2800	2900	2000	2000	7000	8000	7500
164	4100	3200	3000	2900	2800	2800	2900	2000	2000	7000	8000	7500
168	4100	3200	3100	3000	2900	2900	3000	2000	2000	7000	8000	7500
172	4100	3200	3100	3000	2900	2900	3000	2000	2000	7000	8000	7500
176	4200	3300	3200	3100	3000	3000	3000	2000	2000	7000	8000	7500
180	4200	3300	3200	3100	3000	3000	3000	2000	2000	7000	8000	7500
184	4300	3400	3300	3200	3100	3200	3200	2000	2000	7000	8000	7500
188	4300	3400	3300	3200	3100	3200	3200	2000	2000	7000	8000	7500
192	4300	3400	3300	3200	3100	3200	3200	2000	2000	7000	8000	7500
196	4300	3400	3400	3300	3200	3200	3200	2000	2000	7000	8000	7500
200	4300	3600	3500	3400	3300	3400	3500	2000	2000	7000	8000	7500
204	4400	3700	3500	3400	3300	3400	3500	2000	2000	7000	8000	7500
208	4400	3700	3600	3500	3400	3500	3600	2000	2000	7000	8000	7500
212	4400	3700	3600	3500	3400	3500	3600	2000	2000	7000	8000	7500
216	4400	3700	3600	3500	3400	3500	3600	2000	2000	7000	8000	7500
220	4400	3800	3600	3500	3400	3500	3600	2000	2000	7000	8000	7500
224	4400	3700	3600	3500	3400	3500	3600	2000	2000	7000	8000	7500
228	4300	3600	3500	3400	3300	3400	3500	2000	2000	7000	8000	7500
232	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
236	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
240	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
244	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
248	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
252	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
256	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
260	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
264	4400	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
268	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
272	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
276	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
280	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
284	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
288	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
292	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
296	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
300	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
304	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
308	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
312	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
316	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
320	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
324	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
328	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
332	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
336	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
340	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
344	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
348	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
352	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
356	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
360	4300	3800	3700	3600	3500	3600	3700	2000	2000	7000	8000	7500
364												

TABLE IV-22. FUEL CONCENTRATIONS IN PPM
 Test 2: Conditions: Fuel - JP-4. Temperature - 77°F. R.H. - 65%. Sample Configuration No. 3. Four gallons JP-4 in spill at the center of the east wall. 12/14/71.

Time [min] ^a	Sample Point Numbers													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
4	400	0	0	0	0	0	400	400	300	600	200	4200	19500	34000
8	1200	300	200	100	100	100	1100	1200	300	1000	500	8400	20000+	129000
12	1300	400	300	200	200	200	1300	1900	1200	1800	800	10600	19500	166000+
16	1400	400	300	300	300	300	1900	2200	1700	2300	1000	9400	19600	176000+
20	1500	500	400	400	300	300	600	2000	1700	1900	1300	10400	18700	18000+
24	1500	600	400	400	400	400	1500	2300	2100	2800	2000	9700	17200	16700+
28	1500	600	400	600	500	400	1600	2200	2000	2500	1600	16900	15400	19700
32	1500	600	500	700	500	400	700	2000	1900	2300	1800	9800	16200	18800
36	1500	600	500	700	600	400	1300	2100	2100	2700	2300	9600	16200	15000
40	1500	700	500	700	500	500	700	1900	1800	2100	1300	10400	15200	18500
44	1500	700	600	600	700	500	800	1900	1800	2000	1400	8200	15300	14800
48	1400	700	600	600	600	500	800	2100	2400	2200	1900	8700	13800	13600
52	1400	700	600	600	700	500	1400	2100	2300	2600	1900	8000	13400	12800
56	1400	700	600	600	700	600	1200	2400	2400	2600	2300	7700	12600	21800
60	1400	700	600	600	600	600	1300	2300	2600	2900	2400	6300	12300	11600
68	1400	600	500	500	450	500	2000	2300	2300	2450	1950	5550	10600	13200
72	1100	500	500	500	700	1900	2300	2500	2600	2400	6000	10400	12000	10300
76	1200	600	500	600	600	700	1900	2300	2600	2800	2100	4700	9600	9900
80	1200	700	600	600	700	600	700	1800	2200	2500	2800	5800	9200	9800
84	1200	700	600	600	700	700	1700	2000	2600	2800	2200	14000	11000	11700
88	1200	700	600	700	700	700	1600	2100	2500	2400	1800	4500	9200	14400
92	1200	700	600	700	700	700	1700	2300	2400	1900	5300	8700	9400	10400
96	1200	700	600	700	700	700	1600	2200	2600	4900	2400	8500	8800	10700
100	1200	700	700	700	700	700	1700	2100	2200	5100	2500	8400	9000	10500
104	1200	700	700	700	700	700	1300	2000	2100	2400	2000	5000	8500	8600
108	1300	800	700	700	800	700	1400	1800	2100	1700	1500	9100	10800	8100
112	1300	800	800	800	700	700	1500	2000	2400	1800	1800	5100	7900	8900
116	1300	800	800	800	700	700	1700	1900	2100	1500	1500	5500	8400	9000
120	1300	800	800	800	700	700	900	1600	1700	1300	5500	8400	9000	10500
124	1300	900	800	800	800	800	1600	1500	1400	1100	5700	8500	9100	10500
128	1300	900	800	800	800	800	1500	1500	1000	1000	5500	8600	9200	10600
160	600	500	500	400	400	400	400	600	600	400	300	700	1200	2400
192	600	400	400	300	300	300	300	300	300	300	400	300	1600	500
224	500	400	300	300	300	300	300	300	300	500	600	400	2500	500
256	500	400	300	300	300	300	300	300	300	500	400	2900	1500	400
288	500	400	400	300	300	400	300	600	800	500	300	1500	2500	400
324	400	400	400	300	300	300	300	300	300	500	700	300	1000	1800

^aThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 3 is 30 sec).

TABLE IV-23 FUEL CONCENTRATIONS IN PPM

Test 23 Conditions: Fuel - JP-4 Temperature - 62°F R.H. - 65% Sample Configuration No. 4. Four gallons of JP-4 in spill at the center of the east wall to coordinate Configuration No. 3 with No. 4. 12/16/71.

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 20 is 200 sec).

TABLE IV-24. FUEL CONCENTRATIONS IN PPM

Test 24 Conditions: Temperature - 45°-66°F. R. H. - 31-93%. Preliminary Run at Hangar 935 at Kelly AFB; six F-100 aircraft. 12/18/71 to 12/20/71.

Time (min)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
84	25	25	20	25	25	35	35	30	40	40	30	25	25	20	20	25	25	25	20	20	20	20	20	20
132	20	20	25	25	25	25	25	15	20	15	15	20	20	20	20	30	30	30	15	10	10	10	10	10
204	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
300	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
708	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
1116	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
1524	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
1932	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
2340	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
2748	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
2780	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec).

TABLE IV-25 FUEL CONCENTRATIONS IN PPM
 Test 25 Conditions: Temperature - 47°-78°F R H - 31-100% Run at Hangar 935 at Kelly AFB, eight F-100 aircraft. 12/22/71 to 12/27/71.

Time (min)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
504	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1008	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5
1512	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5
2016	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13	13
2520	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
3024	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14	14
3528	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15
3535	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19
4039	18	19	19	19	18	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19
4543	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19
5047	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23	23
5551	19	19	18	18	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19	19
6055	25	25	26	26	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25	25
6253	25	26	26	26	25	25	25	25	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26	26
6295	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5
6559	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
7087	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec).

TABLE IV-26 FUEL CONCENTRATIONS IN PPM
 Test 26 Conditions: Temperature - 45°-69°F. R.H. - 37-93%. Run at Hangar No. 5 at Randolph Field with 23 T-38 aircraft. 12/30/71 to 1/2/72.

Time (min)*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
57	2	2	2	2	2	2	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3	3	
144	2	2	2	2	2	2	3	3	3	4	4	5	2	4	2	2	2	3	3	3	3	3	3	3	
150	4	5	5	5	5	6	6	7	7	7	8	12	8	9	8	9	8	9	9	9	9	11	12	12	
156	10	10	10	10	10	10	10	11	10	10	11	14	13	11	11	11	11	11	11	11	11	11	10	14	
216	19	19	20	20	20	20	20	20	20	20	21	23	23	22	21	20	21	20	20	20	20	20	20	23	
224	9	9	9	9	9	9	10	10	10	10	10	10	10	10	10	10	10	9	9	9	9	9	9	9	12
378	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
432	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4
720	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6
1296	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9
1420	22	22	22	22	22	22	22	22	22	22	23	23	23	23	23	23	23	23	23	23	23	23	23	24	
1894	9	9	9	9	9	9	9	9	9	9	10	10	11	10	9	9	9	9	9	9	9	9	9	9	
2686	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4
2830	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
3838	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
3910	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1	1
4198	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g. Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec).

Test 27 Conditions: Fuel - JP-4. Temperature - 57°F. R.H. - 100%. RAFF. Special Sample Configuration No. 2. Fifty-three gallons of fuel spilled as indicated on drawing. 1/18/72.

Time (min)	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	
4	40	35	280	330	60	1150	430	80	60	50	75	100	50	40	130	60	40	40	40	40	40	40	45	
8	110	45	540	410	80	1580	650	175	100	65	80	65	50	45	70	60	40	90	215	90	45	210	140	
12	190	65	10	580	105	1980	1940	580	180	90	240	155	75	60	190	100	45	275	140	60	55	260	225	
16	280	75	1330	830	1300	2000*	2000*	650	235	110	90	70	60	75	70	100	185	160	780	120	190	300	360	
20	440	120	1100	680	1690	2000*	2000*	600	270	155	330	250	150	120	360	215	100	230	190	240	120	195	390	
24	500	170	1560	1490	1530	2000*	2000*	590	330	185	300	430	230	150	255	130	225	200	200	195	220	325	375	
28	740	210	1680	1320	1700	2660	440	400	280	150	350	250	150	200	200	120	420	300	800	540	290	550	550	
32	620	210	2000	1450	1200	2200	1650	535	340	235	295	305	230	250	335	260	165	375	295	340	470	480		
36	590	220	1450	1930	990	2000*	2000*	560	380	225	405	420	245	170	400	340	145	260	190	365	160	305	635	
40	720	425	1700	180	650	2000*	2000*	490	340	240	500	400	210	280	570	260	190	270	190	535	170	180	430	
44	540	295	1780	1350	850	2000*	2000*	480	365	175	450	355	240	430	335	185	235	200	200	445	190	215	320	
48	600	250	1760	1580	1450	2000*	1765	510	400	320	490	425	330	310	390	330	250	455	220	225	230	485	375	
52	650	175	1805	1860	1635	2000*	1560	535	380	270	440	440	300	375	345	335	275	350	295	345	190	315	565	570
56	660	270	1840	1860	1285	2000*	1370	410	350	255	295	270	200	215	375	245	330	330	220	610	175	235	345	545
60	590	445	2000*	1240	840	2000*	1240	345	300	255	380	275	210	255	350	245	300	200	200	400	150	125	180	390
64	570	160	1600	1300	1200	2400	1300	300	250	200	500	400	200	300	225	150	200	160	360	155	160	360	630	
68	560	400	1880	1560	1845	2000*	1640	370	350	260	395	230	240	475	345	205	215	150	370	150	155	435	475	
72	640	300	1560	1250	1520	2000*	1430	345	315	240	415	355	210	245	365	270	200	345	190	225	160	200	525	545
76	600	420	2000*	1860	1595	2000*	1440	385	360	300	460	355	230	310	420	290	255	350	180	180	350	350	350	
80	630	370	1680	1300	1100	2000*	1590	370	325	285	480	380	225	315	440	285	200	255	165	215	160	165	325	
84	500	345	1580	1360	440	1945	1210	310	295	370	480	375	245	440	360	195	240	175	265	160	170	245	190	
88	450	350	1510	1180	350	1400	1100	275	280	305	755	555	235	400	370	250	175	315	155	190	135	145	185	
92	290	1140	1080	315	1300	850	240	275	295	390	300	185	285	345	240	205	215	190	150	225	145	150	165	
96	350	280	1070	1140	315	1080	720	230	245	385	300	200	280	385	250	180	175	140	180	150	140	170	160	
100	355	250	1370	1300	395	1140	795	245	260	425	345	290	210	275	250	210	165	175	150	165	145	145	145	
104	370	235	1350	1240	350	1500	1000	275	265	230	280	250	205	125	275	210	170	180	140	200	145	145	235	
108	370	225	1030	990	285	1430	840	240	225	325	275	190	275	285	215	170	175	145	165	145	145	240	175	
112	350	215	970	850	275	1070	740	240	225	275	230	190	265	270	200	170	175	145	165	145	145	170	155	
116	295	215	1020	870	270	1490	950	260	240	225	305	240	180	215	295	210	160	155	140	160	140	140	320	
120	320	205	780	325	1230	820	230	210	195	240	305	225	200	270	210	145	135	130	135	130	135	145	375	
124	290	190	730	680	250	1350	850	220	200	280	205	170	210	245	190	150	150	165	170	150	170	165	165	
128	270	210	970	810	245	730	485	185	200	220	310	235	175	245	275	205	155	195	130	135	120	120	130	
132	255	200	560	495	215	1080	610	185	195	345	330	210	190	290	255	150	185	130	300	140	130	175	185	
136	265	210	480	570	1580	920	270	250	245	275	355	325	260	365	310	200	190	175	305	180	165	200	190	
140	370	250	875	835	540	700	480	230	275	355	325	285	250	245	265	285	195	200	185	230	185	190	275	
144	355	305	490	315	415	350	220	250	250	300	285	250	210	225	195	205	160	165	170	150	170	165	235	
148	356	275	356	410	450	290	340	305	220	205	230	225	195	185	210	205	160	165	170	150	170	165	235	
152	210	170	270	300	190	250	305	165	150	170	150	125	130	115	140	130	115	115	110	110	100	100	130	
156	150	125	205	235	150	190	130	130	115	125	120	110	110	110	110	110	110	110	110	110	110	110	130	
160	120	100	170	190	110	155	150	75	105	100	110	110	90	110	90	110	75	70	95	60	60	60	60	
164	95	80	140	160	90	130	125	80	80	80	80	80	80	70	70	70	95	60	60	60	60	60	60	
200	35	30	60	65	30	60	60	35	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	
228	20	20	45	45	25	45	45	20	20	20	20	20	20	20	20	20	20	20	20	20	20	20	20	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec. Sample Point No. 3 is 30 sec).
**Spread fuel out with brooms to double spill area at 132 min.
***Opened one pair of doors (1 at each end of the hangar and diagonally opposite) NW and SE.
****Opened two more pairs of doors (NE and SW).
*****Opened three more pairs of doors (NE and SW).

Test 28 Conditions: Temperature - 44°-66°F. Field test at Bergstrom AFB with four RF-4 aircraft in Hangar 4534. 1/21/72 to 1/24/72.

TABLE IV-28 FUEL CONCENTRATIONS IN PPM

Time (min)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
156	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5
168	5	5	5	5	5	5	5	5	5	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
180	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15	15
192	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5	5
240	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
372	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
720	10	20	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
732	10	10	25	15	10	10	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
744	10	10	25	10	10	10	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
756	10	10	30	15	10	10	15	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
804	10	10	30	15	10	10	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
816	10	10	25	15	10	10	50	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
828	10	10	45	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
840	10	10	20	15	10	10	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
852	15	10	15	15	10	10	40	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
864	10	10	25	15	10	10	25	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
876	10	10	15	15	10	10	45	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
888	10	10	10	10	10	10	10	20	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
996	10	10	10	10	10	10	10	25	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1008	10	10	10	10	10	10	10	30	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1020	10	10	10	10	10	10	10	15	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1032	10	10	10	10	10	10	10	50	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1044	10	10	10	10	10	10	45	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1056	10	10	20	10	10	10	10	100+	20	15	15	10	10	10	10	10	10	10	10	10	10	10	10	10
1068	10	10	15	10	10	10	100+	25	15	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1080	10	10	15	10	10	10	100+	25	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1116	10	10	15	10	10	10	100+	25	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1128	10	10	15	10	10	10	100+	35	40	25	15	10	10	10	10	10	10	10	10	10	10	10	10	10
1140	10	10	55	20	15	15	100+	40	20	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10
1152	15	10	20	15	15	15	100+	90	30	25	15	15	10	10	10	10	10	10	10	10	10	10	10	10
1164	15	15	50	20	20	20	100+	100+	30	25	15	15	15	15	15	15	15	15	15	15	15	15	15	
1176	15	15	35	20	15	15	100+	100+	35	25	20	15	15	10	10	10	10	10	10	10	10	10	10	
1188	15	15	100+	40	25	25	100+	100+	150	35	30	20	15	15	10	10	10	10	10	10	10	10	10	
1200	15	10	140	50	25	15	100G-	300	40	25	15	15	10	10	10	10	10	5	5	5	10	10	10	10
1212	10	10	35	20	15	15	100G-	400	50	20	15	15	10	10	10	10	10	10	10	10	10	10	10	
1224	15	15	30	20	20	20	100G-	765	285	40	30	15	15	10	10	10	10	10	10	10	10	10	10	
1236	20	15	45	25	20	15	100G-	570	70	85	20	50	15	15	15	15	15	15	15	15	15	15	15	
1248	15	15	135	30	20	20	985	405	115	45	20	15	15	15	15	10	10	10	10	10	20	20	20	
1260	20	15	80	35	20	20	655	245	65	40	20	15	15	15	15	15	15	15	15	15	15	15	15	
1272	20	15	140	50	20	20	870	355	50	35	20	15	15	15	15	15	15	15	15	15	15	15	20	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec). Sample Point No. 20 is 600 sec.

Test 28 Conditions: Temperature - 46° - 66° F. Field test at Bergstrom AFB with four RF-4 aircraft in Hangar 4534. 1/21/72 to 1/24/72.

Time (min)*	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
1296	20	15	30	25	20	20	740	220	40	45	20	20	15	15	15	15	15	15	15	15	15	15	20	20
1308	20	20	25	25	20	15	1000*	290	55	80	25	20	15	15	15	15	15	15	15	15	15	15	15	20
1320	20	15	30	25	20	15	795	385	160	70	20	20	15	15	15	15	15	15	15	15	15	15	15	15
1332	20	15	35	25	20	15	840	290	70	45	20	15	15	15	15	15	15	15	15	15	15	15	15	20
1344	20	15	35	40	20	1000*	290	75	65	20	15	15	15	15	15	15	15	15	15	15	15	15	15	15
1449	20	25	150	45	30	20	875	450	120	55	25	25	20	15	15	15	15	15	15	15	15	15	35	40
1452	20	25	150	45	35	20	1000*	260	55	35	25	125	20	15	15	15	15	15	15	15	15	15	30	45
1468	20	30	80	30	25	20	1000*	930	120	65	25	25	20	20	15	15	15	15	15	15	15	15	25	30
1536	25	40	35	30	25	105	275	36	20	10	10	10	10	10	10	10	10	10	10	10	10	10	15	15
1548	25	35	30	25	25	85	360	50	20	10	10	10	10	10	10	10	10	10	10	10	10	10	15	15
1560	20	20	25	25	20	105	145	35	20	10	10	10	10	10	10	10	10	10	10	10	10	10	15	15
1596	10	15	20	15	10	350	70	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	15	15
1660	10	10	10	10	10	40	180	25	15	10	10	10	10	10	10	10	25	25	25	25	25	25	10	15
1692	15	15	15	15	15	35	180	15	10	5	5	5	5	5	5	5	5	5	5	5	5	5	10	15
1704	10	10	10	10	10	30	15	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1884	10	10	10	10	10	10	115	25	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
1908	10	10	10	10	10	10	26	35	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
2424	10	10	10	10	10	50	15	10	15	10	10	10	10	10	10	10	10	10	10	10	10	10	10	10
2508	10	35	15	10	10	375	135	35	25	15	15	10	10	10	10	10	10	10	10	10	10	10	10	10
2592	15	30	20	15	15	265	135	70	40	20	15	15	15	15	15	15	15	15	15	15	15	15	15	15
2664	20	15	95	45	30	20	1000*	705	120	75	20	20	20	20	20	20	20	20	20	20	20	20	20	
2776	20	20	120	40	20	20	1000*	705	120	75	20	20	20	20	20	20	20	20	20	20	20	20	20	
2916	20	215	55	40	30	1000*	730	95	35	35	50	30	30	20	20	20	20	20	20	20	20	20	20	
2928	20	45	30	20	30	990	505	115	40	25	25	20	25	15	15	15	15	15	15	15	15	15	25	25
3024	15	15	20	15	15	25	70	100	20	15	10	10	10	10	10	10	10	10	10	10	10	10	10	
3144	5	5	5	5	5	25	35	50	10	5	5	10	10	10	10	10	10	10	10	10	10	10	10	
3156	5	5	5	5	5	25	35	50	10	5	5	10	10	10	10	10	10	10	10	10	10	10	10	
3168	15	10	10	10	10	30	35	55	20	15	15	10	10	10	10	10	10	10	10	10	10	10	10	
3216	15	15	15	15	15	25	30	100+	30	15	10	10	10	10	10	10	10	10	10	10	10	10	10	
3696	5	5	5	5	10	15	60	15	10	5	5	5	5	5	5	5	5	5	5	5	5	5	5	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec. Sample Point No. 20 is 600 sec).

TABLE IV 29. FUEL VAPOR CONCENTRATIONS IN PPM
 Test 29 Conditions: Fuel - avgas. Temperature - 69°F. R.H. - 55%. Sample Configuration No. 4. Four gallons of avgas in a spill at the center of the east wall. 2/14/72.

Time (min)*	Sample Point Numbers													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	100	100	500	100	200	1000	1400	2800	1800	1500	1100	1300	800	1000
12	19500	16000	8500	7700	4500	3500	2100	800	600	400	400	400	400	3000
24	19400	16400	11500	9200	6400	4100	2900	1600	800	400	400	400	400	3600
36	18200	16100	10600	8800	6700	5200	3900	2500	1000	500	500	600	600	900
48	17100	13900	8900	6900	6000	5000	4100	3300	1800	1000	700	600	600	900
60	16000	13200	8400	7000	5600	4200	3600	2100	1300	600	600	700	1200	3400
72	15000	11900	7300	6300	5100	4300	3900	3200	2900	1500	800	800	1100	1900
84	12600	11900	6800	5600	4200	3900	3500	3500	2200	1400	800	900	800	800
96	11900	10300	6700	5100	4100	3300	3000	2500	1800	1300	1100	1000	800	800
108	10700	8300	4800	4000	3600	3200	3000	2800	2100	1700	800	900	1000	1000
120	8400	6700	4800	3900	2700	2500	2200	1900	900	700	700	600	600	600
132	9800	8000	4300	3700	3100	2000	1900	1100	800	600	600	600	600	600
216	6700	4650	2750	1850	950	600	800	850	950	900	900	900	1000	1000
288	4150	3000	1150	1250	850	750	500	550	550	600	550	550	550	550
384	2300	1500	900	700	550	500	400	250	300	250	250	250	250	250
480	3100	2500	1150	750	700	600	350	250	250	250	250	250	250	250
576	3200	2700	1250	750	500	450	450	450	450	450	450	450	450	450
672	2000	1400	700	550	600	600	600	600	600	650	650	650	650	650
720	600	700	550	500	500	500	500	500	500	450	450	450	450	450
816	500	500	500	500	500	500	500	500	500	500	500	500	500	500

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 3 is 90 sec).

TABLE IV 30. FUEL VAPOR CONCENTRATIONS IN PPM

Test 30 Conditions: Fuel - avgas. Temperature - 62°F. R.H. - 43%. Sample Configuration No. 3. Four-gallon spill with floor fan operating part time to simulate draft under hangar door

time (min)*	Sample Point Numbers															
	1	2	3	4	5	6	7	8	9	10	11	12	13	14		
0	0	0	0	0	0	20	100	100	H0	700	350	650	18400	20000*		
12	700	400	300	250	250	340	450	850	850	4900	3800	3200	18400	20000*		
24	1050	700	600	550	550	400	350	850	1100	2850	7250	6650	6700	17850	20000*	
36	1150	900	700	600	600	1350	1650	7050	5205	7650	6400	16550	19100	19800	20000*	
48	1400	1000	850	700	650	2000	2500	5500	7350	5400	14200	17500	18550	19550	16600	
60	1500	1200	1000	950	900	650	2100	2450	5100	6750	4800	5400	13800	16600	17400*	
72	1350	1150	800	900	900	1100	1900	4010	6100	4550	3950	13000	16550	16750	18600	
84	1600	1350	1200	1200	1200	1000	1500	2500	5350	3450	4350	12350	14700	15900	16750	
96	1000	1450	1250	1200	850	800	1100	1150	4750	3450	2450	11450	13950	15050	16500	
108	1550	1400	1250	1200	1050	800	1050	1350	4600	3450	3350	10800	14850	16250	17250	
120	1750	1500	1300	1500	1100	950	1150	1450	1300	4000	3350	1800	11200	13950	16150	
132	1200	1550	1500	1350	1200	1100	1200	1300	3000	2050	1300	10500	13550	14650	15650	
144	1700	1650	1550	1500	1200	1200	1250	1300	1350	1500	2550	1450	13000	14250	15250	
156	1700	1650	1500	1500	1500	1500	1500	1500	1500	1500	1200	1200	1200	1200	1200	
168	1650	1700	1550	1400	1350	1150	1300	1400	1550	2300	1400	950	12050	13900	14750	
180	1700	1550	1500	1350	1150	1050	1250	1350	1550	2050	1300	1000	12250	1450	15250	
192	1600	1550	1400	1300	1300	1000	1250	1300	1350	1300	1250	8150	9900	11450	12550	
204	1900	1350	1150	1200	1300	1200	1200	1200	1200	1250	1500	1200	10500	11800	12500	
216	1800	1450	1300	1250	1150	900	1200	1200	1200	1200	1200	1150	5300	8350	9950	
**228	1900	1250	1300	1400	1150	1250	1250	1300	1400	1750	2050	1400	10200	12700	13900	
240	1300	1250	1350	1300	1150	1350	1350	1350	1350	1350	1350	1150	950	12050	13150	
**252	1100	1250	1000	1700	1850	1700	1850	1850	1850	1850	1850	1850	1850	2050	2350	
***264	1400	1525	1325	1775	1825	1759	1825	1759	1759	1759	1600	1725	1775	1900	1900	
276	1325	1525	1525	1775	1775	1775	1775	1625	1650	1700	1650	1650	1150	5300	4475	
288	1450	1600	1500	1500	1675	1725	1725	1625	1825	1675	1875	1675	1250	2350	4600	
300	1350	1600	1500	1600	1600	1300	1800	2100	1350	1350	1350	1350	1350	1350	1350	
312	1350	1550	1325	1650	1825	1225	1675	1725	1625	1700	1575	2775	6200	8000	9100	
324	1425	1300	1575	1725	1375	1500	1575	1590	1425	1425	1475	3650	4750	5350	6200	
336	1500	1500	1325	1525	1675	1175	1225	1525	1425	1425	1500	3675	4775	6175	6200	
348	1300	1400	1175	1500	1500	1350	1500	1400	1325	1375	1300	3450	4650	6600	6925	
360	1200	1300	1100	1350	1225	1050	1475	1375	1300	1275	1275	1275	3775	4800	6550	
372	1225	1300	1125	1300	1175	1000	1375	1375	1300	1250	1250	1250	3650	4675	6675	
384	1175	1225	1100	1200	1025	1225	1225	1350	1225	1200	1175	3650	4950	6705	6875	
396	1200	1175	1025	950	1075	1000	1075	950	1225	1150	1150	1075	3675	4600	5275	
408	1150	1150	975	1050	1225	1100	1175	1100	1025	1125	1075	3675	4600	6425	6575	
420	1100	975	1050	1100	1175	1100	1175	1100	1100	1100	1075	3100	4450	6150	6390	
432	1100	1050	1100	1150	1050	1000	1050	1200	1050	1025	1075	3200	4375	6075	6200	
444	1050	1075	1050	1075	1000	1075	1000	1075	975	1050	975	3375	4250	6050	6125	
456	1075	1100	1050	1000	975	950	1175	1000	975	1025	950	2400	4100	5750	5990	
576	725	725	725	725	700	700	700	675	650	650	650	675	700	725	750	
588	700	700	700	700	675	675	675	675	650	650	650	650	700	675	700	
600	675	675	675	675	675	675	675	675	675	675	675	675	675	700	675	
708	5	15	10	10	10	10	5	5	5	60	50	45	40	30	30	30
														0	10	10
														0	60	0

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).

**Fan turned on.

***Fan turned off.

TABLE IV-31 FUEL VAPOR CONCENTRATIONS IN PPM
 Test 31 Conditions: Fuel 1 - JP-4. Temperature - 89°F. R.H. - 28%. Sample Configuration No. 3. Four-gallon spill with floor fan operating part time
 to simulate draft under hanger door.

Time [min] ^a	Sample Point Numbers													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
12	100	50	100	75	80	200	80	200	100	50	400	2150	3500	5000
24	200	100	200	150	175	125	150	450	325	175	100	750	4925	7175
36	225	125	100	200	150	150	150	275	225	125	250	800	3725	7400
48	200	150	100	150	125	125	125	350	300	150	125	500	2975	5025
60	200	125	100	150	100	125	125	350	200	125	125	300	2825	4325
72	cal	cal	cal	150	125	125	100	100	200	100	100	225	1775	3650
84	150	100	75	75	50	125	75	150	225	100	75	200	1425	3400
96	175	100	75	100	50	50	100	100	45	125	50	125	75	3000
108	150	75	100	75	50	100	75	175	75	100	150	1050	2950	3925
120	150	75	75	50	50	100	75	172	125	75	75	1650	2500	3700
132	125	75	75	50	50	50	125	100	75	75	75	775	2075	3175
*144	125	75	100	125	50	50	50	75	100	25	25	50	500	2075
156	75	50	150	250	225	300	300	300	325	325	475	575	600	400
*168	125	100	100	275	350	350	350	375	375	400	550	375	550	575
180	225	175	150	325	275	350	350	350	300	250	225	200	750	1850
192	200	150	125	275	250	225	225	200	250	175	200	1025	1215	675
204	150	125	100	175	200	150	150	150	150	125	125	850	2375	850
216	150	100	100	125	100	100	200	175	200	225	125	100	175	2325
288	125	75	75	50	50	150	75	100	125	75	75	450	2325	575
432	200	175	150	150	150	150	150	150	150	150	150	400	1525	450
576	275	275	275	275	275	325	275	300	300	300	300	350	400	325
720	250	250	275	275	275	275	275	275	257	275	275	275	300	325
1104	150	175	175	175	175	175	175	175	175	175	175	175	175	175

^aThe time shown corresponds to Sample Point No. 1. Each Sample Point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).
 *Fan on (156 min).
 **Fan off (174 min).

TABLE IV-32. FUEL VAPOR CONCENTRATIONS IN PPM
Test 32 Conditions: Fuel - avgas. Temperature - 90° F. R.H. - 40%. Sample Configuration No. 3. Four-gallon drip test with floor fan operating partime to simulate draft under rear door.

Time (min)*	Sample Point Numbers																							
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24
0	75	75	75	75	75	75	100	100	150	300	425	250	457*	7300	9450	10000	1350	10000	1075	925	725	425	500	300
12	475	300	350	300	100	275	140	800	1025	1750	1000	1950	10000*	10000*	10000*	10000*	10000*	2075	2975	2175	1525	775	800	440
24	125	650	675	525	425	550	1425	1425	1500	3075	1650	2675	10000*	10000*	10000*	10000*	10000*	3450	5025	3275	1925	1075	1125	675
36	1225	950	975	400	625	750	2425	2425	1250	4275	2475	4675	10000*	10000*	10000*	10000*	10000*	5075	7125	5225	2925	1525	1775	775
48	1750	1325	1425	1225	1150	1100	4075	3150	4875	9425	3775	5500	10000*	10000*	10000*	10000*	10000*	6900	7900	6650	10000*	2250	1950	903
60	1650	1300	1300	1300	1200	1150	3700	3450	5300	6050	4500	6300	18400	21000	20000*	20000*	20000*	7200	8200	6650	6000	2250	1900	400
72	1850	1500	1500	1450	1500	1300	5000	4150	6100	7150	4250	6350	19900	26000	20000*	20000*	20000*	7900	8500	7250	6500	2250	1900	400
84	1900	1550	1500	1500	1400	1300	5000	3800	6100	7000	5400	6950	19750	20000	20000*	20000*	20000*	7900	8850	7450	6500	2300	2250	901
96	1900	1500	1400	1450	1350	1300	5100	4100	5750	7800	5750	5550	19400	20000*	20000*	20000*	20000*	7900	8500	7600	7300	2600	2000	400
108	1900	1400	1500	1500	1400	1350	5500	4450	6800	6700	5500	6800	19100	20000*	20000*	20000*	20000*	6950	8300	7100	6700	2450	2100	900
120	1900	1500	1400	1450	1400	1400	5750	5550	6350	6250	5200	5750	18550	20000*	20000*	20000*	20000*	6800	8150	7100	6750	3000	3250	900
132	1900	1500	1450	1450	1450	1400	5600	5400	6100	6150	5500	5700	17800	20000	20000*	20000*	20000*	6800	7750	6700	6200	3400	2800	900
144	1800	1350	1350	1200	1150	1400	5100	5400	5850	6150	4750	5550	18450*	20000	20000*	20000*	20000*	6500	8200	7000	5850	3700	3900	900
156	1850	1450	1350	1300	2750	3450	5100	5100	5700	5200	5300	5500	16200	20000*	20000*	20000*	20000*	18700	6600	6700	6300	5400	5900	1000
168	1900	1550	1400	1450	1350	1300	5400	5400	5600	5000	5450	5450	14350	19700	20000*	20000*	20000*	16900	6100	5700	4850	5500	5550	900
180	1900	1700	1650	1600	4600	4600	4750	4850	4700	4950	5000	4500	4800	13500	18000	20000*	20000*	16800	5000	5700	5200	4800	5250	850
192	1700	1500	1500	1500	1500	1500	4400	4400	4800	4800	4800	4800	14150	14150	14150	14150	14150	17600	4250	4250	4250	4950	4950	850
204	2400	2000	1850	1850	4000	4250	4200	4200	4650	4200	4000	4300	17500	20000	20000*	20000*	17350	5050	5050	5300	4700	4700	850	
216	2600	2250	2250	4000	4200	4450	3300	4600	4900	3750	4150	13800	18000	19400	20000*	16200	4900	6550	5000	5100	4700	4600	800	
228	2900	2600	2600	3900	3900	3450	4550	5000	4000	4200	4200	13100	16700	18800	20000*	14900	5100	5700	5000	4300	4450	800		
240	3500	2900	2500	3500	3700	3400	400	450	4550	3600	3900	12400	16300	18300	1850	14150	4700	5400	4250	4250	3950	4750	750	
252	3500	3050	3100	3300	3150	2650	4200	4200	3700	4350	4200	4000	11540	16050	17350	19100	13800	4750	4500	4350	3650	3400	3350	700
264	3100	3100	3100	3000	3000	3100	2850	4050	4000	3150	3200	9100	12750	13800	15600	10600	3850	3350	3350	3250	3150	3450	650	
276	3000	3000	2600	2800	2800	2600	2600	2600	2700	2400	2500	2400	1400	10450	11400	12950	7550	3150	3250	2450	2900	2800	550	
288	2450	2700	2700	2600	2600	2200	2050	2500	2100	2350	2100	2350	5700	7000	7050	10450	11800	7550	3350	2900	2300	2600	500	
420	540	620	545	545	575	575	510	465	525	555	460	565	500	830	275	410	160	605	635	625	605	560	135	
***332	475	585	535	600	650	675	665	650	625	605	705	705	705	705	930	865	595	605	540	540	510	60	60	
444	540	560	560	560	640	640	640	640	640	640	640	640	640	640	750	755	410	575	585	585	555	545	75	
***556	525	540	540	540	595	600	605	605	605	590	590	600	600	600	635	675	730	600	490	490	490	495	65	
468	465	475	480	520	535	535	535	535	530	530	545	545	545	545	645	645	605	420	365	445	495	475	60	
480	445	445	485	485	480	485	475	475	470	465	465	465	515	515	545	545	435	415	415	415	405	425	55	
492	375	395	445	445	440	450	315	400	400	410	465	465	285	490	30	750	160	150	585	440	245	365	55	
576	145	165	155	160	150	170	180	185	160	160	140	140	105	105	665	245	95	110	105	105	105	105	25	
720	65	65	70	75	70	70	105	100	115	105	105	95	95	95	95	95	95	95	95	95	95	95	25	
1008	75	80	80	95	85	85	85	85	95	95	95	95	85	85	85	85	90	155	90	50	85	75	85	
1404	60	60	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	65	

^aThe time above corresponds to Sample Point No. 1.

each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).

TABLE IV-33. FUEL VAPOR CONCENTRATIONS IN PPM
 Test 33 Conditions: Fuel - JP-4. Temperature - 85°F. R.H. - 48%. Sample Configuration No. 3. Four-gallon drip test with floor fan operating part time to simulate draft under hangar door.

Time (min) ^a	Sample Point Numbers											
	1	2	3	4	5	6	7	8	9	10	11	12
0	100	100	100	100	100	100	270	100	300	400	2600	1800
12	300	200	200	200	200	300	400	500	700	1100	5600	7400
24	600	500	500	400	400	700	100	900	1800	1300	8700	12000
36	900	700	700	600	600	1300	1200	1600	2800	1900	2700	11500
48	1000	800	800	800	800	2100	2100	2000	3800	2500	3600	13000
60	1300	900	900	900	900	800	200	1600	2500	3200	3000	3800
72	1300	1000	900	900	900	800	1000	1000	1800	1200	12400	16400
84	1300	900	800	800	900	900	1300	1900	2200	1600	11300	15300
96	1200	900	800	1000	900	900	1100	900	1100	1000	5500	9100
108	1100	800	800	800	800	800	800	1000	1000	5800	9700	11500
120	1000	700	700	800	800	800	1400	1200	1200	1200	7500	11000
132	1100	800	700	1500	1800	1700	2000	2200	1900	1900	3000	11000
144	162.5	170.0	172.5	212.5	230.0	220.0	225.0	307.5	222.5	305.0	3000	2975
156	2000	167.5	180.0	220.0	225.0	215.0	220.0	245.0	215.0	207.5	2950	3000
168	1550	1350	1350	1600	1700	1550	1700	1900	2100	1850	4000	5300
180	1300	1150	1100	1450	1450	1250	1450	1650	1600	1450	1400	5200
192	1200	900	900	1300	1250	1100	1200	1250	1300	1200	1850	1600
204	1000	800	800	1000	1100	900	1000	1000	1200	1000	6250	8350
216	1000	800	700	1200	1200	1000	1000	1100	900	1500	10000	10300
228	800	700	700	1100	1200	900	1000	1000	1200	1100	5300	7900
240	800	700	600	1100	1100	800	1000	1000	1000	800	2500	3900
252	700	600	500	800	1000	800	1000	900	900	800	2000	5900
264	c-1	c-1	c-1	c-1	c-1	c-1	c-1	c-1	c-1	c-1	1150	1900
276	600	500	450	750	700	600	650	650	650	550	1000	1700
288	500	450	500	650	650	550	650	750	650	500	3600	4550
300	450	300	350	550	575	525	550	575	525	500	700	1150
312	42.5	350	350	500	450	450	500	550	550	475	550	1000
324	42.5	37.5	37.5	500	525	500	500	600	600	500	450	500
336	450	400	350	450	525	450	500	500	725	500	450	500
348	450	37.5	350	47.5	47.5	450	500	550	47.5	450	42.5	47.5
360	400	350	32.5	450	450	42.5	47.5	500	42.5	42.5	42.5	450
372	37.5	32.5	30.0	42.5	450	37.5	42.5	42.5	450	400	37.5	400
384	350	30.0	37.5	40.0	40.0	40.0	40.0	40.0	40.0	37.5	400	1450
											1525	550

^aThe time shown corresponds to Sample Point No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).
 eefan on 132 min; fan off 156 min.

TABLE IV-14 FUEL VAPOR CONCENTRATIONS IN PPM

Test 14 Conditions: Fuel - avgas. Temperature - 75°F R.H. - 40%. Sample Configuration No. 6. Four gallons of avgas in a spill in the center of the east wall. 6/6/72.

Time [min] ^a	Sample Point Number												23	24
	1	2	3	4	5	6	7	8	9	10	11	12		
0	0	0	0	0	0	0	0	0	0	0	0	0	0	0
1	18,400	12,800	9,250	5,500	3,700	2,400	1,600	1,050	1,150	1,310	1,200	2,000	2,350	3,150
13	17,600	16,600	15,900	14,400	13,600	12,800	11,500	10,500	9,800	8,750	8,100	6,700	7,100	8,700
25	16,900	16,400	15,700	14,900	14,000	13,200	12,200	11,300	10,600	9,600	8,800	8,000	8,100	9,300
37	16,800	16,300	15,600	14,700	14,100	13,300	12,400	11,600	10,800	10,000	9,000	8,200	8,100	9,000
49	16,300	16,100	15,400	14,600	13,800	13,000	12,100	11,300	10,500	9,500	8,600	7,800	7,700	8,600
61	16,100	15,900	15,200	14,500	13,700	12,900	12,100	11,300	10,300	9,100	8,100	6,700	6,600	7,100
73	15,900	15,700	15,000	14,300	13,400	12,700	11,700	10,800	10,000	8,800	7,900	6,600	7,600	8,000
85	15,200	14,700	13,400	12,500	11,700	10,900	9,700	8,900	8,100	7,000	6,400	6,000	6,400	7,000
97	15,100	14,900	13,400	12,500	11,300	10,500	9,100	7,900	6,700	5,600	4,500	4,600	4,700	5,600
109	15,000	14,500	13,000	12,700	11,800	10,800	9,600	8,500	7,100	5,900	4,600	4,600	4,700	5,400
121	14,800	14,100	12,600	11,800	10,800	9,400	8,100	6,600	5,700	4,200	3,500	3,600	4,000	4,500
133	14,700	13,900	12,800	11,900	10,700	9,500	8,200	6,500	5,600	4,300	2,600	2,700	3,000	3,400
145	14,470	13,500	12,200	11,300	10,000	8,700	6,800	5,300	4,600	3,700	2,700	2,500	2,400	2,700
157	14,300	13,200	11,700	10,800	8,800	6,900	5,400	4,400	4,200	3,400	3,000	2,000	2,000	3,000
169	14,000	12,700	11,200	9,800	7,500	5,400	4,200	3,200	1,100	2,600	2,700	2,800	2,500	3,100
181	13,500	11,600	8,000	5,700	4,300	2,900	3,000	2,300	2,100	2,300	2,000	2,100	2,000	2,900
193	13,200	10,700	8,100	4,600	3,800	2,500	2,600	2,200	2,000	2,100	1,900	2,000	1,900	2,200
205	12,800	10,000	6,900	4,000	3,30	2,300	1,900	2,100	1,400	2,000	1,900	1,300	1,200	1,700
217	12,500	9,500	6,300	3,900	3,100	2,100	1,800	1,800	1,700	1,600	1,600	1,400	1,400	1,800
229	12,200	6,700	3,300	2,900	1,900	2,000	1,600	1,700	1,500	1,500	1,600	1,400	1,500	1,500
241	12,000	6,000	4,000	2,800	2,500	1,700	1,800	1,400	1,400	1,300	1,200	1,200	1,400	1,200
253	11,600	7,300	4,700	2,500	2,200	1,400	1,400	1,200	1,300	1,100	1,200	1,000	1,000	1,400
265	11,300	6,600	4,100	2,300	2,100	1,300	1,400	1,000	1,100	900	1,000	800	800	1,300
277	11,100	6,300	4,100	2,300	2,100	1,300	1,400	1,000	1,000	800	800	800	800	1,300
289	10,800	6,000	3,600	2,000	1,900	1,100	1,300	900	800	800	800	700	700	1,300
301	10,700	6,100	4,100	2,200	2,100	1,300	1,200	1,100	1,000	900	900	700	700	1,200
313	10,400	5,300	3,500	1,800	1,700	1,000	1,200	800	900	900	900	700	700	1,200

^aThe times shown correspond to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec.

TABLE IV 35. FUEL VAPOR CONCENTRATIONS IN PPM

Test 35 Conditions: Fuel - JP-4. Temperature - 66°F. R.H. - 65%. Sample Configuration No. 4. Four gallons of JP-4 in a spill in the center of the east wall. 6/13/72.

Time [min]*	Sample Point Numbers																								
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	
0	8,700	8,200	3,300	3,500	1,100	900	600	500	200	100	100	100	100	300	900	1,500	5,700	8,500	9,000	10,000					
4	12,200	10,100	9,000	7,500	5,100	2,600	1,600	800	400	400	300	400	400	1,900	3,100	5,400	7,200	8,400	9,500	10,500	11,000				
8	11,900	10,500	9,000	9,000	7,000	6,700	4,900	3,200	2,300	1,300	1,300	700	900	800	1,500	1,900	3,500	5,000	7,100	8,200	9,000	10,400	11,000		
12	11,700	10,600	10,000	9,400	8,600	7,800	6,600	4,900	3,700	2,200	1,900	1,000	1,200	2,300	2,900	4,900	6,500	7,700	8,500	9,000	10,500	11,000			
16	11,600	10,600	10,100	9,500	8,800	8,100	7,200	5,800	4,200	2,600	2,200	1,100	1,500	2,700	3,300	5,600	6,800	7,900	8,600	9,300	9,700	10,000	10,400		
20	11,500	10,600	10,000	9,500	8,800	8,100	7,500	6,500	4,000	3,400	2,200	2,600	2,700	4,100	5,300	6,800	7,500	8,700	9,300	9,800	10,200	10,700			
24	11,500	10,400	9,900	9,500	8,900	8,300	7,900	7,200	6,600	5,100	4,500	3,100	3,600	3,700	5,800	7,100	7,700	8,300	8,800	9,300	9,800	10,100	10,600		
28	11,400	10,300	9,900	9,500	9,000	8,600	8,200	7,600	7,100	6,200	5,500	3,900	4,400	5,900	6,700	7,300	7,900	8,500	9,800	9,300	9,800	10,100	10,400		
32	11,200	10,300	9,900	9,500	9,000	8,600	8,100	7,600	6,900	6,000	5,100	3,400	3,900	5,400	6,200	7,700	8,100	8,500	9,800	9,300	9,800	10,100	10,400		
36	11,200	10,300	9,900	9,500	9,000	8,600	8,100	7,600	6,900	5,100	3,500	3,900	5,100	6,100	7,000	7,600	8,100	8,700	9,200	9,700	10,100	10,500			
56	10,800	10,000	9,400	9,200	8,900	8,300	7,800	7,300	6,800	6,000	5,400	4,400	4,300	4,700	5,800	6,300	7,000	7,500	8,000	8,300	8,800	9,200	9,600	10,200	

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec.

TABLE IV 36. FUEL VAPOR CONCENTRATIONS IN PPM

Test 36 Conditions: Fuel - avgas. Temperature - 65°F R.H. - 60% Sample Configuration No. 4. Four gallons of avgas in a spill in the center of the east wall 6/13/72.

Time (min)*	Sample Point Numbers													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
0	11,400	9,000	6,900	3,600	2,400	900	600	700	400	500	400	500	500	500
4	15,000	11,000	10,500	9,000	7,500	5,000	3,700	2,100	1,900	1,100	800	600	400	200
8	15,200	12,100	11,000	10,100	9,700	6,800	5,400	4,000	2,400	1,500	1,000	1,400	1,000	1,000
12	15,000	12,000	11,000	10,100	9,600	6,600	5,100	3,600	7,800	5,100	4,400	3,400	3,300	2,000
16	12,900	11,900	11,100	10,400	9,500	6,900	6,100	7,400	6,600	5,200	4,500	3,200	3,000	2,000
20	11,500	10,700	10,100	9,500	8,400	8,300	7,700	7,000	6,400	5,100	4,900	3,400	3,600	2,000
24	11,500	10,700	10,000	9,500	8,300	8,300	7,800	7,200	6,700	5,100	5,400	4,300	4,100	4,900
52	11,000	10,000	9,500	9,000	8,400	7,900	7,400	6,900	6,500	6,100	6,000	5,800	5,800	5,800
56	11,000	10,000	9,500	9,100	8,100	7,700	7,100	7,400	6,300	6,400	6,100	5,900	5,900	5,900
60	10,900	10,000	9,500	9,000	8,400	8,100	7,400	7,100	6,700	6,400	6,200	5,800	5,900	5,900

^aThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec.

TABLE IV-37. FUEL VAPOR CONCENTRATIONS IN PPM

Test 37 Conditions: Fuel - avgas. Temperature - 76°F. R.H. - 40%. Sample Configuration No. 4. Four gallons of avgas in a drip test. 6/16/72.

Time (min)*	Sample Point Number													21	22	23	24
	1	2	3	4	5	6	7	8	9	10	11	12	13				
0	4,000	400	400	200	200	200	200	200	200	200	200	200	200	200	200	200	200
4	10,000	2,000	1,000	500	500	200	200	200	200	200	200	200	200	200	200	200	200
8	4,000	4,500	2,500	1,200	1,000	500	500	200	200	200	200	200	200	200	200	200	200
12	10,100	6,000	3,700	2,600	2,000	1,100	900	400	400	300	300	300	300	300	300	300	300
16	10,100	7,200	5,100	3,800	3,200	2,300	1,800	1,000	1,000	500	500	300	300	400	1,000	1,000	1,000
20	10,700	7,800	6,200	4,800	4,100	3,000	2,500	1,800	1,800	900	900	600	600	500	1,000	1,000	1,000
24	10,100	8,100	7,100	5,900	5,100	3,900	3,200	2,600	2,600	1,200	900	1,000	1,000	1,000	1,000	1,000	1,000
48	11,100	8,400	8,300	7,800	6,900	6,000	6,000	4,200	3,600	3,300	2,900	2,100	2,900	3,900	3,800	5,000	5,000
72	12,700	9,300	8,900	8,400	7,800	7,300	6,100	5,500	4,500	3,700	3,700	3,900	3,900	4,600	5,100	6,000	7,400
96	12,600	10,500	10,000	9,600	9,200	8,700	8,200	7,700	7,200	6,700	6,400	6,000	6,000	6,000	6,000	6,000	6,000
112	12,600	10,800	10,300	10,000	9,700	9,200	8,800	8,100	7,900	7,600	7,300	7,000	7,000	7,000	7,000	7,000	7,000
44	10,000	10,000	10,000	10,100	9,600	9,100	8,600	8,100	7,700	7,400	7,100	6,900	6,800	6,900	7,200	7,400	7,700
104	12,400	10,700	10,100	9,700	9,100	8,500	8,000	7,300	6,100	5,100	5,000	5,600	5,600	5,700	6,100	6,400	7,000
122	11,800	11,700	10,400	10,600	10,000	9,400	8,800	8,100	7,100	7,000	6,600	6,600	7,000	7,000	7,000	7,000	7,000
142	11,800	11,800	10,900	10,600	9,800	9,100	8,500	7,300	7,400	6,100	6,800	6,400	6,800	6,900	7,500	8,100	8,800
162	13,800	11,900	11,300	10,900	10,500	9,800	9,300	8,100	7,900	7,600	7,400	7,400	7,400	7,400	8,100	8,500	9,500

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec.

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